## Chapter 3

## Physics of cavitation: GAS CONTENT AND NUCLEI

Objective: General description of the behavior of gas bubbles which act as cavitation nuclei

The beginning of cavitation is called cavitation inception. Inception is a special topic, because in the initial formation of cavitation nuclei are involved and once cavitation occurs these nuclei loose their meaning. In this chapter the need of nuclei will be explained and the presence of nuclei in fluids investigated.

### 3.1 Cohesive Forces

The initial formation of vapor (cavitation inception) is complicated, because pure water can withstand much lower pressures than the equilibrium vapor pressure without vaporization. This is due to the mutual attraction or cohesionof the water molecules. A classical experiment dating back to 1950 is that of Lyman J.Briggs [4, a soil physicist who after his retirement (at age 77!) did investigate the tension strength of fluids. He used a capillary Z-shaped tube rotating horizontally in a centrifuge. This created a calculable pressure in the center of the tube. The water remained inside the tube as long as no vapor was formed. The maximum tension (negative
pressure)as a function of temperature was obtained at 10 degrees Celcius and amounted to 277 bars ( 27.7 MPa )! Although this value was reduced to some 20 bars near the freezing point, it remained far away from the equilibrium vapor pressure. Similar experiments were carried out much earlier by Berthelot (1950) and Dixon(1909), See 5].It required careful attention of cleaning and purification of the water to obtain these high tensions, and still the theoretical tensile strength of water molecules is even much higher (5). In practical circumstances one may conclude that pure water does not cavitate. It should be kept in mind that it is very difficult to make "pure" water [7]. Contaminations of some sort are unavoidable in practice, and these contaminations determine the tensile strength of water.
The cohesive forces between water molecules are much greater than the forces between water molecules and other materials, the adhesive forces. It means that the next weak spot in water is the wall of the container or the surface of a wing in the low pressure region. So when a low pressure occurs on a surface, cavitation will start at the surface. However, the tensile strength due to these adhesive forces between e.g. metals and water is still orders of magnitude higher than the equilibrium vapor pressure.

In practice the main mechanism of inception is the growth of small gas bubbles called $n u$ clei, which are present in the water. These nuclei are small bubbles, filled with air (or other gases) and vapor. The diameter can vary from a few microns to nearly visible bubbles of the order of 1 mm . That seems queer, because in standing water at atmospheric conditions gas bubbles will generally disappear due to two mechanisms: bubble rise and dissolution. To understand the behavior of nuclei it is useful to describe these two phenomena first.

### 3.2 Rising bubbles

In standing water a bubble will rise to the surface due to the difference between the weight of the bubble and the weight of the displaced water. This difference causes a buoyancy force on the bubble. Neglecting the weight of the air in the bubble this force $F$ is equal to the weight of water displaced by the bubble:

$$
F=\frac{\rho_{w} * \pi * D_{b}^{3} * g}{6}
$$

, in which $\rho_{w}$ is the specific mass of water and $D_{b}$ is the bubble diameter.
The subsequent rise velocity is determined by the drag $D_{b}$ of the bubble. That is a complicated matter, but the simplest solution is a solution of the Navier-Stokes equation in which the kinematic forces are negligible relative to the viscous forces. The drag of the bubble is thus completely due to friction along the bubble wall wilt a laminar boundary layer and this condition is expressed in non-dimensional terms as a low Reynolds number $R e_{b}=\frac{V_{b} D_{b}}{\nu}$, in which $n u$ is the kinematic viscosity of water and $V_{b}$ is the bubble velocity. In this equation it is also assumed that the bubble remains spherical, which is applicable for small bubbles at low velocities. The drag of a bubble can then be written as

$$
D_{b}=3 \pi \mu D_{b} V_{b}
$$

in which $\mu$ is the dynamic viscosity of water (related to the kinematic viscosity $\nu$ by $\nu=\frac{\mu}{\rho}$. The rise velocity of a bubble can then simply be written by equating the rise force $F_{D}$ with the bubble drag, which results in Stokes' law:

$$
\begin{equation*}
V_{b}=\frac{g * D^{2}}{18 * \nu} \tag{3.1}
\end{equation*}
$$

This equation is useful to estimate the time needed for a bubble to rise out of the measurement volume. Consider e.g. a nucleus of 100 microns ( $100 * 10^{-} 6 \mathrm{~m}$ )in diameter. As we will see later in chapter 4 , such a nucleus is sufficient in many cases to bring the cavitation inception pressure close to the vapor pressure. Such a nucleus reaches a rising speed (from eq. 3.1 ff

$$
\frac{9.81 * 10^{-} 8}{18 * 10^{-} 6}=0.55 * 10^{-} 2 \mathrm{~m} / \mathrm{sec}
$$

or approximately $5 \mathrm{~mm} / \mathrm{sec}$. In a towing tank the upper layer of 1 meter depth will be free of such nuclei after a few minutes. Nuclei of 10 microns take 100 times as much time, so a few hours.
At sea the turbulent motions in the upper layer of the water are often in sufficient motion to keep nuclei mixed up forever. But after a storm the nuclei content of the upper layer of the sea can contain much more larger nuclei. The storm itself creates these nuclei by breaking waves and the increased wave motions prevent the rise to the surface or at least delay it considerably. However, over time they will rise to the surface.

### 3.3 Dissolving bubbles

Another mechanism for gas bubbles to disappear is dissolution. In that case the gas bubbles disappear because the air dissolves in the surrounding water due to diffusion and the vapor in the bubble condensates because of the surface tension.

