



**TU Delft**

**Deltares**  
Enabling Delta Life

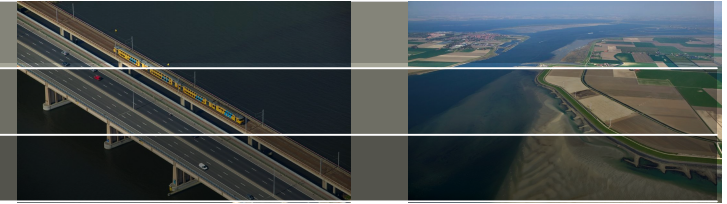


# **CT 5550 Pumping stations and transport pipelines**

Guest lecture on waterhammer

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# Learning goals



- Understand basic waterhammer phenomena
- Key notions for preliminary risk assessment
  - Pipe period – characteristic time
  - Wave speed
  - Joukowsky pressure
- Mitigating measures to reduce transient pressures

# Waterhammer problems in practice

Pipe burst during commissioning tests of 150 km, 1.6 m Diam. Pipe.

Control valve closed too early

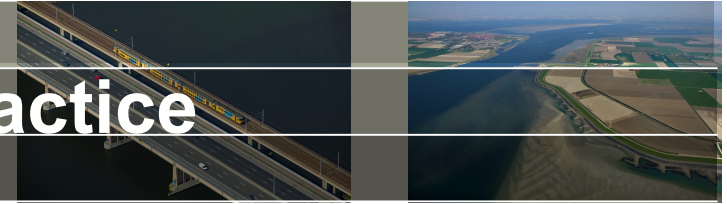


# Waterhammer problems in practice

Check valve closure caused  
severe pipe motion



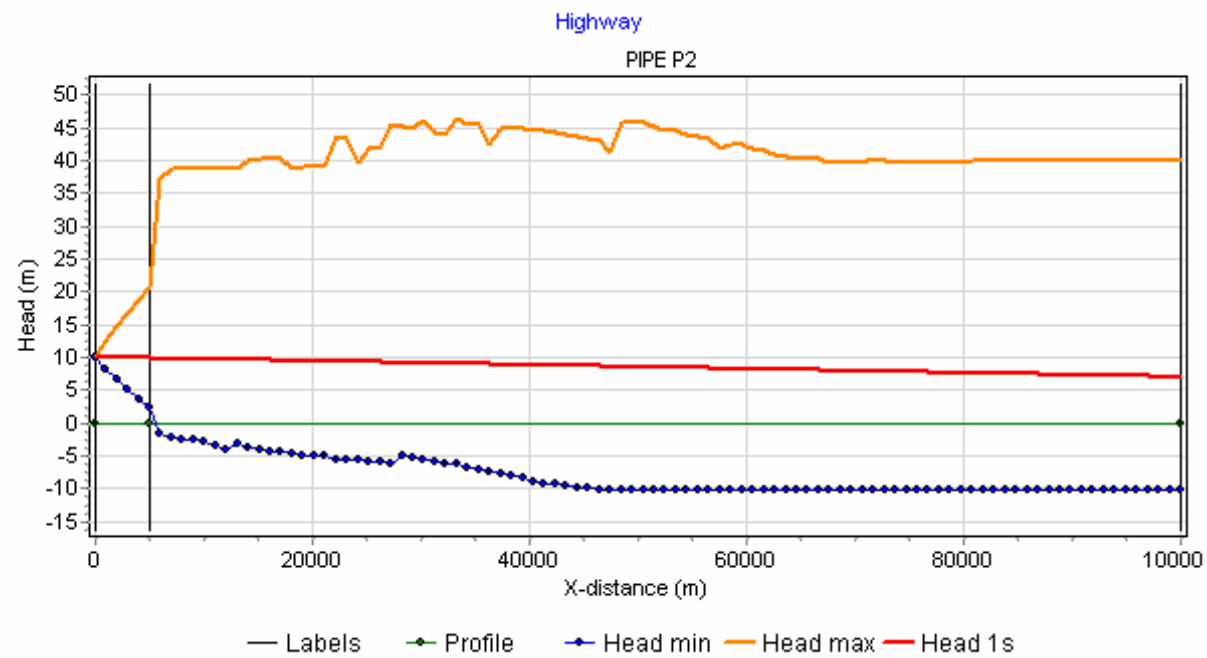
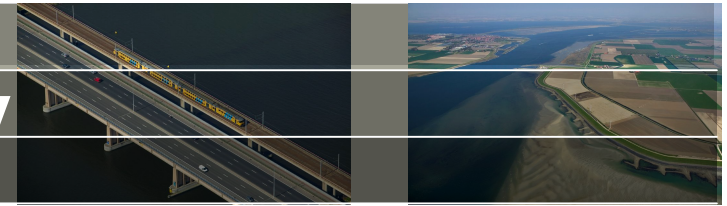
# Waterhammer problems in practice



Movie from Youtube –  
waterhammer on the highway

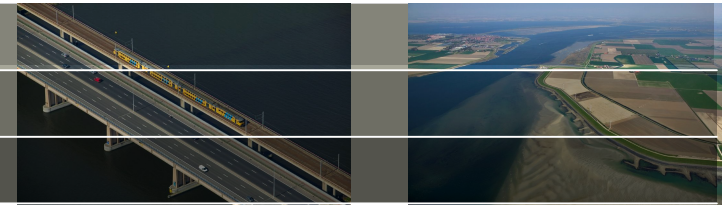


# Waterhammer on the highway





# Water hammer



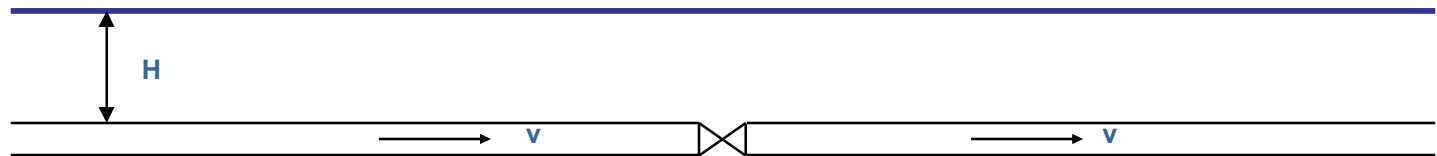
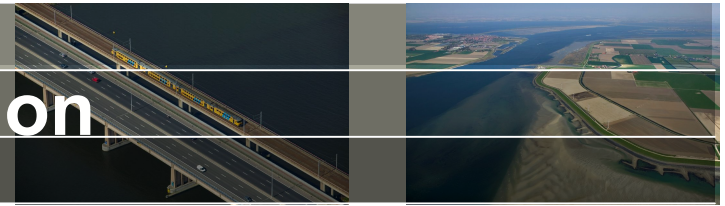
Pressurised systems

Exchange of kinetic and potential energy:

velocity changes  $\Leftrightarrow$  pressure changes

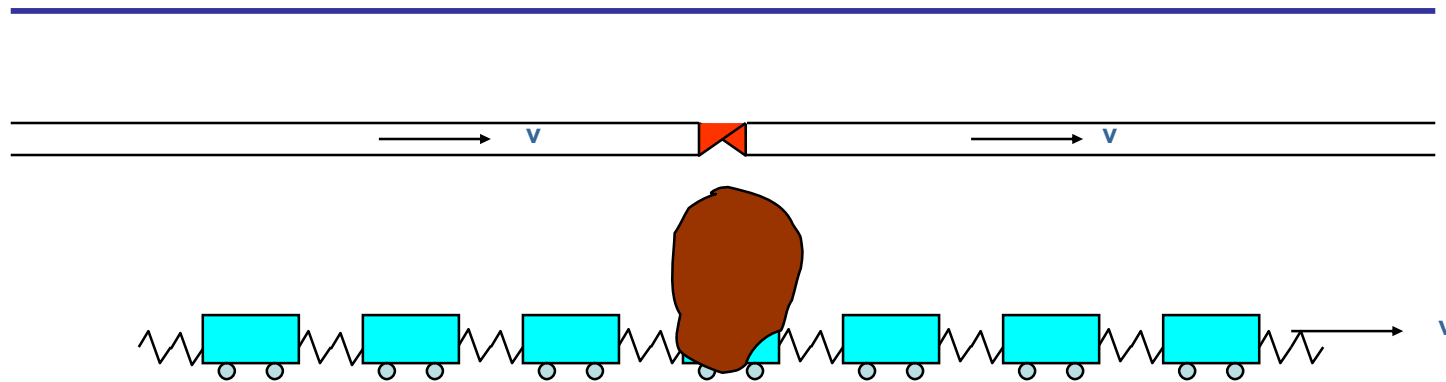
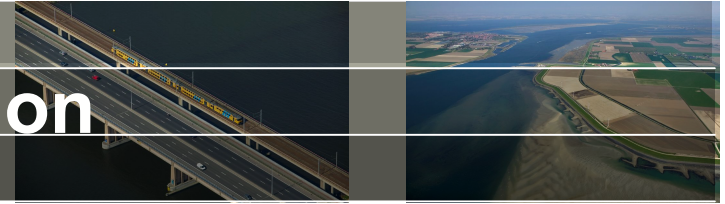
Changes are propagated through the pipeline system as high speed waves (pressure surges, water hammer)

# The water hammer phenomenon

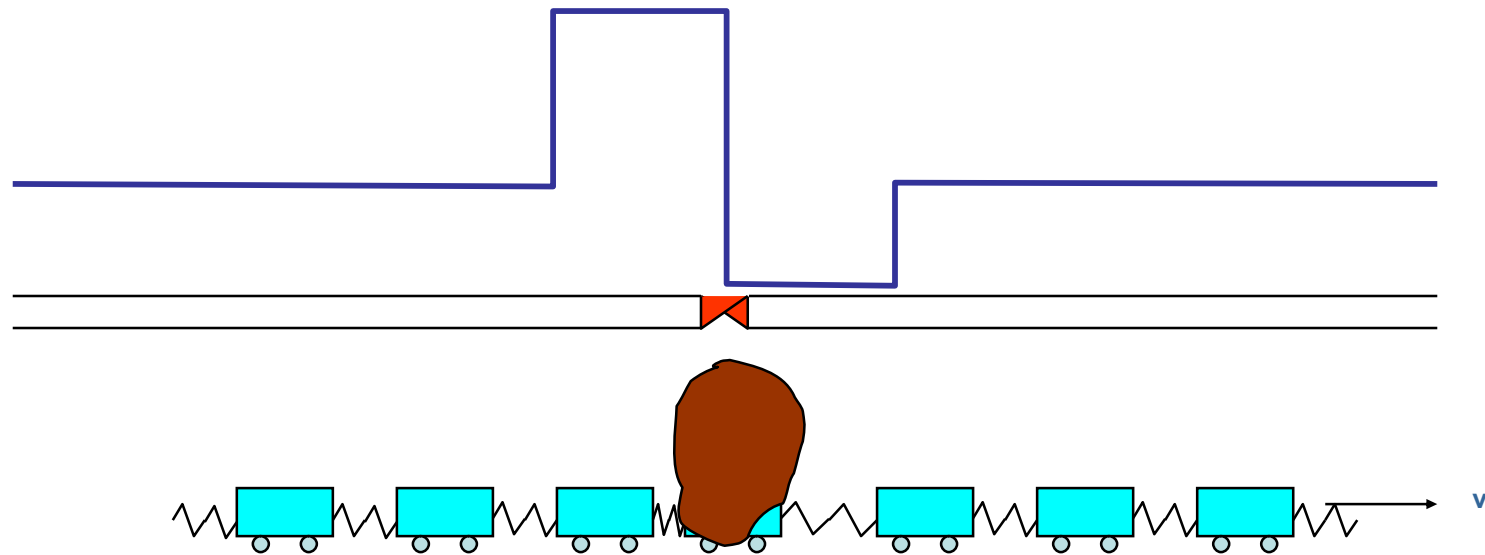
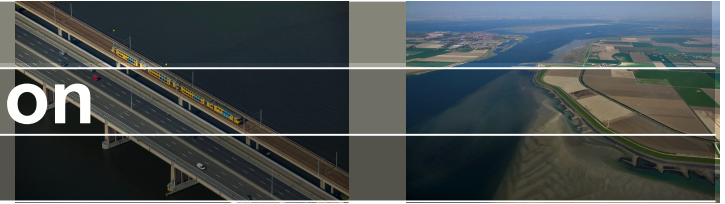




