

## Unsteady Conduction Probs, Pt. 1

1. a) From Eq. 11.1-10,  $q_s = \frac{k}{\sqrt{\pi \alpha t}} (T_i - T_o)$ . Using SI units given, we will get answer in J/m<sup>2</sup>s (W/m<sup>2</sup>). Can either convert to "days" at start or at end. Let  $t$  [sec],  $t'$  [days]  
 If stay with SI units until end,  $q_s = (0.99) / [\pi (\frac{0.99}{2320(761)}) t]^{1/2} \cdot [\frac{300-150}{1.8}] = 6.22 \cdot 10^4 t^{-1/2}$  W/m<sup>2</sup>.  
 $Q = (10,000) q_s = 6.22 \cdot 10^8 t^{-1/2}$  W; but since  $t$  is in sec here & we want days,  
 $Q = (6.22 \cdot 10^8) (t' [(24)(3600)])^{-1/2} = 2.11 \cdot 10^6 (t')^{-1/2}$  in watts, with  $t$  expressed in days. If instead of watts (joules/sec) we want units of (joules/day), then  $Q = 1.82 \cdot 10^{11} (t')^{-1/2}$  J/day.  
 If instead were to convert all time units to days at start, then  $k = (0.99)(8.64 \cdot 10^4)$  (J/mK day);  
 $q_s = (8.55 \cdot 10^4) / [\pi (\frac{8.55 \cdot 10^4}{2320(761)} t')^{1/2}] = (\frac{300-150}{1.8}) = 1.83 \cdot 10^7 (t')^{-1/2}$  J/(m<sup>2</sup>d),  $t'$  expressed in days.  
 $Q = (10,000)(1.83 \cdot 10^7 (t')^{-1/2}) = 1.83 \cdot 10^{11} (t')^{-1/2}$  (J/d),  $t$  expressed in days.

- b) For part b it is much easier to begin with  $Q$  in terms of days ( $t'$ ). Then  
 Cum heat loss at any time  $t^* = \int_0^{t^*} Q(t') dt' = 1.83 \cdot 10^{11} (t')^{-1/2} dt' = 1.83 \cdot 10^{11} (t'^{-1/2})(2) \Big|_0^{t^*}$   
 $= 3.66 \cdot 10^{11} (t^*)^{1/2}$ ,  $t^*$  expressed in days.  
 If one used  $Q(t)$  instead, cum heat loss  $= \int_0^{t^*} (6.22 \cdot 10^8) t^{-1/2} dt$  with both  $t^{-1/2}$  in sec<sup>-1/2</sup>  
 and  $t$  in (sec).  $\rightarrow$   $= (6.22 \cdot 10^8)(2) t^{1/2}$  with heat loss in J and  $t$  in sec.  
 $= 3.66 \cdot 10^{11} t^{1/2}$  with  $t$  expressed in days.

2.  $y = 0.05$  m      $\alpha = k / (\rho \hat{c}_p)$       $k = 0.346$  W/cm°C = 34.6 W/(mK)  
 $\rho = 11.34$  g/cm<sup>3</sup> = 11,340 Kg/m<sup>3</sup>      $\hat{c}_p = 0.031$  cal/(g°C) = 130 J/(KgK)  
 $\rightarrow \alpha = (34.6) / [(11,340)(130)] = 2.35 \cdot 10^{-5}$   
 $y / \sqrt{4 \alpha t} = 0.05 / [4(2.35 \cdot 10^{-5})(60)]^{1/2} = 0.67$   
 From figure handed out in class,  $y / \sqrt{4 \alpha t} = 0.67 \rightarrow \frac{T-100}{300-100} = 0.17$   
 $T = 134^\circ \text{F}$ .