Water can absorb a lot of air and it is very important to distinguish between dissolved air and free air. Free air is present in the form of bubbles. The majority of the air in water is dissolved and dissolved air has no significant effect on the cohesive forces in the water.
At 15 degrees Celcius in atmospheric conditions the amount of air that can be dissolved in one cubic meter of water is about $25-30 \mathrm{~g}$ (25-30 liters in atmospheric conditions). This is expressed as the gas concentration $C=3 * 10^{-} 2 \mathrm{~kg} / \mathrm{m}^{3}$. In that case the water is saturated. In that condition there is no net transfer of air molecules through the free surface. The air content of water is often expressed as the fraction of the maximum amount of gas that can be absorbed: the saturation rate. For the calculation of the air content in in various units see Appendix A. Note that the saturation rate can be exceeded considerably without gas coming out of solution immediately. In that case the water is oversaturated or supersaturated and this can amount to two or three times the saturation rate.

As mentioned bubbles in water contain air and vapor. Dalton's law states that the total pressure exerted by a gaseous mixture is equal to the sum of the partial pressures of each individual component in a gas mixture. This empirical law was observed by John Dalton in 1801. So the pressure inside of a bubble is the sum of the partial pressures of air and vapor. The partial pressure of vapor is the equilibrium vapor pressure. In many conditions the vapor pressure can be neglected and a bubble can be considered as a pure gas bubble.

Transport of gas through the bubble wall is governed by Henry's law (formulated by William Henry in 1803), which states that at a constant temperature, the amount of a given gas dissolved in a given type and volume of liquid is directly proportional to the partial
pressure of that gas in equilibrium with that liquid. The coefficient is called Henry's constant, but this "constant" is temperature dependent.
When the water is not saturated, there will be a mass flow through the bubble wall and the bubble will disappear because the free air goes into solution. Even when the water is saturated, small bubble will disappear because the pressure inside a bubble is higher than in the surrounding fluid due to the surface tension, as will be discussed later.

Contrary to evaporation, diffusion is a relatively slow process. Evaporation takes place at the surface of a bubble only, but diffusion extends over a much thicker layer of fluid around the bubble. At the bubble wall the saturation rate of the water will immediately be such that the partial pressure of the dissolved air is equal to the partial pressure of the air in the bubble. When the saturation rate of the bulk of the water is different, air molecules will migrate to or from the bubble. Over a certain distance a concentration gradient will form.

The mass flow m in $\mathrm{kg} / \mathrm{m}^{3}$ through the wall of a bubble with radius R can be written as

$$
\begin{equation*}
\frac{d m}{d t}=4 \pi R^{2} D_{g}\left(\frac{d C_{g}}{d r}\right)_{R} \tag{3.2}
\end{equation*}
$$

in which $D_{g}$ is a diffusion coefficient ( $m^{2} / \mathrm{sec}$ ) and $C_{g}$ is the gas concentration in $\left(\mathrm{kg} / \mathrm{m}^{3}\right)$. The gradient $\left(\frac{\partial C_{g}}{\partial r}\right)_{R}$ is the gradient of the gas concentration at the bubble wall. When the vapor is neglected and the gas density remains the same the mass change is

$$
\frac{d m}{d t}=\rho_{g} \frac{d\left(4 / 3 \pi R^{3}\right)}{d t}
$$

and from eq. 3.2 the bubble radius changes as

$$
\begin{equation*}
\frac{d R}{d t}=\frac{D_{g}}{\rho_{g}}\left(\frac{d C_{g}}{d r}\right)_{R} \tag{3.3}
\end{equation*}
$$

Eppstein and Plesset 9 gave an approximate solution for the concentration gradient:

$$
\begin{equation*}
\left(\frac{d C_{g}}{d r}\right)_{R}=\left(\frac{1}{R}+\frac{1}{\left(\pi D_{g} t\right)^{1 / 2}}\right)\left(C_{g \infty}-C_{g R}\right) \tag{3.4}
\end{equation*}
$$

in which the length $\left(\pi D_{g} t\right)^{1 / 2}$ can be regarded as a diffusion boundary layer thickness. For small bubbles this thickness is much larger than the radius R , so eq. 3.4 can be written as

$$
\left(\frac{d C_{g}}{d r}\right)_{R}=\left(\frac{\left(C_{g \infty}-C_{g R}\right)}{R}\right.
$$

and eq. 3.3 can be integrated and written as

$$
\begin{equation*}
R^{2}=R_{0}^{2}+\frac{2 D_{g}\left(C_{g \infty}-C_{g R}\right)}{\rho_{g}} t \tag{3.5}
\end{equation*}
$$

The time to go completely into solution is when $\mathrm{R}=0$ in eq 3.5 and when $C_{g \infty}-C_{g R}$ is negative:

$$
\begin{equation*}
t=\frac{R_{0}{ }^{2} \rho_{g}}{2 D\left(C_{g R}-C_{g \infty}\right)} \tag{3.6}
\end{equation*}
$$

The diffraction coefficient $D_{g}$ is close to $2 * 10^{-9} \mathrm{~m}^{2} / \mathrm{sec}$.

An example can give a rough idea about time scales. Consider a bubble with a diameter of 100 microns ( $R=0.5 * 10^{-} 5 \mathrm{~m}$ ) in water at atmospheric pressure with a saturation rate of $50 \%$. The saturation rate of the water at the bubble wall will be $100 \%$. The concentration gradient is then estimated as $1.5 * 10^{-2} \mathrm{~kg} / \mathrm{m}^{3}$ and with $\rho_{g}=1$ this means that $\frac{\left(C_{g \infty}-C_{g R}\right)}{\rho_{g}}=-1.5 * 10-2$. From eq. 3.6 it follows that the time for the bubble to dissolve is 41 seconds. When submerged at 1 m below the surface, such a bubble will not reach the surface (at $5 \mathrm{~mm} / \mathrm{sec}$ ), but go into solution. At a time $t=41$ the term
$(\pi D t)^{1 / 2}$ is $5 * 10^{-} 4$, which is still an orders of magnitude larger than the initial radius $R_{0}=5^{-5}$. It is therefore justified to neglect this term in eq 3.4 .