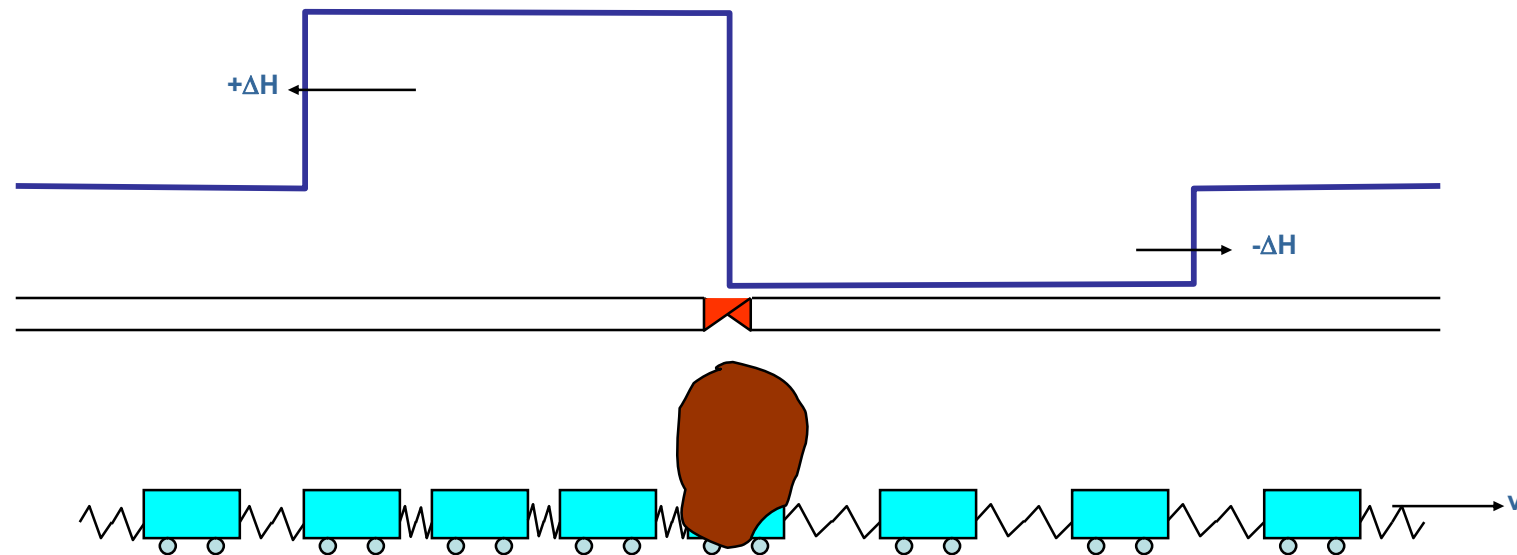
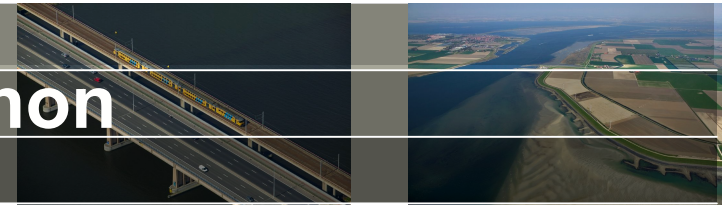
# The water hammer phenomenon



# The water hammer phenomenon



# The water hammer phenomenon

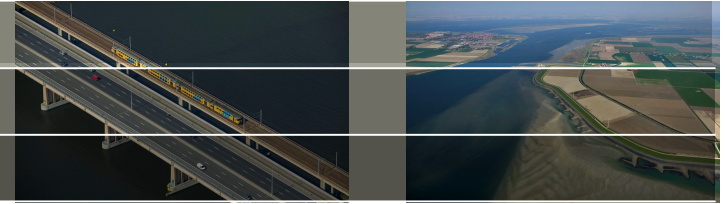


Overpressure and negative pressure waves

Head and velocity are interrelated

Pressure waves travel through system

# Water hammer essentials



Equations

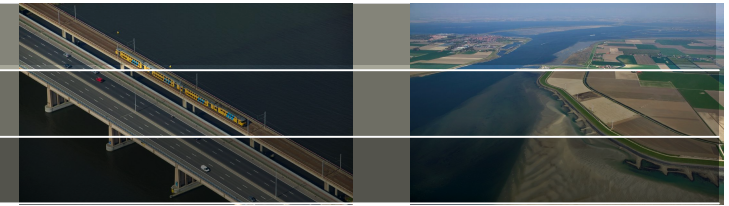
Assumptions

Wave propagation speed

characteristic time

Joukowsky pressure pulse

# Water hammer equations



**Momentum:** 
$$g \frac{\partial H}{\partial s} + \frac{\lambda}{8 A / P} v |v| + \frac{\partial v}{\partial t} = 0$$

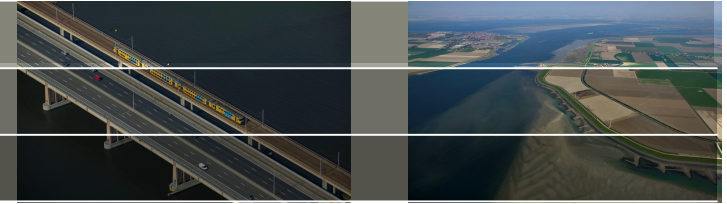
**Continuity:** 
$$\frac{\partial v}{\partial s} + \frac{g}{c^2} \frac{\partial H}{\partial t} = 0$$

with

$$c^2 = 1 / \rho \left( \frac{1}{K} + \frac{1}{A} \frac{dA}{dp} + \frac{1}{\Delta s} \frac{d\Delta s}{dp} \right)$$

in which  $H(s, t)$  and  $v(s, t)$

# Assumptions



## Momentum

- uniform velocity
- velocity head is negligible
- $v \frac{\partial v}{\partial x} \ll \frac{dv}{dt}$
- quasi-steady friction applies

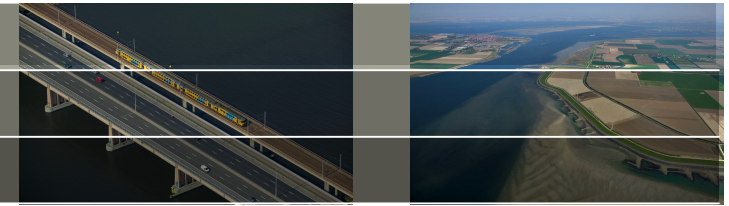
## Continuity

- $\frac{\partial \Delta s}{\partial s} v \ll \frac{\partial \Delta s}{\partial t}$
- $v \frac{\partial p}{\partial s} \ll \frac{\partial p}{\partial t}$

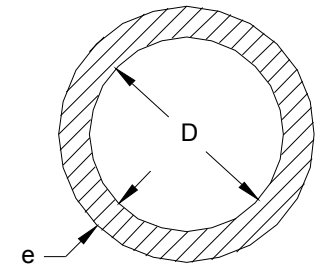
## Wave speed

- axial stress in pipe is zero  $\Rightarrow c_1 = 1$

# Wave propagation speed



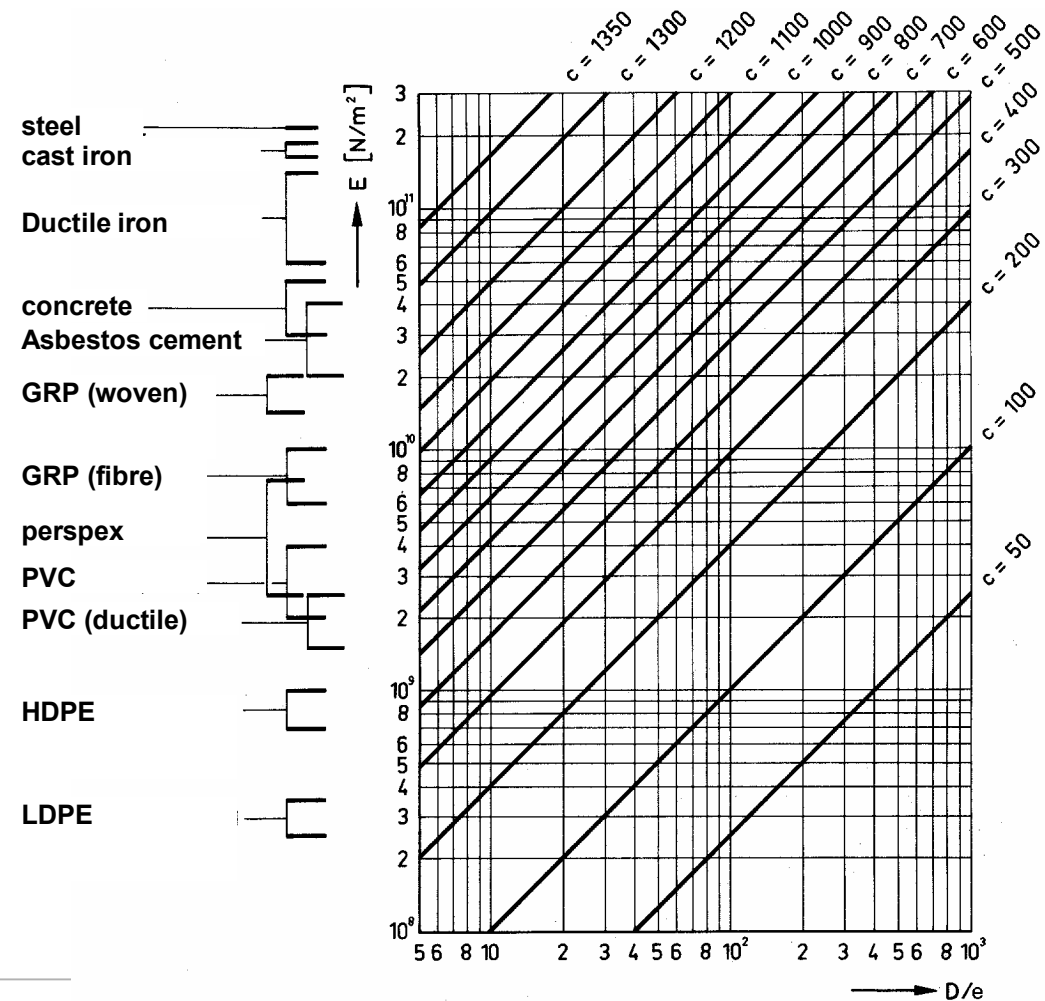
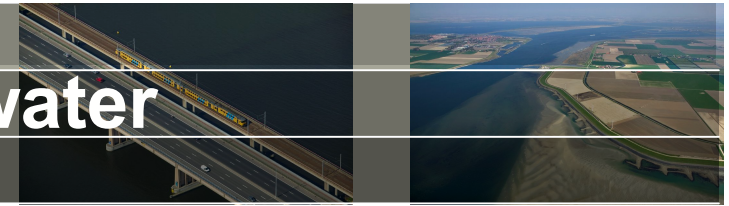
Pipe elasticity, Young's modulus ( $E$  [Pa]), +  
liquid bulk modulus ( $K$  [Pa]), +  
density ( $\rho$  [kg/m<sup>3</sup>], -  
diameter - wall thickness ratio ( $D/e$  [-]), -