3. a) For these rock properties,  $\alpha = k / (\rho \hat{c}_p) = (0.99) / (2320 \cdot 761) = 5.61 \cdot 10^{-7}$  m<sup>2</sup>/s  
 $r_{\text{well}} = [(4.5) / 12] [(3048)] = 0.1143$       $t = (2)(24)(60)^2 = 1.73 \cdot 10^5$   
 Fig 42 of Carslaw + Jaeger applies.  
 $\log_{10} [\alpha t / r_{\text{well}}^2] = \log_{10} [(5.61 \cdot 10^{-7})(1.73 \cdot 10^5) / (0.1143)^2] = \log_{10} (7.42) = 0.87$   
 My best reading of Fig 42 is  $\log_{10} [(r_{\text{well}} q_{\text{well}}) / (k(T_{\text{well}} - T_o))] = -0.25$   
 $\frac{(0.1143) q_{\text{well}}}{(0.99)(-200/1.8)} = 0.56 \rightarrow q_{\text{well}} = -540$  W/m<sup>2</sup>  
 (The negative sign is because  $q_{\text{well}}$  is really  $q_r$  ( $r=r_{\text{well}}$ ); since the heat flux is inward, in the negative  $r$  direction,  $q_{\text{well}} < 0$ .)  
 The heat transfer/unit depth =  $(2\pi r) q_{\text{well}} = 2\pi(0.1143)(-540) = -390$  W/m.

- b)  $\alpha = k / (\rho \hat{c}_p) = (0.658) / [(983)(4181)] = 1.60 \cdot 10^{-7}$   
 We want time for  $(T - T_o) / (T_i - T_o) = 0.75$  at  $r/R = 0$ . Fig 11-2 applies.  
 My best guess is that  $\alpha t / R^2 \approx 0.34 \rightarrow t = (0.34)(0.1143)^2 / (1.60 \cdot 10^{-7})$   
 $t = 2.77 \cdot 10^4$  s  $\approx 7$  hr 42 min.

~~Prob 27.8 Transport P57 Soln~~

Unsteady Conduction Probs, Pt 2

1. This problem uses the "product method" and 3 applications of Fig 11.1-1.

$$\alpha = k/\rho \hat{c}_p = 2.61 / ((2270)(1000)) = 1.15 \cdot 10^{-6} \text{ m}^2/\text{s}; \quad t = 6 (3600) = 2.16 \cdot 10^4 \text{ sec.}$$

For short dimension,  $\alpha t / b^2 = (1.15 \cdot 10^{-6})(2.16 \cdot 10^4) / (0.25)^2 = 0.40$ . From Fig 11.1-1,  $(T_1 - T) / (T_1 - T_0) \approx 0.48$

For long dimension,  $\alpha t / b^2 = (1.15 \cdot 10^{-6})(2.16 \cdot 10^4) / (0.5)^2 = 0.10$ . From Fig 11.1-1,  $(T_1 - T) / (T_1 - T_0) \approx 0.95$ .

For rectangular solid,  $(T_1 - T) / (T_1 - T_0) = (0.48)(0.95)^2 = 0.43$ .  $T \approx 220^\circ \text{ F}$ .

2. We want  $(\frac{T_1 - T}{T_1 - T_0})_{\text{cube}} = \frac{-20}{-100} = 0.2$  at the center. Because the block is cubical,

$$\left(\frac{T_1 - T}{T_1 - T_0}\right)_{\text{cube}} = \left(\frac{T_1 - T}{T_1 - T_0}\right)_{\text{slab}}^3 \quad \text{or} \quad \left(\frac{T_1 - T}{T_1 - T_0}\right)_{\text{slab}} = (0.2)^{1/3} = 0.58. \quad \frac{T_1 - T}{T_1 - T_0} = 0.58 \text{ at } \frac{y}{b} = 0$$

for  $\alpha t / b^2 \approx 0.32$ .  $\alpha = 2.61 / [(2270)(1000)] = 1.15 \cdot 10^{-6} \text{ m}^2/\text{s}$ ;  $b = 0.5$

$$t = (0.32)(0.5)^2 / (1.15 \cdot 10^{-6}) = 6.96 \cdot 10^4 \text{ sec (about 19 hr, 20 min)}$$

One side is insulated; therefore this is equivalent to a slab temporarily heated on both sides with width 0.2 m (i.e.,  $b=0.1$  m).

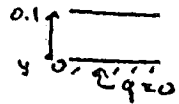
75 min = 4500 s.  $\alpha = k/\rho c_p = (1.21)/[3010(850)] = 4.57 \cdot 10^{-7} \text{ m}^2/\text{s}$

The solution to this problem is

$\frac{T-T_0}{T_1-T_0} \equiv \Theta = \Theta_1(y, t) - \Theta_1(y, t-t_1)$ , where, more precisely, we are interested in  $\Theta$  at  $y=0$ .