Surface tension will reduce this time for a bubble to dissolve, but these approximations can be used to determine a time scale. It follows that the diffusion rate is low when compared to the time scale of bubble dynamics in a flow. However, when the existence of gas bubbles in a fluid is considered, small bubbles will tend to go into solution.

### 3.4 Mechanisms to sustain nuclei

From the foregoing it is still unexplained why there are so many nuclei in water. One mechanism that can keep nuclei in the water without rising to the surface is the combination of gas and solid particles. For that mechanism we have to consider the surface tension of a fluid. The difference in bond between cohesion between the water molecules and adhesion between water and air molecules causes surface tension. The cohesion attracts the molecules at a free surface and prevent these molecules to mix with the air. The result is also a tension on the surface molecules, which curves the surface in the neighborhood of a solid wall. The surface tension makes that a small gas bubble tends to be spherical. The surface tension increases the pressure inside a spherical gas bubble with an amount of $2 s / R_{b} \mathrm{~Pa}$, in which $s$ is the surface tension and $R_{b}$ the bubble radius. The surface tension of water in contact with air at 15 degrees Celcius is 0.075 Nm and the sensitivity to the temperature is not very strong.

Consider again a nucleus of 0.1 mm diameter in a fluid of 1 bar $\left(10^{5} \mathrm{~Pa}\right)$. The pressure


Figure 3.1: Contact Angle
inside the bubble is higher than the surrounding pressure due to the surface tension. The difference is $0.15 / 10^{-} 4=1500 P a$. Note that this is of the same magnitude as the vapor pressure. When the bubble is only 10 microns in diameter the surface tension increases the pressure with 15000 Pa !. The surface tension will increase the diffusion of gas into the fluid and thus decrease the time required to go into solution and this is increasing with decreasing bubble size.

Surface tension also causes a contact angle at the interface of water-gas-solid. This contact angle depends on the molecular forces in the water, the gas (air) and the material. Two types of material can be distinguished. On hydrophobic surfaces the contact angle is larger than 90 degrees, and air bubbles have the tendency to stick to the surface. In hydrophilic surfaces the contact angle is smaller than 90 degrees and air bubbles have the tendency to detach from the surface (Fig. 3.1).

When the surface is not flat but has the shape of a crevice, the schematic model is as in Fig. 3.2,

The material in Fig 3.2 is hydrophobic. The pressure inside the gas bubble will be lower than in the water due to the surface tension. When the water is not saturated an equilibrium is possible where no net gas diffusion takes place and the bubble is stable. The density of the particle and bubble together can in principle be equal to water and the nucleus is stable. Note that this model was first used by Edmund Newton Harvey [16], a biologist


Figure 3.2: Gas Pocket in a Crevice
working on bioluminescence and interested in nuclei in blood.

Diffusion can also be prevented by a molecular skin on the surface of the nucleus, as was already assumed by Fox and Herzfeld in 1964 [14]. A variation on this assumption was used by Yount [50], who assumes a skin of surface active molecules that make the nucleus stable. Morch [38, [39] showed that gas could not only be present in crevices, as Harvey assumed, but also in slightly concave surfaces on solid particles and that the effective radius of these thin gas remains could be larger than the size of the solid particle.

Experiments have shown that solid particles are important for the tensile strength of water. Filtering of water delays cavitation inception and increases the tensile strength of the water [24]. But also pre-pressurization can strongly increase the tensile strength of water by driving the nuclei attached to the solid particles into solution before the low pressure occurs. Nuclei with an organic skin seem to be crushed at some pressure and thus can go into solution also.

### 3.5 Mechanisms to generate nuclei

As discussed in previous sections, diffusion and gravity will remove nuclei from water. How-
ever, in general there are still ample nuclei in regular tap water and also in sea water. At sea, the breaking of waves is a major source of bubbles in the water and the mixing effect of these waves and the related turbulence will prevent small nuclei to rise to the surface. Biological life in the water can also produce free gases and in combination with biological matter it can be a source of nuclei. Actually the tensile strength of sea water in prototype conditions is close to zero and cavitation inception will thus take place at the vapor pressure. //

In test facilities this is different. First of all the amount of organic or solid matter may be less in clean test facilities, but also the size of the nuclei required for inception is larger. And these larger nuclei are not always available in sufficient numbers. So in test facilities like cavitation tunnels and depressurized towing tanks the nuclei content is always a point of concern. Locations where nuclei are formed are low pressure regions in a flow, especially when sharp edges cause local flow separation. These edges may occur on a very small scale, such as on surface roughness.

### 3.6 Nuclei measurements

It is not easy to measure the size distribution of nuclei. These techniques will be discussed later. Measurements indicate that there are many small nuclei in water. Gates [15] compiled such measurements in his thesis and shown in Fig. 3.3. The size range of the nuclei measured is from 5 microns to 500 microns. The number of nuclei is expressed as the number density $N d$, which is the number of nuclei in a small small size range divided by the size range. Its unit is therefore $m^{-}$.
The range of number densities is between $10^{10}$ and $10^{14}$. It helps to get a feeling for those numbers. When the number density is $10^{12}$ and we consider nuclei in the range of $50-100$ microns (a size range of $50 * 10 *-6 m$ ) it means that there are $50 * 10^{-6} * 10^{12}=50 * 10^{6} \mathrm{nu}$ -


Figure 3.3: Nuclei densities
clei per cubic meter or, more imaginable, 50 nuclei per cubic centimeter. The average distance between the nuclei is then 2.5 mm . Fig. 3.3 also shows that this amount can easily vary with a factor 100 depending on the circumstances. Even when there are $50 * 10^{6}$ nuclei of in average 75 microns in diameter in $1 m^{3}$ of water, this means that there is a volume of $1.1 * 10^{-5} \mathrm{~m}^{3}$ of free gas per $m^{3}$ of water. In atmospheric conditions this is also $1.1 * 10^{-5} \mathrm{~kg}$ and this is the free air content in $1 \mathrm{~m}^{3}$. This is still only a third of the dissolved air content of $C=3 * 10^{-} 2 \mathrm{~kg} / \mathrm{m}^{3}$. In general the amount of free air will be (much) smaller then the amount of dissolved air. So when there is a mechanism to bring air out of solution and create bubbles, this will not immediately deplete the dissolved air content. It is also important to note that the dissolved air content has little or no effect on cavitation inception.