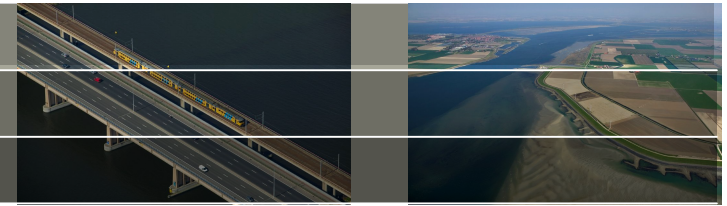
$$c = \frac{l}{\sqrt{\rho \left( \frac{C_l D}{eE} + \frac{l}{K} \right)}}$$



# Wave propagation speed in water

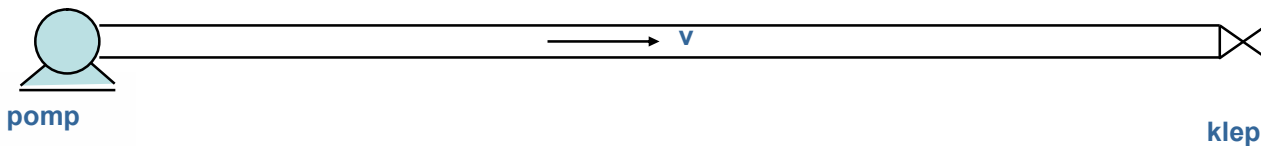
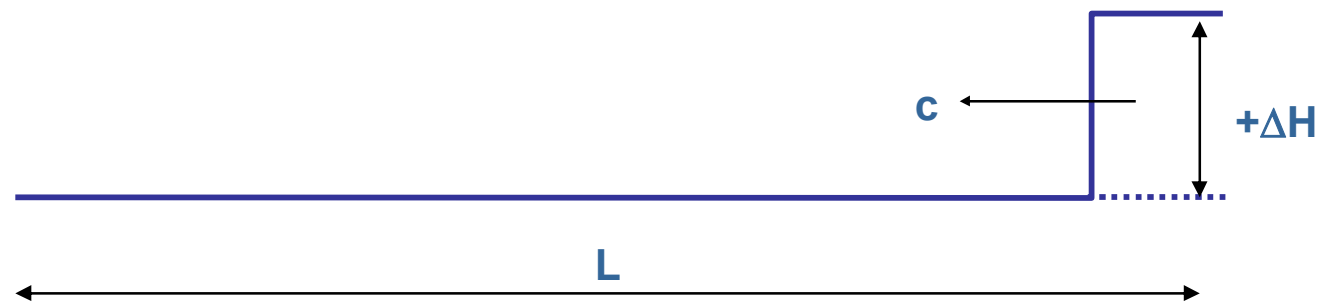


# Characteristic time

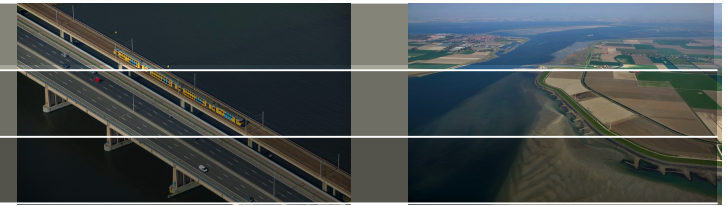


$$\mu = \frac{2L}{c}$$

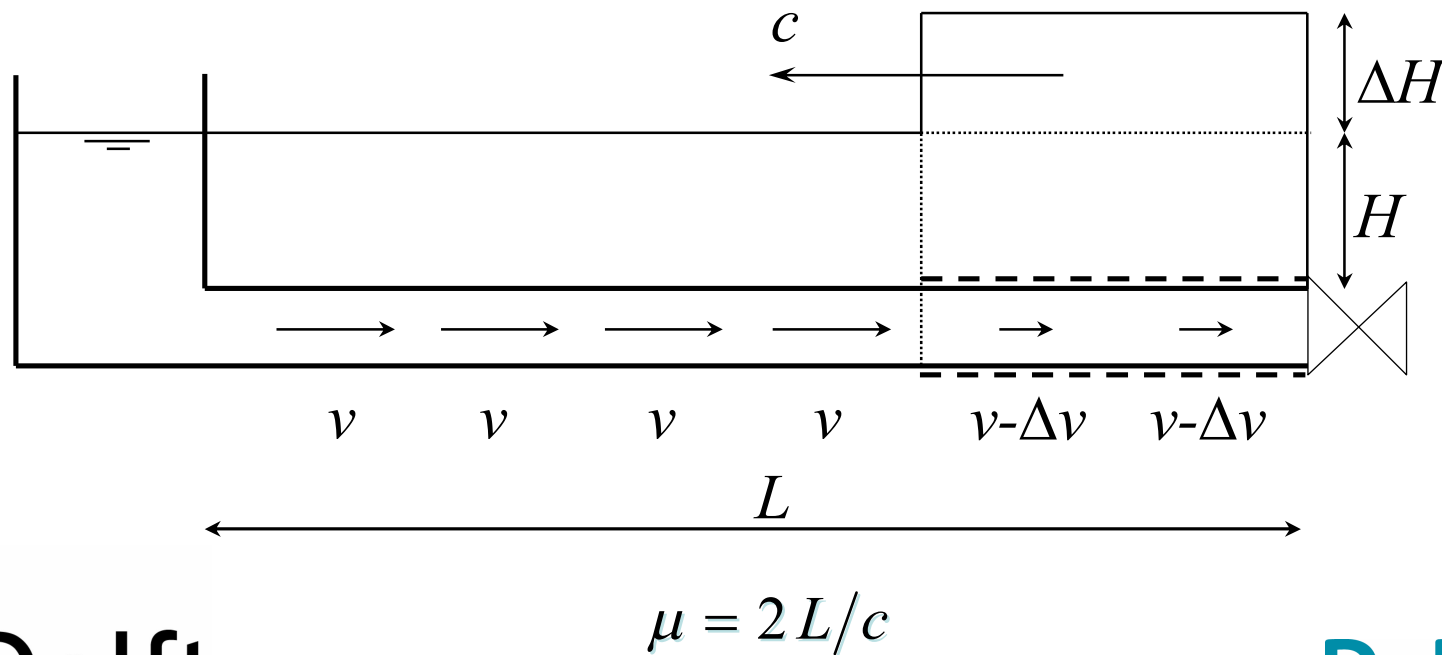
Travel time of a pressure wave to return to the source of the wave



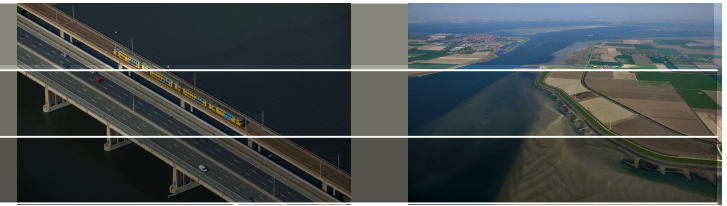
# Water hammer first estimate



**Joukowski:**  $\Delta H = \frac{c}{g} \Delta v$  **or:**  $\Delta p = \rho c \Delta v$

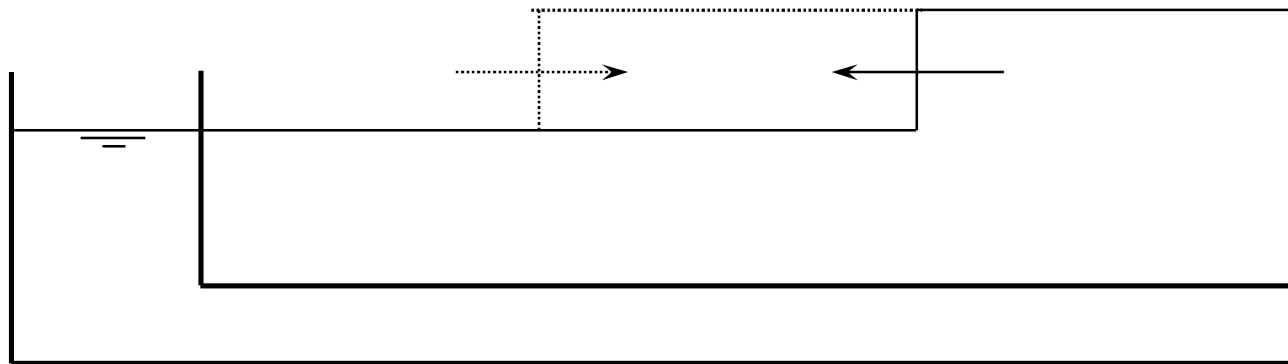


# Water hammer first estimate

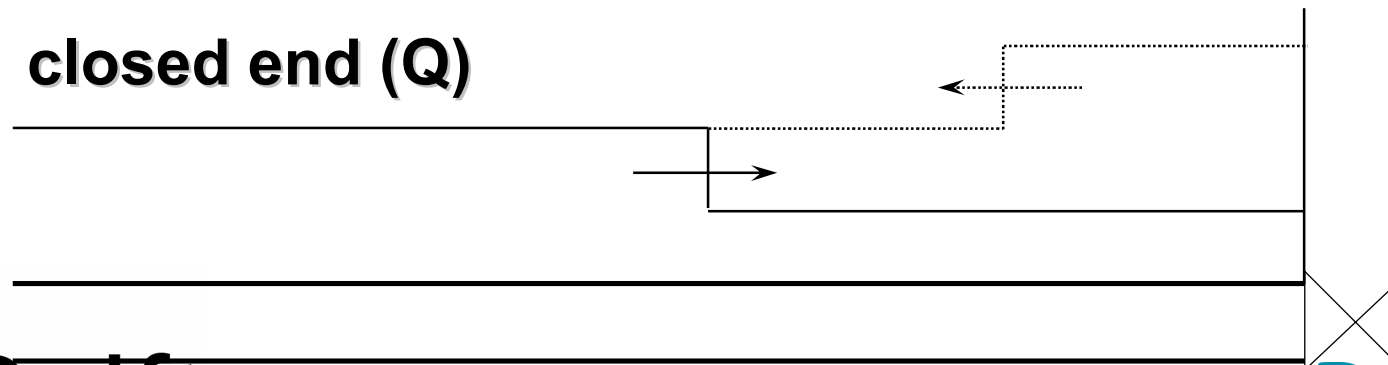


## Reflections:

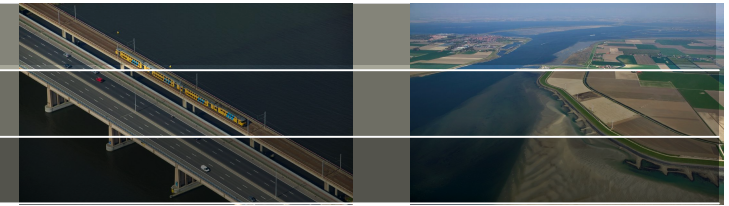
open reservoir (H)