From Fig 3.3 it can be seen that the nuclei are predominantly small. These small nuclei can easily be transported through the fluid by
currents and water motions such as waves. But they would still dissolve over time. This seems to be significantly reduced by the presence of an organic skin on the surface of a nucleus. When the nuclei dissolve, the reduction of the radius makes the skin thicker and this ultimately stops the diffusion, making the nuclei stable.
Since in sea water ample nuclei are available not much attention has been given to their origin and presence. However, for model tests the required nuclei size is larger, as explained in chapter refchincept, and these nuclei are often scarce or not available in test facilities. This makes that nuclei distributions dominate the problem of scaling of cavitation inception and the mechanisms of dissolving and rising nuclei have to be considered when test facilities are used.

### 3.7 Bubble Screening

A phenomenon which is often observed is that cavitation does not take place in the minimum pressure location with a minimum pressure significantly below the vapor pressure. This occurs even in conditions with ample free nuclei in the incoming flow. Since this is observed spedifically in cases when the boundary layer is still laminar in hte minimum pressure region, it was suspected that this delay in inception was caused by a local lack of nuclei. It means that the incoming flow contains enough nuclei, but that they are inhibited to enter the low pressure region. The interpretation of what happens is only tentative because it is very difficult to verify experimentally. A possible explanation is The common explanation is that bubble screening occurs. In a pressure gradient nuclei experience a force, similar to the rising force in a gravitational field. Near the leading edge of a foil there is a strong pressure gradient along the foil surface, but also perpendicular to the wall outside the


Figure 3.4: Path of a Nucleus in the Pressure Field near the Leading Edge of a Foil
boundary layer (the pressure in a thin boundary layer is constant perpendicular to the wall). This pressure gradient perpendicular to the wall is is especially strong near the stagnation point and, in opposite direction, near the minimum pressure location. Near the stagnation point the pressure gradient will move the nuclei away from the wall. In the minimum pressure region the nuclei are moved towards the wall. As a result the path of the nuclei will not follow the streamlines, but follow a path away from the wall, as sketched in Fig 3.4. The path of the nuclei may thus avoid the minimum pressure close to the wall. The pressure gradient thus has a screening effect and this effect will be greater with increasing size of the nuclei.
Calculations of the path of nuclei were first made by Johnsson and Hsieh [22] in 1966, assuming a certain drag coefficient of nuclei and assuming that they remained spherical.

Although bubble screening is a plausible hypothesis, experimental evidence is difficult to obtain.

## Bibliography

[1] Arakeri,V.H., Acosta, A.J., 1979, Viscous Effects in the Inception of Cavitation, A.S.M.E. Int. Symposium on Cavitation, New York, USA.
[2] Arndt, R.E.A., 1976, Cavitation on Model Propellers with Boundary Layer Trips, A.S.M.E.Conference on Polyphase Flow, New Orleans, USA.
[3] Arndt, R.E.A., Ellis, C.R., Paul, S. 1995, Preliminary Investigation of the Use of Air Injection to mitigate Cavitation Erosion, A.S.M.E. Journal of Fluids Engineering, Vol. 117.
[4] Briggs, L.J., 1950 Limiting negative pressure of water., J. Applied Phys. 21:721722.
[5] Brennen, C.E., 1995 Cavitation and Bubble Dynamics, Oxford University Press, ISBN 0-19-509409-3. Also available on internet.
[6] Burrill, L.C., 1951, Sir Charles Parsons and Cavitation, Transactions of the Institute of Marine Engineers.
[7] Borkent, B.M., 2009, Interfacial Phenomena in Micro- and Nanofluidics: nanobubbles,cavitation, and wetting, Thisis Twente University, The Netherlands.
[8] Coutier-Delgosha, O., Devillers, J-P., Leriche, M., Pichon, T., 2005, emphEffect of Roughness on the Dynamics of Unsteady Cavitation, Journal of Fluids Eng. , vol 127.
[9] Epstein, P.S., Plesset, M.S. 1950 On the stability of Gas Bubbles in Liquis-Gas Solutions, Journal of Chemical Physics, Vol.18., pp1505-1509.
[10], Feindt, E.G., 1956, Untersuchungen uber die Abhangigkeit des Umschlages Laminar-Turbulent von der Oberflachenrauhigkeit und der Druckverteilung, Jahrbuch STG, Bd.50, pp180-205
[11] Flynn, H.G., 1964, Physics of Acoustic Cavitation, W.P.Mason ed. Vol1,PartB,Academic Press New YorkLondon.
[12] Foeth, E-J., Kuiper, G. 2004, Exploratory experiments to determine flow and structure borne noise of erosive cavity implosions, $\mathrm{A}_{j} \mathrm{~S}_{¡} \mathrm{M}_{¡} \mathrm{E}_{\dot{i}}$ Fluids Eng. Summer Conference, HT-FED200456789, Charlotte, NC. USA.
[13] Foeth, E-J., The Structure of ThreeDimensional Sheet Cavitation, Thesis Technical University Delft.
[14] Fox, F.E., Herzfeld, K.F., 1954 Gas Bubbles with Organic Skin as Cavitation Nuclei, J.Acoust. Soc. Am. Vol.26, pp 984989.
[15] Gates, E.M., 1977 ( The influence of FreeStream Turbulence, Free Stream Nuclei Populations and a Drag-reducing Polymer on Cavitation Inception on Two Axisymmetric Bodies California Institute of Technology, Rep. No. Eng 183-2.
[16] Harvey, E.N., McElroy, W.D., Whiteley, A.H., 1947 On Cavity Formation in Water, Journal of Applied Physics, Vol.18, pp162-172.
[17] Hoekstra, M., Vaz, G. The Paartial Cavity on a @D Foil Revisited, 7th Int. Conference on Cavitation CAV2009, Ann Arbor, Michigan, U.S.A.
[18] Holl, J.W., 1960, An Effect of Air Content on the Occurrence of Cavitation, Trans. A.S.M.E., Journal of Basic Eng. Vol.82, pp941-946.
[19] Holl, J.W., Carrol, J.A., 1981, Observations of the Various Types of Limited Cavitation on Axisymmetric Bodies, PUB A.S.M.E. Journal of Fluids Eng.,Vol 103,pp415-423
[20] Huang, T.T., 1981, Cavitation Inception Observations on Six Axisymmetric Headforms, A.S.M.E. Journal of Fluids Engineering, Vol 103,PP273-278
[21] ITTC, 1978,Proceedings 15th ITTC, The Haque, Report of the Performance Committee.
[22] Johnsson, C.A., Hsieh,T., 1966, The Influence of Trajectories of Gas Nuclei on Cavitation Inception, 6th Symposium on Naval Hydrodynamics, Washington D.C., pp163-178.
[23] Takagi,K., Kato,H.,Kato,D.,Sugimoto, A., 2006, Destruction of Plankton by Two-Dimensional Cavitating Jet, Sixth International Symposium on Cavitation CAV2006, Wageningen, The Netherlands.
[24] Keller, A.P., 1974 Investigations Concerning Scale Effects of the Inception of Cavitation, Proc. I.Mech.Eng. Conference on Cavitation, Edinburgh, 109-117.
[25] KLEBANOFF, P.S., SCHUBAUER, G.B., TIDSTROM,K.D., 1955, Measurements of the Effect of Two-dimensional and Three-dimensional Roughness Elements on Boundary Layer Transition, J. Aeron. Sciences
[26] Knapp, R.T., Hollander, A., 1948, Laboratory Investigations of the Mechanism of Cavitation, Trans. A.S.M.E., Vol.70, pp.419-435.
[27] Knapp, R.T., Daily, J.W., Hammitt, F.G., 1970, Cavitation, New York : McGraw-Hill.
[28] Knapp, R.T., Hollander, A., 1948, Laboratory Investigations of the Mechanism of Cavitation, Trans. A.S.M.E., Vol 70, pp419-435.
[29] Korkut, E., Atlar, M., 2000, On the Importance of Effect of Turbulence in Cavitation Inception Tests of Marine Propellers, Proceedings of Royal Society of London A: Mathematical, Physical and Engineering Sciences, Vol.458, pp.29-48.
[30] Kreider, W., Crum, L., Bailey,M., Matula, T.,Khoklova, V., Sapozhnikov,O., 2006, Acoustic Cavitation and Medical Ultrasound,Sixth International Symposium on Cavitation CAV2006, Wageningen, The Netherlands.
[31] Kumar, S., Brennen, C.E., 1996, A Study of Pressure Pulses generated by Travelling Bubble Cavitation, Journal of Fluid Mechanics Vol 255 pp541.
[32] Hwansung Lee, Tomonori Tsukiya, Akihiko Homma, Tadayuki Kamimura,Eisuke Tatsumi, Yoshiyuki Taenaka, Hisateru Takano, Observation of Cavitation in a Mechanical Heart Valve, Fifth International Symposium on Cavitation (cav2003), Osaka, Japan.
[33] Kuiper, G., 1978, Scale Effects on Propeller Cavitation, 12th Symposium on Naval Hydrodynamics, Washington D.C., USA.
[34] Kuiper, G. 1981, Cavitation Inception on Ship Propeller Models, Thesis Technical University Delft.
[35] Kuiper, G. 2008, Fundamentals of Ship Resistance and Propulsion, Course Lectures Technical University Delft.
[36] Landa, E.R., Nimmo, J.R., 2003 The Life and Scientific Contributions of Lyman J. Briggs, Journal of the Soil Science Society of America, Vol 67 no 3, pp 681-693.
http://soil.scijournals.org/cgi/reprint/67/3/681
[37] Ligtelijn, J.T., van der Kooij, J., Kuiper, G., van Gent,W., 1992, Research on Propeller-Hull Interaction in the Depressurized Towing Tank, Hydrodynamics, Computations,Model Tests and Reality (Marin ), Elseviers Science Publishers.
[38] Morch E.M., 2000, Paper on Cav2003.
[39] Moerch, K.A. 2009, Cavitation Nuclei: Experiment and Theory,Journal of Hydrodynamics Vol21 p176.
[40] Neppiras, E.A., Noltink, B.E., 1951, Cavitation produced by Ultrasonics, Proc. Phys. Soc. London, pp 1032-1038.
[41] Ohl, C-D., Arora, M. ,Roy, I., Delius. M., Wolfrum, B.,2003, Drug Delivery Following Shock Wave Induced Cavitation, Fifth International Symposium on Cavitation (cav2003),Osaka, Japan.
[42] Plesset, M.S., 1949, The Dynamics of Cavitation Bubbles, ASME Journal of Appl. Mech. 1949, pp 277-232.
[43] Schiebe, F.R., 1972, Measurement of the Cavitation Susceptibility of Water using