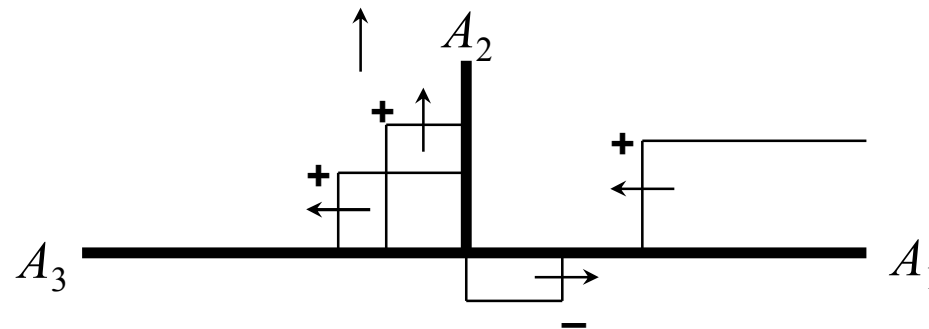
closed end (Q)



# Water Hammer first estimate



## Reflections on branches or diameter changes:



reflection: 
$$r = \frac{2 A_1}{\sum_{i=1}^n A_i} - 1$$

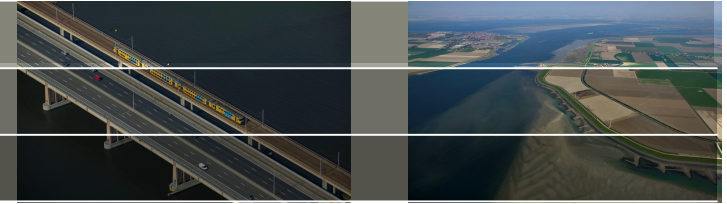
transmission: 
$$s = r + 1$$

**If  $A_1 = A_2 = A_3$ :**

$$r = \frac{2 A}{3 A} - 1 = -\frac{1}{3}$$

$$s = -\frac{1}{3} + 1 = \frac{2}{3}$$

# Examples in WANDA

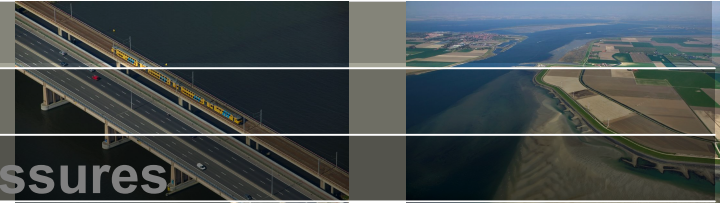


Valve closure (cases 1, 2)

Diameter change (cases 8, 9)

# Mitigation of waterhammer

Prevention of unacceptable transient pressures



$$\Delta H = \frac{c \cdot \Delta v}{g}$$

Reduce “ $c$ ”

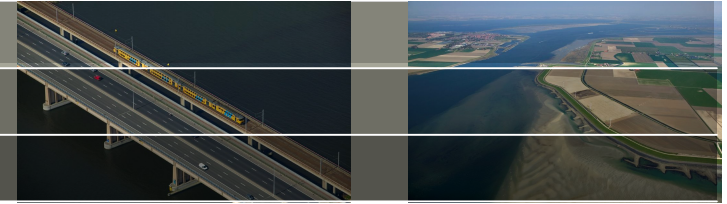
Reduce rate of “ $\Delta v$ ”

Limit local pressures

Geometrical modifications



Reduce “ $c$ ”



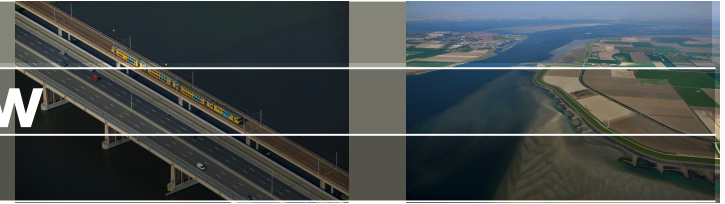
$$c = \frac{l}{\sqrt{\rho \left( \frac{l}{K} + \frac{D}{eE} \right)}}$$

Other pipe material ( $E$ )

Increase “free gas” concentration ( $K$ ) (tricky measure)

Thinner pipe wall ( $e$ ), not realistic

# Reduce rate of “ $\Delta v$ ” - overview



Air vessel

Water tower

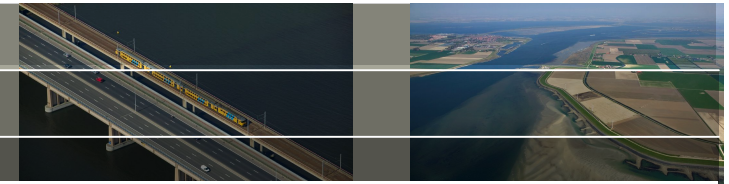
soft start/stop or frequency driven pumps

Slower valve manipulations

Flywheel on pumps

# Air vessels

reduce rate of " $\Delta v$ "

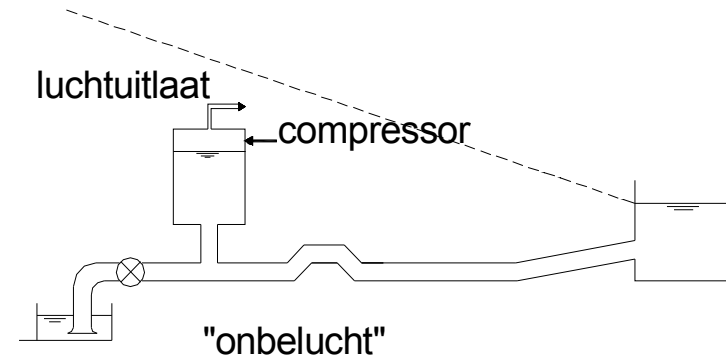


## Pro's

- Applicable at any pressure discharge combination

## Cons (depends on installation)

- Air volume must be maintained (air dissolves) with compressor, which requires maintenance
- Air vessels in side branches are vulnerable for biological contamination



**NOTE: check valve requirements**

Fast closing check valve or damped check valve is required

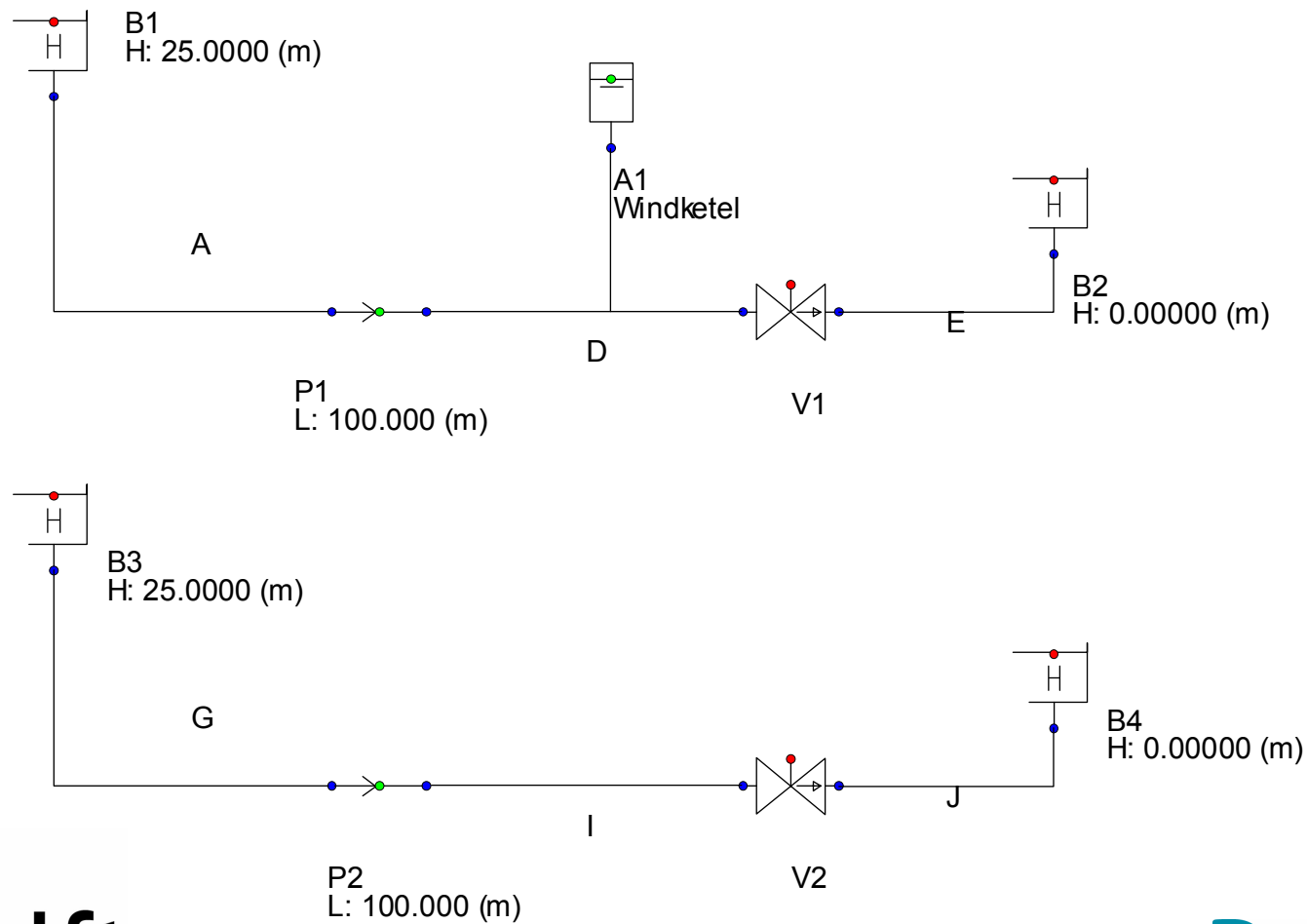
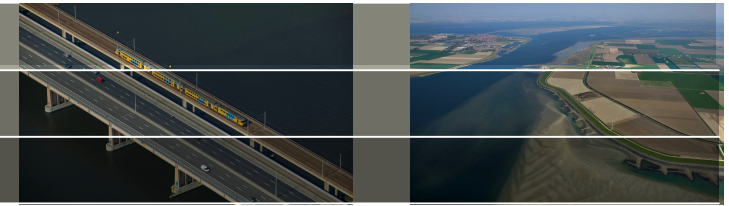
Sufficient distance between air vessel and suction level