Standard Bodies, St. Anthony Fall Hydraulic Lab, Univ. of Minnesota, report 118.
[44] Schlichting, H., 1968, Boundary Layer Theory, McGraw-Hill, 6th edition.
[45] Terwisga, T.J.C., Fitzsimmons, P.A., Li,Z., Foeth, E-J. Cavitation Erosion-A review of Physical Mechanisms and Erosion Risk Models, 7th International Symposium on Cavitation, CAV2009, Ann Arbor, Michigan, U.S.A.
[46] Jin Wang, 2009, Nozzle-geometrydependent breakup of diesel jets by ultrafast $x$-ray imaging: implication of in-nozzle cavitation, Seventh Int. Symp. on Cavitation: CAV2009, Ann Arbor, Michigan, U.S.A.
[47] Watanabe, S., Furukawa, A., Yoshida, Y., Tsujimoto, Y., 2009, Analytical investigations of thermodynamic effect on cavitation characteristics of sheet and tip leakage vortex cavitation, Seventh Int. Symp. on Cavitation: CAV2009, Ann Arbor, Michigan, USA.
[48] Williams,M., Kawakami, E., Amromin, E., Arndt,R. Effects of Surface Characteristics on Hydrofoil Cavitation, Seventh Int. Symp. on Cavitation: CAV2009, Ann Arbor, Michigan, USA.
[49] Yoshimura,T., Kubota, S., Seo, T., Sato,K., 2009, Development of Ballast Water Treatment Technology by Mechanochemical Cavitations,Seventh Int. Symp. on Cavitation: CAV2009, Ann Arbor, Michigan, USA.
[50] Yount, D.E. 1979, Skins of Varying Permeability: A Stabilization Mechanism For Gas Cavitation Nuclei,A. ACCOUST. SOC. AM. 65(6).

## Appendix A

## Air Content of Water

The amount of air dissolved in water $\alpha$ can be expressed in many ways. The most common ways in literature are

- the gas fraction in weight ratio $\alpha_{w}$
- the gas fraction in volume ratio $\alpha_{v}$
- the molecule ratio
- the saturation rate
- the partial pressure of air


## A. 1 Solubility

Air is a mixture of 21 percent oxygen, 78 percent nitrogen and one percent of many other gases, which are often treated as nitrogen. The specific mass of gases involved in air are:

| Oxygen $\left(O_{2}\right)$ | 1.429 | $\mathrm{~kg} / \mathrm{m}^{3}$ |
| :--- | :--- | :--- |
| Nitrogen $\left(N_{2}\right)$ | 1.2506 | $\mathrm{~kg} / \mathrm{m}^{3}$ |
| Air | 1.292 | $\mathrm{~kg} / \mathrm{m}^{3}$ |

The maximum amount of gas that can be dissolved in water, the solubility), depends on pressure and temperature. It decreases with increasing temperature and increases with increasing pressure. The solubility of oxygen in water is higher than the solubility of nitrogen. Air dissolved in water contains approximately 36 percent oxygen compared to 21 percent in air.The remaining amount can be considered as Nitrogen. Nuclei which are in equilibrium
with saturated water therefore contain 36 percent oxygen. But nuclei which are generated from the air above the water contain 21 percent oxygen. Since the ratio between oxygen and nitrogen is not fixed, it is difficult to relate measurements of dissolved oxygen (by osmose) to measurements of dissolved air (from e.g a van Slijke apparatus).

The amount of oxygen dissolved in water at atmospheric pressure at 15 degrees Celcius is approximately $10 * 10^{-} 6 \mathrm{~kg} / \mathrm{kg}$. For nitrogen this value is about $15 * 10^{-} 6$, so the solubility of air in water is the sum of both: $25 * 10^{-} 6$. Here the dissolved gas contents are expressed as a weigth ratio $\alpha_{w}$. Air is very light relative to water and the weight ratio is very small. This ratio is therefore often expressed as parts per million (in weight), which is $10^{6} * \alpha_{w}$.

## A. 2 The Gas Fraction in Volume Ratio

The volume of gas dissolved per cubic meter of water depends on temperature and pressure. Therefore this volume ratio is expressed in standard conditions of 0 degrees Celcius and 1013 mbar (atmospheric conditions). The dependency of the volume of water on temperature and pressure is neglected. The volume of the dissolved air is then described by the law of Boyle-Gay-Lussac:

$$
\begin{equation*}
\frac{p * V o l}{273+T}=\text { constant } \tag{A.1}
\end{equation*}
$$

The volume fraction at ( $\mathrm{p}, \mathrm{T}$ ) can be related to the volume fraction in standard conditions:

$$
\begin{equation*}
\alpha_{v}=\alpha_{v}(p, T) \frac{273 p}{(273+T) 1013} \tag{A.2}
\end{equation*}
$$

The gas fraction in volume ratio is dimensionless $\left(m^{3} / m^{3}\right)$. Be careful because sometimes this is violated by using $\mathrm{cm}^{3} / l\left(1000 * \alpha_{v}\right)$ or parts per million ( ppm ) which is $10^{6} * \alpha_{v}$.
$\alpha_{v}$ is found from $\alpha_{w}$ by:

$$
\begin{equation*}
\alpha_{v}=\frac{\rho_{\text {water }}}{\rho_{\text {air }}} \alpha_{w} \tag{A.3}
\end{equation*}
$$

in which $\rho$ is the specific mass in $\mathrm{kg} / \mathrm{m}^{3}$. At 15 deg. Celcius and 1013 mbar pressure the specific mass of water $\rho_{w}=1000 \mathrm{~kg} / \mathrm{m}^{3}$ and the specific mass of air is $1.223 \mathrm{~kg} / \mathrm{m}^{3}$, so for air $\alpha_{v}=813 \alpha_{w}$.

## A. 3 The Gas Fraction in Molecule ratio

The dissolved amount of gas can also be expressed as the ratio in moles $(\mathrm{Mol} / \mathrm{Mol})$. Molar masses may be calculated from the atomic weight in combination with the molar mass constant ( $1 \mathrm{~g} / \mathrm{mol}$ ) so that the molar mass of a gas or fluid in grams is the same as the atomic weight.
The molar ratio $\alpha_{m}$ is easily found from the weight ratio by

$$
\begin{equation*}
\alpha_{w}=\alpha_{m} \frac{M_{(\text {water })}}{M_{(\text {gas })}} \tag{A.4}
\end{equation*}
$$

in which M is the molar weight, which is 18 for water, 16 for oxygen $\left(O_{2}\right)$ and 28 for Nitrogen $\left(N_{2}\right)$. For air a virtual molar weigth can
be defined using the ratio of oxygen and nitrogen of $21 / 79$ this virtual molar weight of air is about 29 .

## A. 4 The saturation rate

The saturation rate is the amount of gas in solution as a fraction of the maximum amount that can go in solution in the same conditions. Since the saturation rate is dimensionless. It is independent of the way in which the dissolved gas or the solubility is expressed. The saturation rate is important because it determines if and in which direction diffusion will occur at a free surface. The saturation rate varies with temperature and pressure, mainly because the solubility of gas changes with these parameters.

## A. 5 The partial pressure

Sometimes the amount of dissolved gas is expressed as the partial pressure of the gas (mbar or even in mm HG). This is based on Henry's law, which states that the amount of gas dissolved in a fluid is proportional to the partial pressure of that gas. In a van Slijke apparatus a specific volume of water is taken and subjected to repeated spraying in near vacuum conditions (a low pressure decreases the solubility). This will result in collecting the dissolved in a chamber of specific size. By measuring the pressure in that chamber the amount of dissolved gas is found. Note that this pressure is not directly the partial pressure. A calibration factor is required which depends on the apparatus.

## Appendix B

## Standard Cavitators

A standard cavitator is a reference body which can be used to compare and calibrate cavitation observations and measurements. Its geometry has to be reproduced accurately and therefore an axisymmetric headform has been used as a standard cavitatior.

Such an axisymmetric body has been investigated in the context of the ITTC (International Towing Tank Conference).This is a worldwide conference consisting of towing tanks (and cavitation tunnels) which have the goal of predicting the hydrodynamic behavior of ships. To do that model tests and calculations are used. They meet every three years to discuss the state of the art and to define common problem areas which have to be reviewed by committees. The ITTC headform has a flat nose and an elliptical contour [22]. Its characteristics are given in Fig B.1.

This headform has been used to compare cavitation inception conditions and cavitation patterns in a range of test facilities. The results showed a wide range of inception conditions and also a diversity of cavitation patterns in virtually the same condition, as illustrated in Fig B.3. This comparison lead to the investigation of viscous effects on cavitation and cavitation inception.

The simplest conceivable body to investigate cavitation is the hemispherical headform. This is an axisymmetric body with a hemispere as the leading contour. Its minimum pressure coefficient is -0.74 . The hemisperical


Figure B.1: Contour and Pressure Distribution on the ITTC Headform 31]
headform was used to compare inception measurements in various cavitation tunnels. However, it was realized later on that the boundary layer flow on both the ITTC and on the hemisperical headform was not as simple as the geometry suggested. In most cases the Reynolds numbers in the investigations was such that the boundary layer over the headform remained laminar and the pressure distribution was such that a laminar separation bubble occurred, in the position indicated in Fig. B.1. This caused viscous effects on cavitation inception and made the headform less suitable as a standard body. Note that the location of laminar separation is independent of the Reynolds number. When the Reynolds number becomes high transition to turbulence occurs upstream of the sep-


Figure B.2: Contour and Pressure Distribution of the Schiebe body [31]
aration location and separation will disappear.
To avoid laminar separation another headform was developed by Schiebe ([43) and this headform bears his name ever since. The contour and pressure distribution on the Schiebe headform are given in Fig. B.2. This headform has no laminar separation and transition to a turbulent boundary layer will occur at a location which depends on the Reynolds number.

Many other headform shapes have been investigated with different minimum pressure coefficients and pressure recovery gradients.(e.g.[20])


Figure B.3: Comparative measurements of cavitation inception on the ITTC headform source:ITTC

## Appendix C

## Tables

| T <br> Celcius | $p_{v}$ <br> $N / m^{2}$ |
| :---: | :---: |
| 0 | 608.012 |
| 2 | 706.078 |
| 4 | 813.951 |
| 6 | 932 |
| 8 | 1069 |
| 10 | 1226 |
| 12 | 1402 |
| 14 | 1598 |
| 15 | 1706 |
| 16 | 1814 |
| 18 | 2059 |
| 20 | 2334 |
| 22 | 2638 |
| 24 | 2981 |
| 26 | 3364 |
| 28 | 3785 |
| 30 | 4236 |
| 32 | 4756 |
| 34 | 5315 |
| 36 | 5943 |
| 38 | 6619 |
| 40 | 7375 |

Table C.1: Vapor pressure of Water.