Anchor forces

See also presentation on check valves

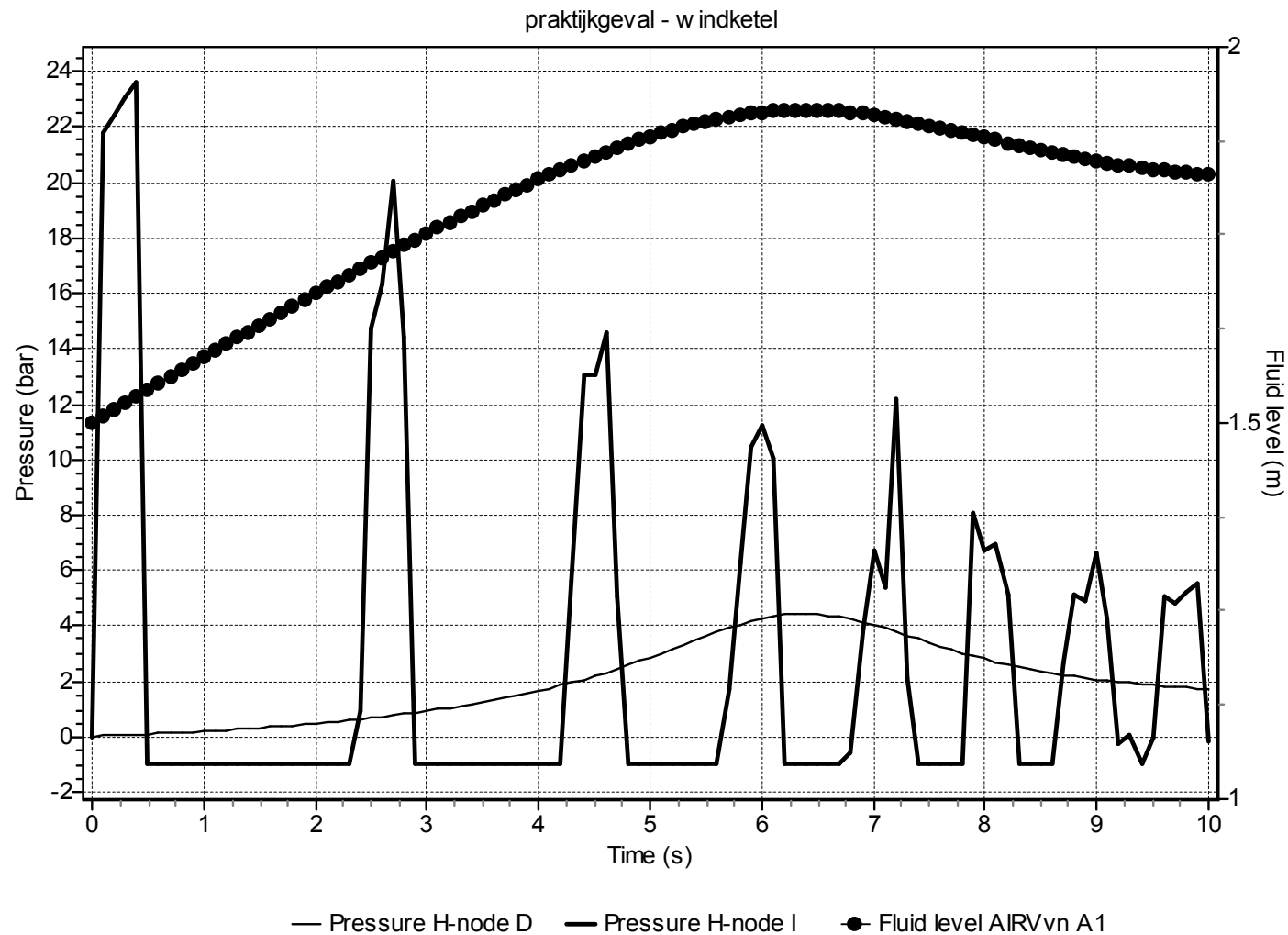
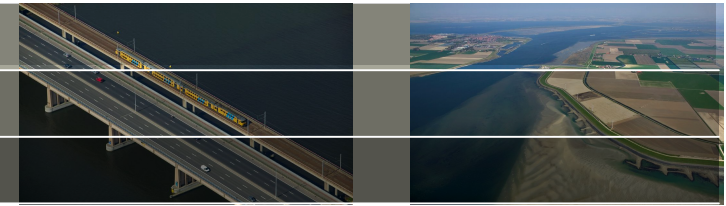
# Effect air vessel (1)

reduce rate of “ $\Delta v$ ”



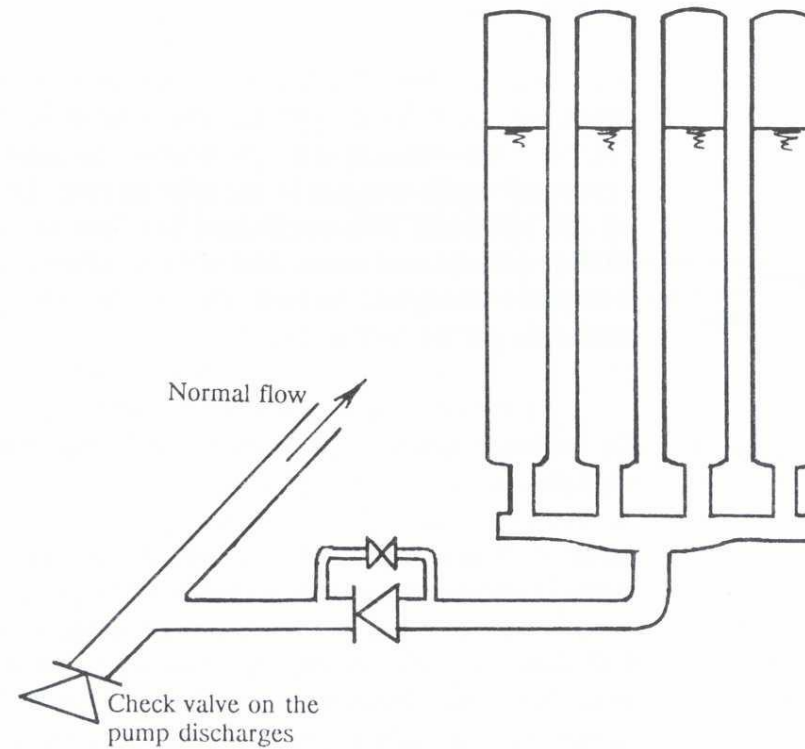
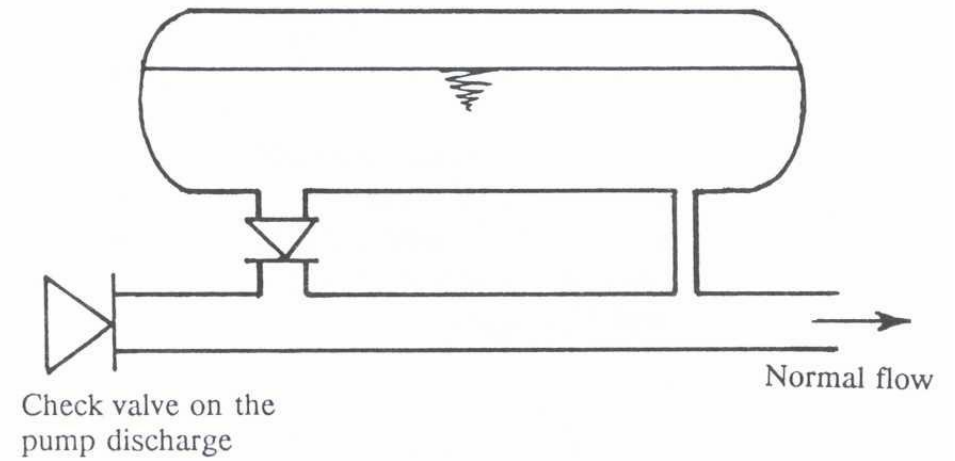
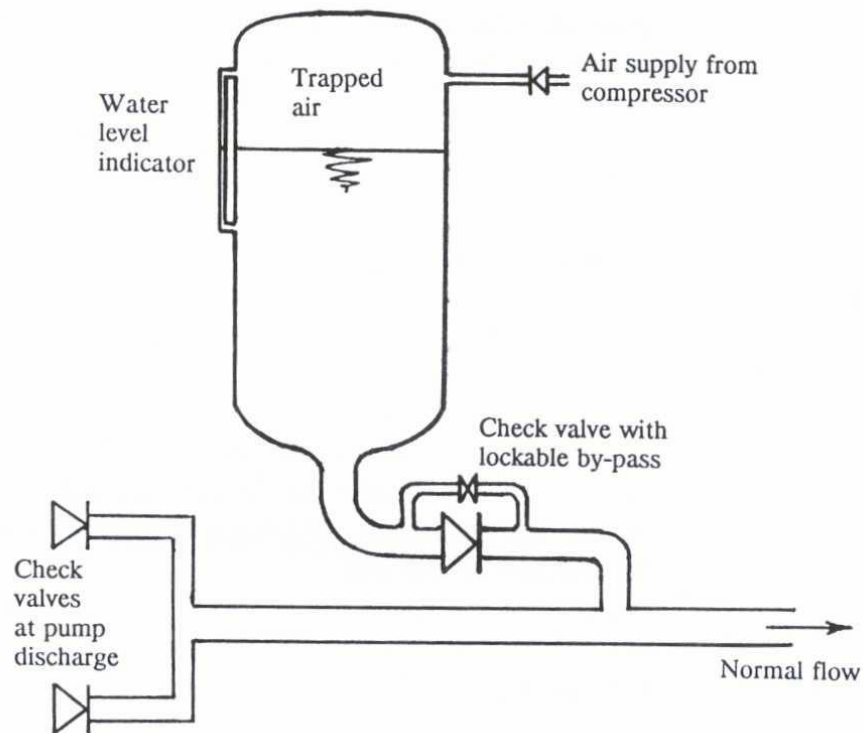
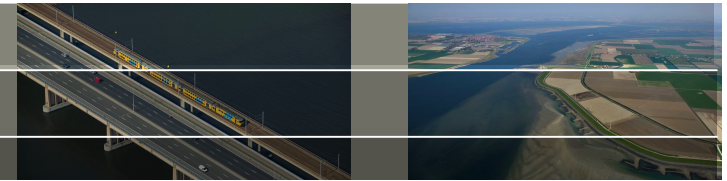
# Effect air vessel (2)

reduce rate of " $\Delta v$ "



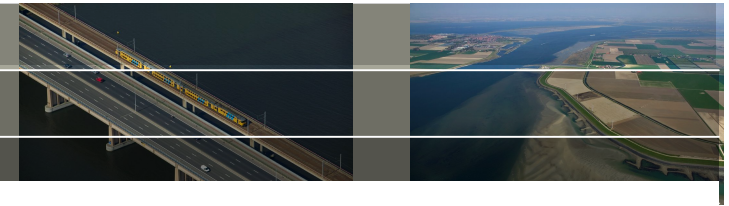
# Air vessels

reduce rate of “ $\Delta v$ ”



# Water tower

reduce rate of “ $\Delta v$ ”

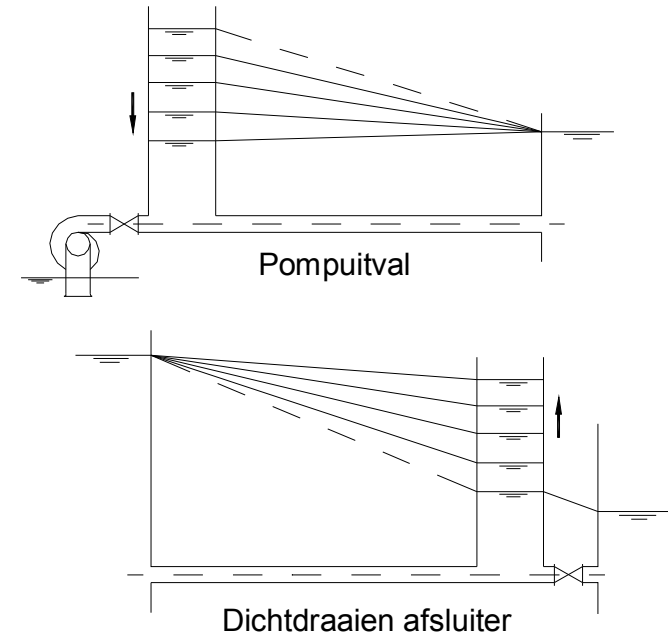


## Pro

- simple and reliable (no mechanical components required)
- Relatively large storage capacity (e.g. filling up the water tower before the break of a world cup final soccer)

## Cons

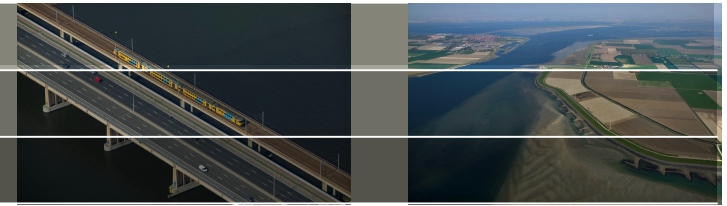
- Application is limited
  - > height of tower must exceed pump shut off head
  - > esthetic objections against high tower
- capacity of tower cannot be increased on an increase of the water demand
- odour problems (sewerage)
- risk for water quality deterioration
- maintenance is expensive



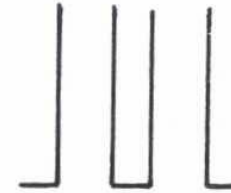


# Water tower

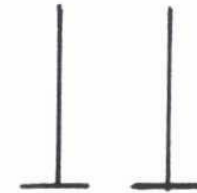
reduce rate of “ $\Delta v$ ”



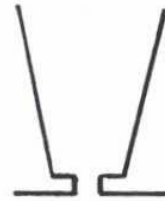
Simple



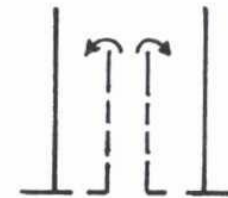
Multiple



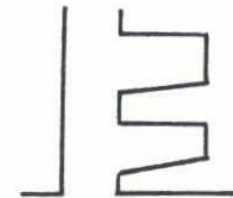
Orifice



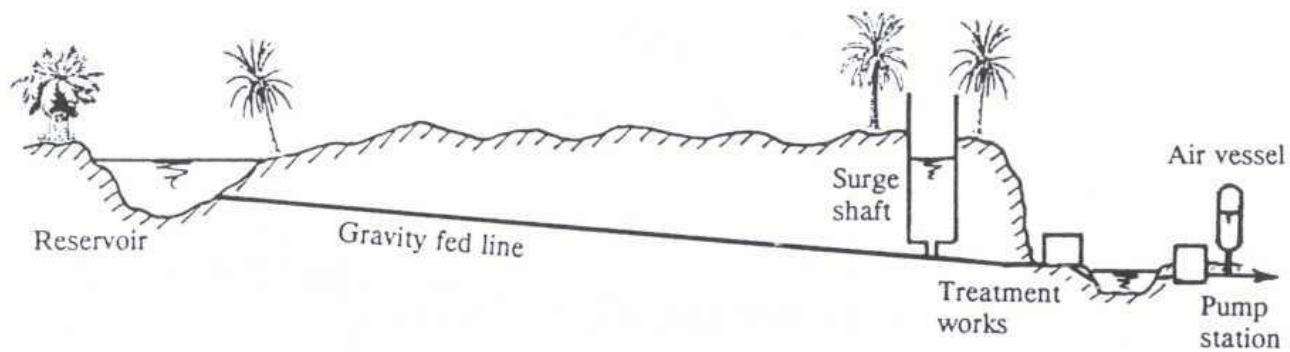
Tapered



Differential

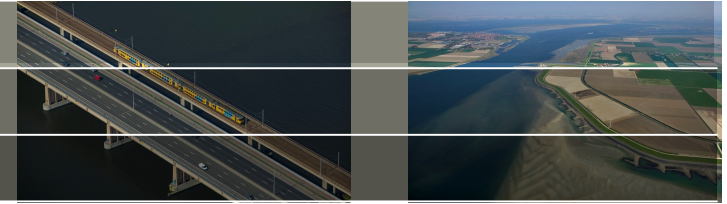


Galleried



# By-pass line

reduce rate of “ $\Delta v$ ”



## Pro

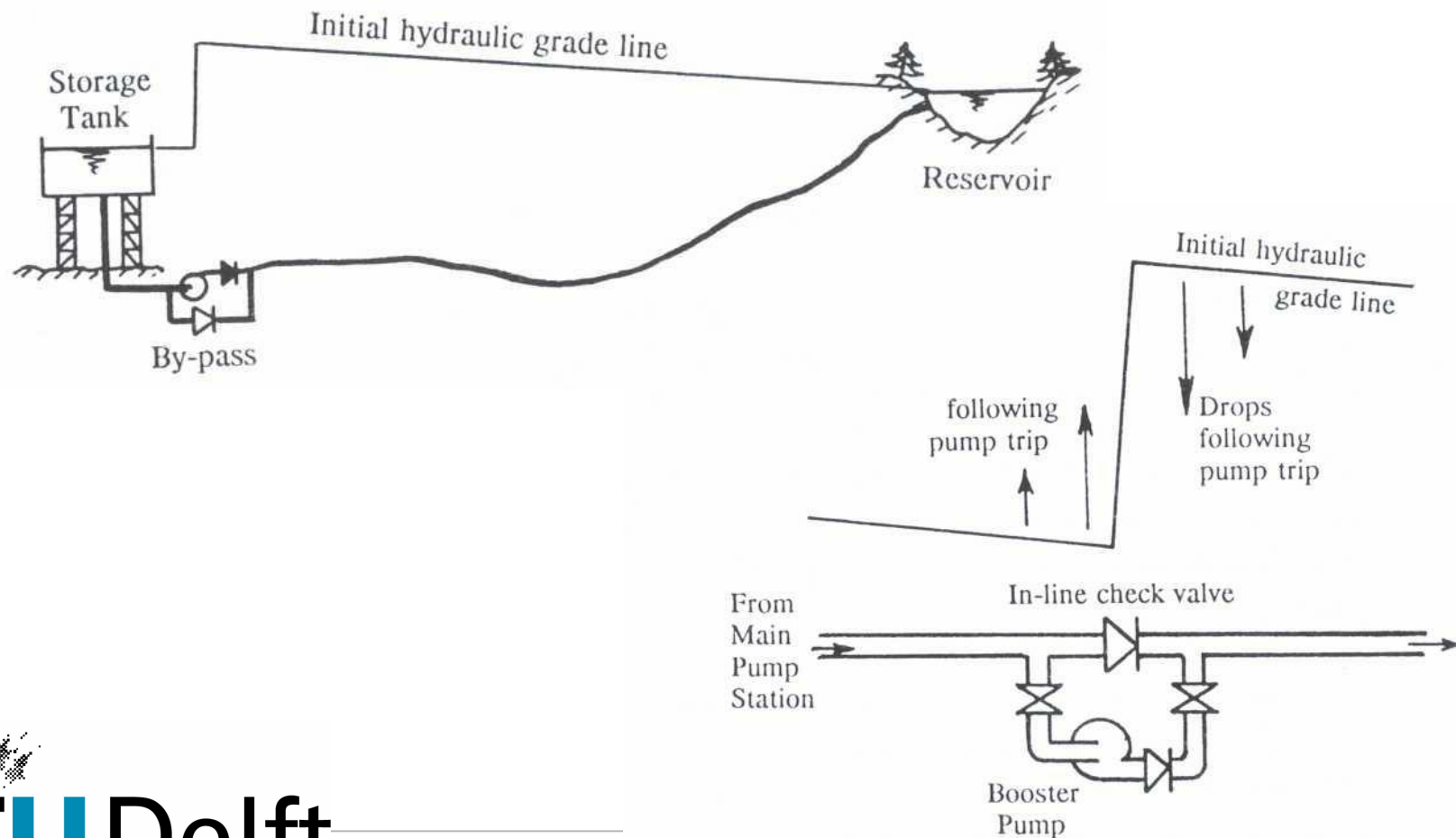
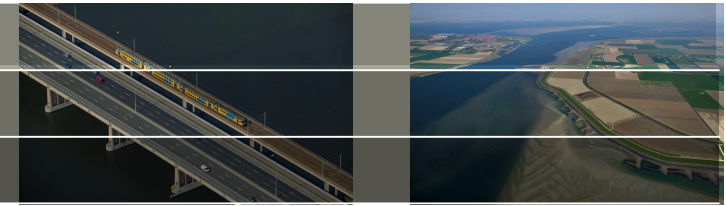
- No special requirements for pump check valves

## Cons

- ‘reservoir’ at sufficient level for effective by-pass
- by-pass delivery starts only after the system pressure has dropped to the suction level
- Application is limited to rel. short systems lengths

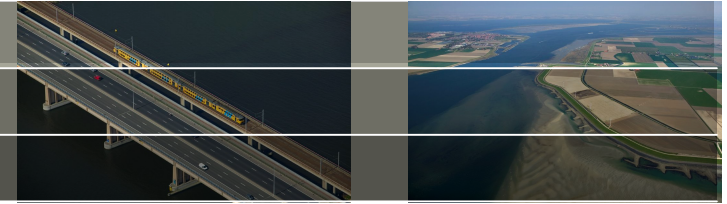
# By-pass line

reduce rate of " $\Delta v$ "



# Soft-starters / FO pumps

reduce rate of “ $\Delta v$ ”



## Pro

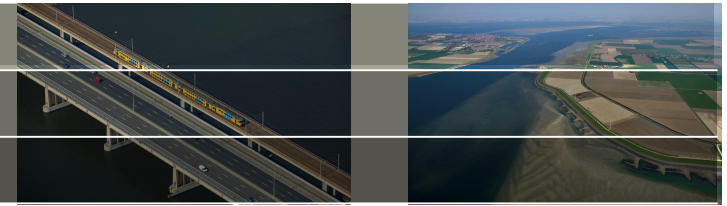
- Beneficial during normal operation

## Cons

- After power failure these measures provide no protection

# Slower valve manipulation

reduce rate of “ $\Delta v$ ”