| Temp. <br> deg. C. | kinem. visc. <br> fresh water <br> $m^{2} /$ sec $\times 10^{6}$ | kinem. visc. <br> salt water <br> $m^{2} /$ sec $\times 10^{6}$ |
| :---: | :---: | :---: |
| 0 | 1.78667 | 1.82844 |
| 1 | 1.72701 | 1.76915 |
| 2 | 1.67040 | 1.71306 |
| 3 | 1.61665 | 1.65988 |
| 4 | 1.56557 | 1.60940 |
| 5 | 1.51698 | 1.56142 |
| 6 | 1.47070 | 1.51584 |
| 7 | 1.42667 | 1.47242 |
| 8 | 1.38471 | 1.43102 |
| 9 | 1.34463 | 1.39152 |
| 10 | 1.30641 | 1.35383 |
| 11 | 1.26988 | 1.31773 |
| 12 | 1.23495 | 1.28324 |
| 13 | 1.20159 | 1.25028 |
| 14 | 1.16964 | 1.21862 |
| 15 | 1.13902 | 1.18831 |
| 16 | 1.10966 | 1.15916 |
| 17 | 1.08155 | 1.13125 |
| 18 | 1.05456 | 1.10438 |
| 19 | 1.02865 | 1.07854 |
| 20 | 1.00374 | 1.05372 |
| 21 | 0.97984 | 1.02981 |
| 22 | 0.95682 | 1.00678 |
| 23 | 0.93471 | 0.98457 |
| 24 | 0.91340 | 0.96315 |
| 25 | 0.89292 | 0.94252 |
| 26 | 0.87313 | 0.92255 |
| 27 | 0.85409 | 0.90331 |
| 28 | 0.83572 | 0.88470 |
| 29 | 0.81798 | 0.86671 |
| 30 | 0.80091 | 0.84931 |
|  |  |  |

Table C.2: Kinematic viscosities adopted by the ITTC in 1963

| $R_{n}$ | $C_{f} \times 10^{3}$ |
| :--- | :---: |
| $1 \times 10^{5}$ | 8.333 |
| 2 | 6.882 |
| 3 | 6.203 |
| 4 | 5.780 |
| 5 | 5.482 |
| 6 | 5.254 |
| 7 | 5.073 |
| 8 | 4.923 |
| 9 | 4.797 |
| $1 \times 10^{6}$ | 4.688 |
| 2 | 4.054 |
| 3 | 3.741 |
| 4 | 3.541 |
| 5 | 3.397 |
| 6 | 3.285 |
| 7 | 3.195 |
| 8 | 3.120 |
| 9 | 3.056 |
| $1 \times 10^{7}$ | 3.000 |
| 2 | 2.669 |
| 4 | 2.390 |
| 6 | 2.246 |
| 8 | 2.162 |
| $1 \times 10^{8}$ | 2.083 |
| 2 | 1.889 |
| 4 | 1.721 |
| 6 | 1.632 |
| 8 | 1.574 |
| $1 \times 10^{9}$ | 1.531 |
| 2 | 1.407 |
| 4 | 1.298 |
| 6 | 1.240 |
| 8 | 1.201 |
| $1 \times 10^{10}$ | 1.17 x |
|  |  |

Table C.3: Friction coefficients according to the ITTC57extrapolator.

| Temp. <br> deg. C. | density <br> fresh water <br> $k g / m^{3}$ | density <br> salt water <br> $\mathrm{kg} / \mathrm{m}^{3}$ |
| :---: | :---: | :---: |
| 0 | 999.8 | 1028.0 |
| 1 | 999.8 | 1027.9 |
| 2 | 999.9 | 1027.8 |
| 3 | 999.9 | 1027.8 |
| 4 | 999.9 | 1027.7 |
| 5 | 999.9 | 1027.6 |
| 6 | 999.9 | 1027.4 |
| 7 | 999.8 | 1027.3 |
| 8 | 999.8 | 1027.1 |
| 9 | 999.7 | 1027.0 |
| 10 | 999.6 | 1026.9 |
| 11 | 999.5 | 1026.7 |
| 12 | 999.4 | 1026.6 |
| 13 | 999.3 | 1026.3 |
| 14 | 999.1 | 1026.1 |
| 15 | 999.0 | 1025.9 |
| 16 | 998.9 | 1025.7 |
| 17 | 998.7 | 1025.4 |
| 18 | 998.5 | 1025.2 |
| 19 | 998.3 | 1025.0 |
| 20 | 998.1 | 1024.7 |
| 21 | 997.9 | 1024.4 |
| 22 | 997.7 | 1024.1 |
| 23 | 997.4 | 1023.8 |
| 24 | 997.2 | 1023.5 |
| 25 | 996.9 | 1023.2 |
| 26 | 996.7 | 1022.9 |
| 27 | 996.4 | 1022.6 |
| 28 | 996.2 | 1022.3 |
| 29 | 995.9 | 1022.0 |
| 30 | 995.6 | 1021.7 |
|  |  |  |

Table C.4: Densities as adopted by the ITTC in 1963.

## Appendix D

## Nomenclature

$\rho \quad$ density of water
$C_{g} \quad$ gas concentration
$D_{g}$ diffusion coefficient
D diameter
$F_{d}$ drag
$g \quad$ acceleration due to gravity
$N d \quad$ number density of nuclei
$p_{g} \quad$ gas pressure
fracNm ${ }^{2}$
$p_{v} \quad$ equilibrium vapor pressure
R radius
$\mu \quad$ dynamic viscosity of water
$\nu \quad$ kinematic viscosity of water
$s \quad$ surface tension
$\frac{k g}{m^{3}}$
$\mathrm{kg} / \mathrm{m}^{3}$
$m^{2} / \mathrm{sec}$
$m$
$N$
$\frac{m}{s^{2} c^{2}}$
$m^{-4}$
fracNm ${ }^{2}$
$m$
$\frac{\mathrm{kg}}{m^{m} \sec }$
$\frac{m^{2}}{\mathrm{sec}}$
sec
Nm

See TableC. 4
see Appendix A
representative value $2 * 10_{9}$

Taken as 9.81
$\left(\nu=\frac{\mu}{\rho}\right)$ See Table C. 2
for water 0.075