## Pro

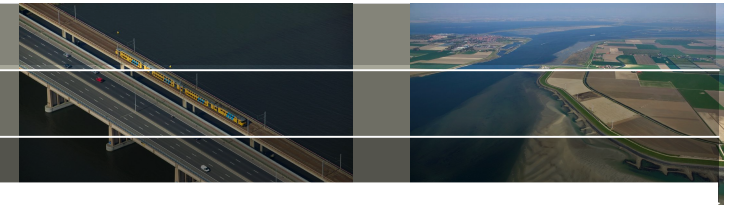
- No expensive anti-surge devices required

## Cons

- Manipulations must be slower than several ( $> 5$ ) pipe periods
- Pipeline cannot be blocked or opened very quickly

# Flywheel

reduce rate of “ $\Delta v$ ”

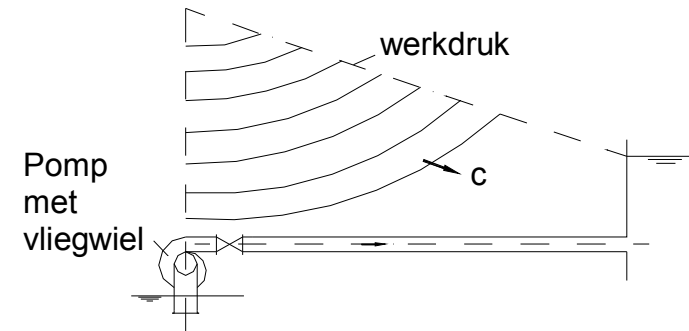
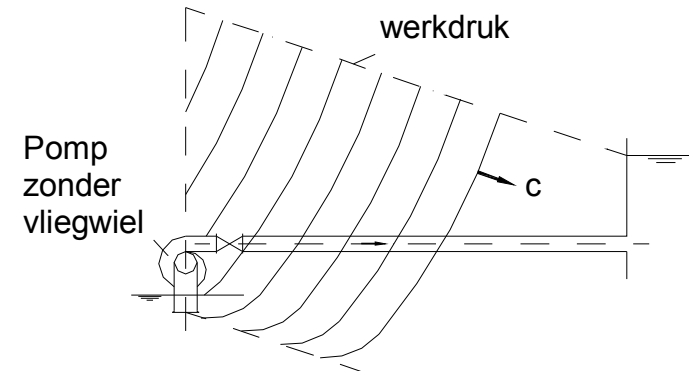


## Pro

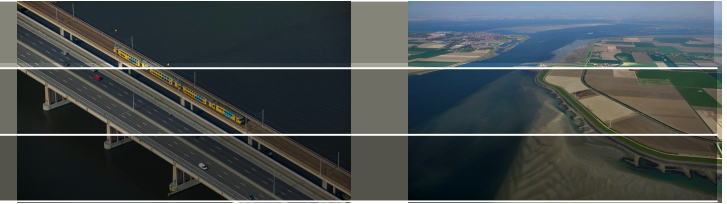
- Cheap construction
- Gradual check valve closure
- Limited maintenance

## Cons

- effect is limited to several km
- Pump motor must be large enough to start the flywheel
- No effect if impeller blocks
- Pump start costs more energy. Only economically feasible for pumps that run continuously on fixed speed



# Limit pressures - Overview



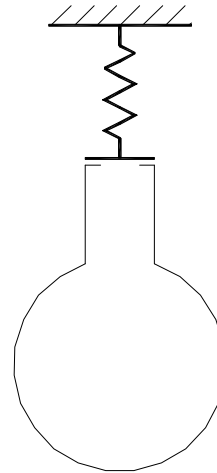
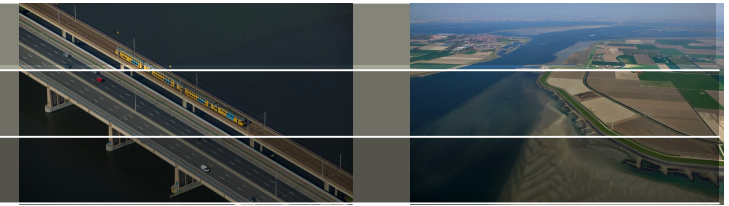
Local effect. Hence less effective than previous measures  
Suitable if inadmissible pressure are local as well (e.g. high points in cooling water system)

Safety valve / Pressure Relief Valve (PRV)  
Air valve / vent / vacuum breaker

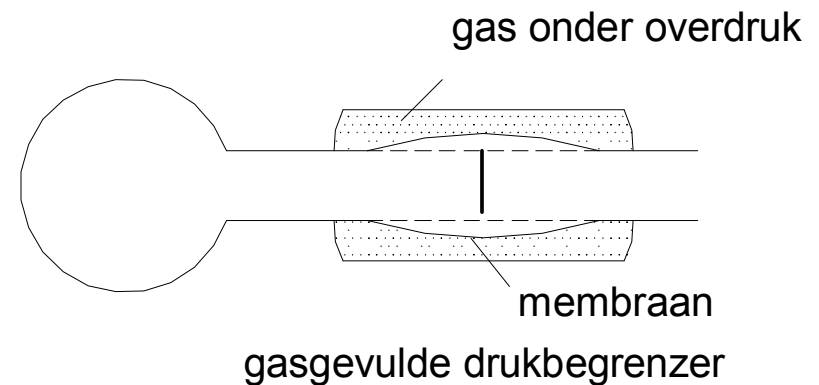


# Pressure relief valve

Limit pressures



Veerbelaste  
drukbegrenzer



## Pro

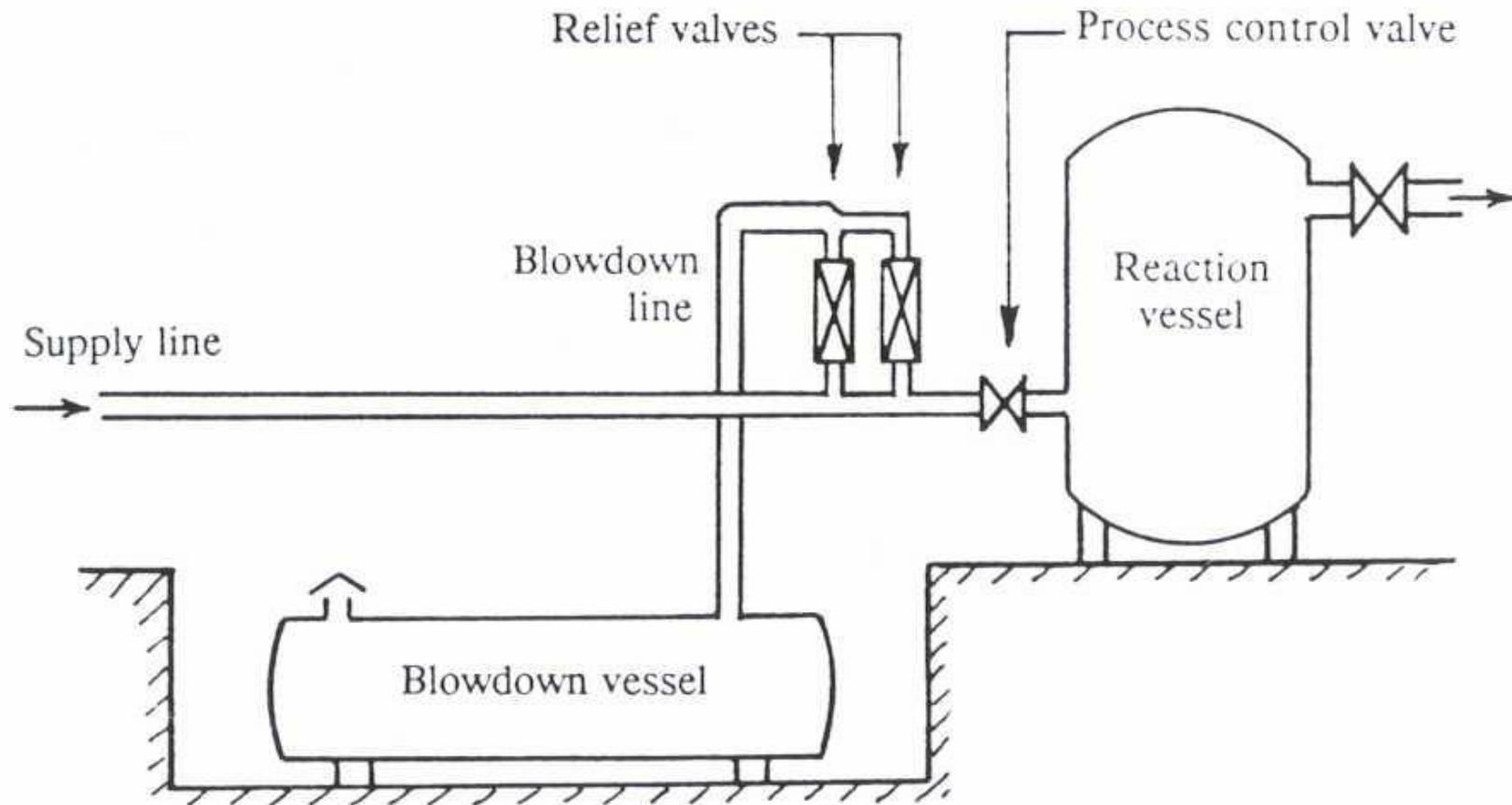
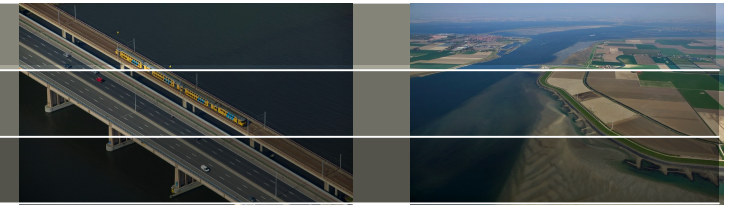
- Pressure is limited locally

## Cons

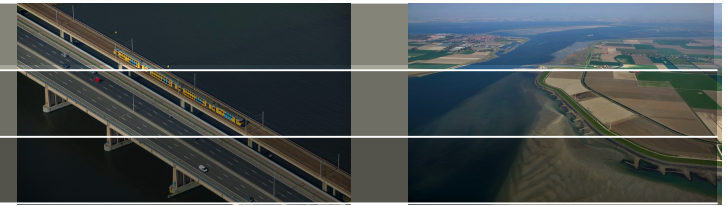
- Periodic maintenance required
- Relief lines required to dump ejected liquids
- Risk of hammering PRV, if PRV capacity is not well sized

# Pressure relief valve

Limit pressures



# Damper/accumulator



Gas pocket separated by a membrane

## Pro

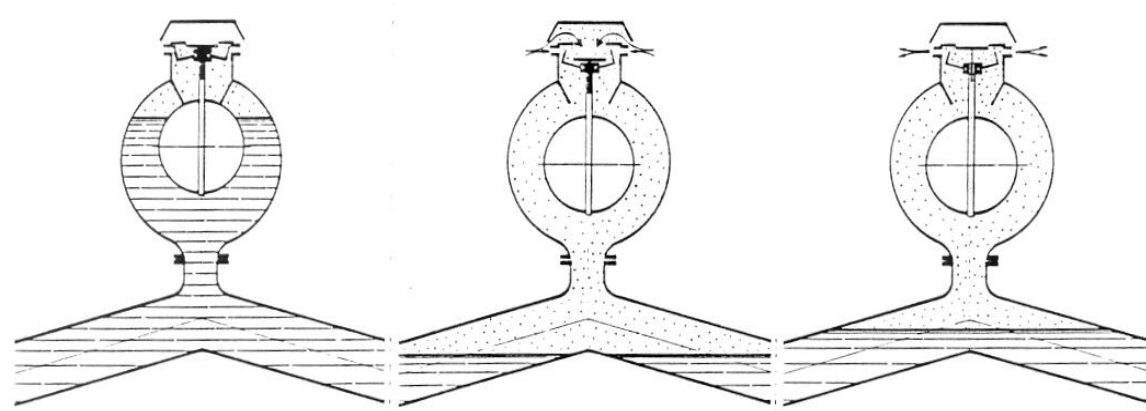
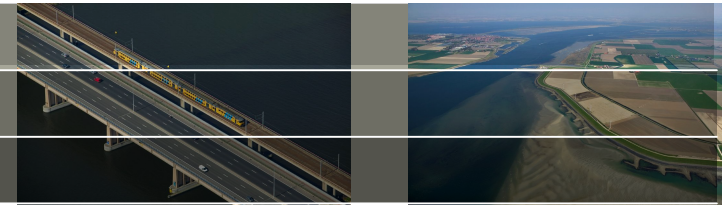
- No direct contact with liquid
- Gas pocket does not dissolve
- Set pressure provides flexibility

## Cons

- Volume limited
- Activated only after set pressure is exceeded

# Air valve

## Limit pressures

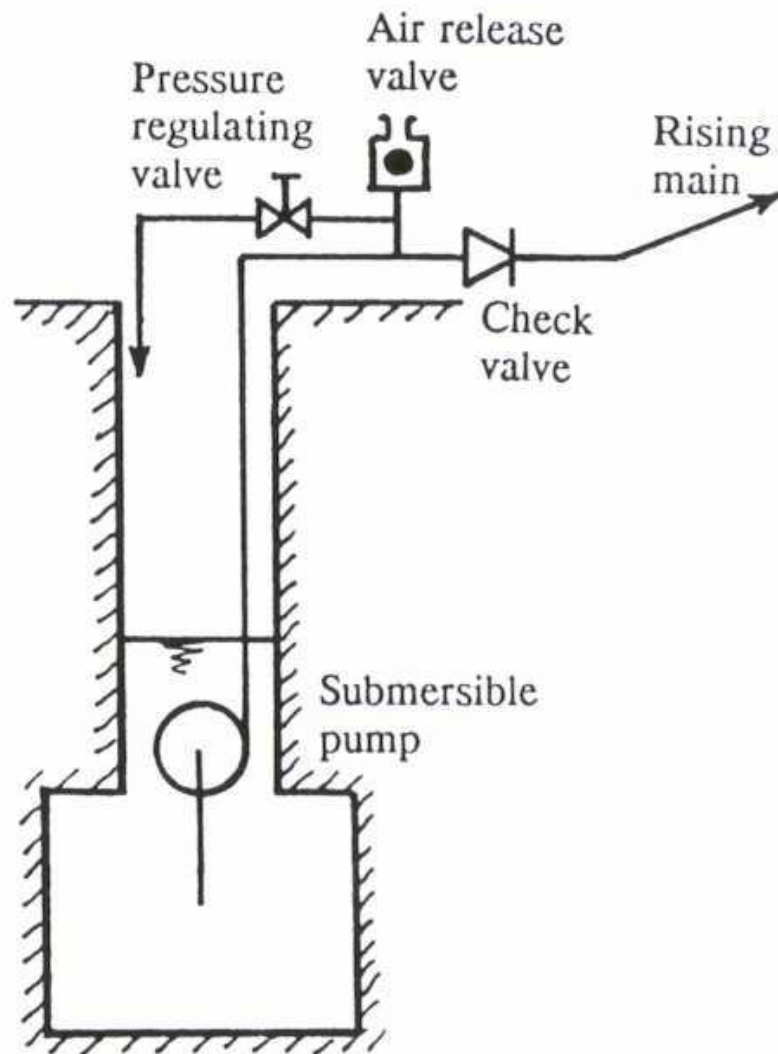


### Pro

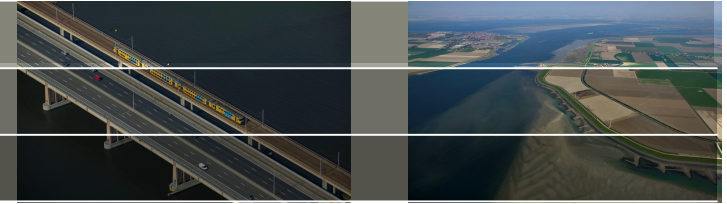
- Limit pressure locally

### Cons

- All incoming air should be released afterwards
- Correct installation and location are paramount for correct operation
- Vulnerable for fouling, blocking. Hence periodic maintenance required

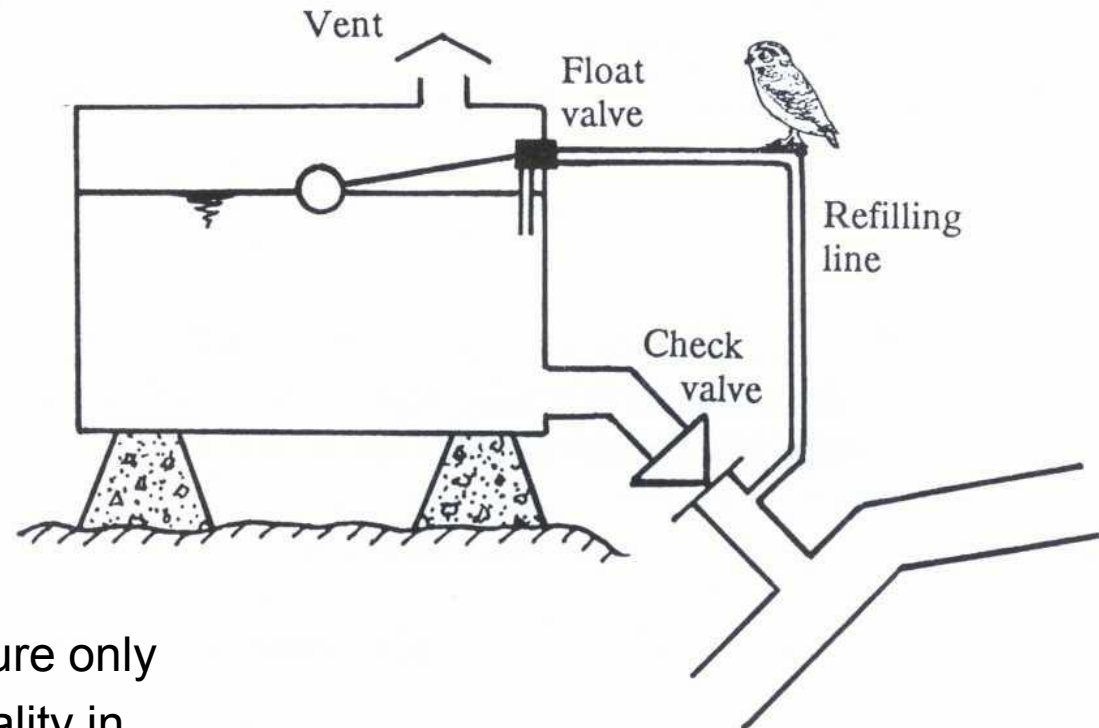


# Feed tank



## Pro

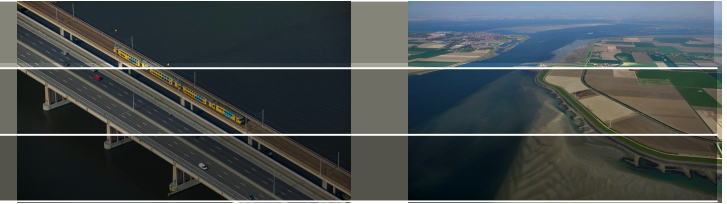
- Simple construction
- Self refilling



## Cons

- Limits negative pressure only
- Risk of poor water quality in feed tank

# Geometrical modifications

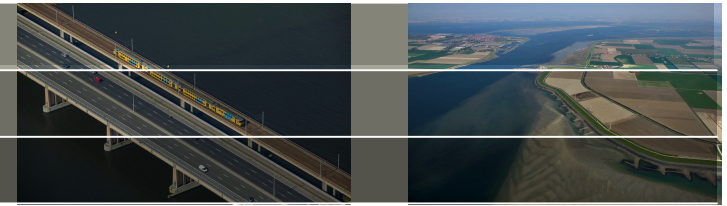


Increase pipe diameter

Reduce average system pressure

- Minimise number of bends, etc.
- Reduce downstream boundary head

# Exercise 8

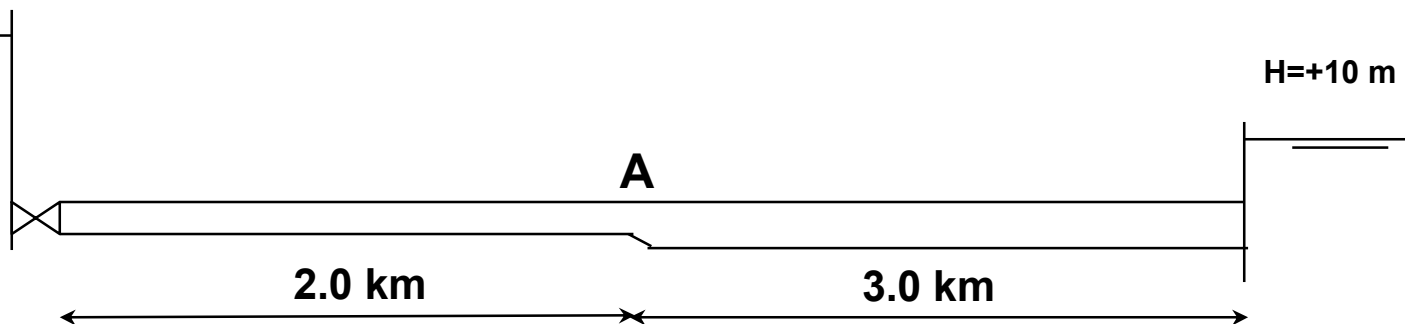


## Fast valve opening

$H=+20$  m

$C = 500$  m/s

$H=+10$  m



$L = 1000$  m

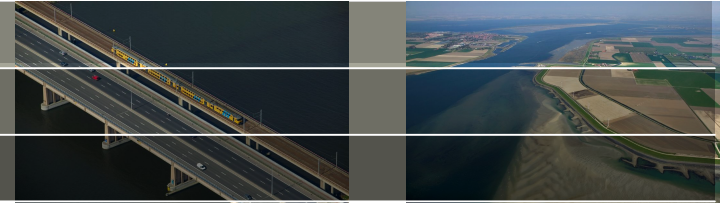
$D_1 = 300$  mm;  $D_2 = 424$  mm

frictionless pipe, conveying water

Draw time graphs of head at 0 km, 2.5 km and 5 km (first 22 s)



## Exercise 9



**Derive Joukowski's Law from Newton's second law of motion. You may assume the wave speed equals  $c$ .**