At  $t_1 = 75 \text{ min} = 4500 \text{ s}$ ,  $\alpha t_1/b^2 \approx 0.2$

For  $t < 75 \text{ min}$ , we can pull data directly off Fig 12-1



$\frac{\alpha t}{b^2}$	$t$	$\frac{T-T_0}{T_1-T_0}$	$T$
0.04	875 (14 1/2 min)	0	0°C
0.1	2190 36 1/2 min	0.05	5°C
0.2	4380 73 min	0.23	23°C

For  $t > 75 \text{ min}$ , both terms must be included.

For  $\alpha t/b^2 = 0.4$ ,  $\Theta_1(t) \approx 0.53$ ; Since  $\alpha t_1/b^2 \approx 0.2$ , then

$\alpha [t-t_1]/b^2 \approx \alpha t/b^2 - 0.2$ . Thus when  $\alpha t/b^2 = 0.4$ ,

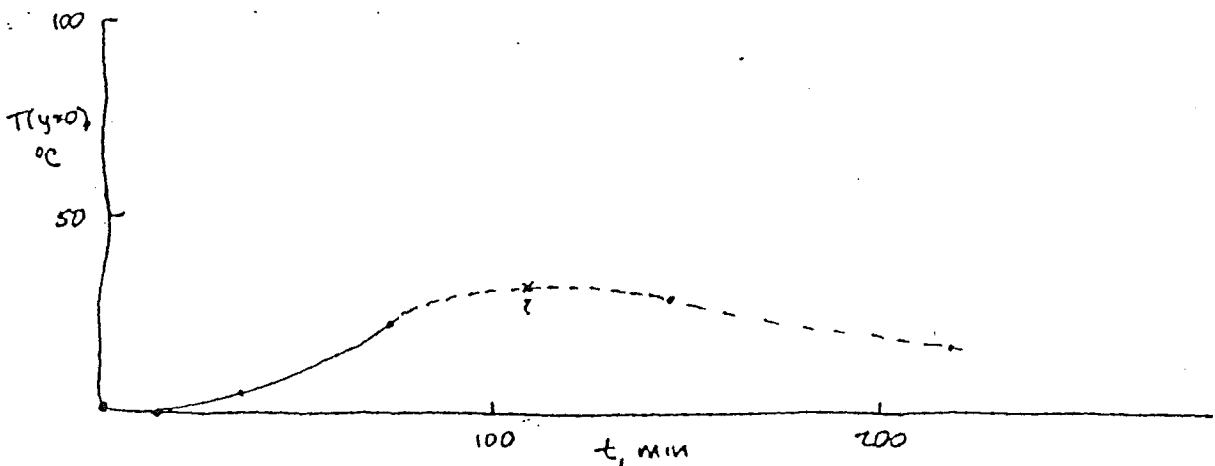
$\alpha [t-t_1]/b^2 = 0.2$ ;  $\Theta_1(t-t_1) \approx 0.23$ .  $\Theta = 0.53 - 0.23 \approx 0.3$ .  $T = 30^\circ\text{C}$ .

This time corresponds to  $t = 0.4 b^2/\alpha = 8760 \text{ sec}$  or 146 min.

For  $\alpha t/b^2 = 0.6$ ,  $\Theta_1(t) \approx 0.71$ ;  $\Theta_1(t-t_1) = \Theta_1(\frac{\alpha t}{b^2} = 0.4) \approx 0.53$ .

$\Theta = 0.71 - 0.53 = 0.18$ ;  $T = 30^\circ\text{C}$ .  $t = (0.6) b^2/\alpha = 13,130 \text{ s} = 219 \text{ min}$ .

A rough plot of these results gives



Getting more precise is difficult because there are so few lines on Fig 12-1.

I might guess that at  $\alpha t/b^2 = 0.3$ ,  $\Theta_1(t) = 0.38$ ,  $\Theta_1(t-t_1) = \Theta_1(\frac{\alpha t}{b^2} = 0.1) \approx 0.05$

$\rightarrow \Theta \approx 0.38 - 0.05 = 0.33$ . This corresponds to  $t = 0.5 b^2/\alpha = 6570 \text{ s} \approx 109 1/2 \text{ min}$

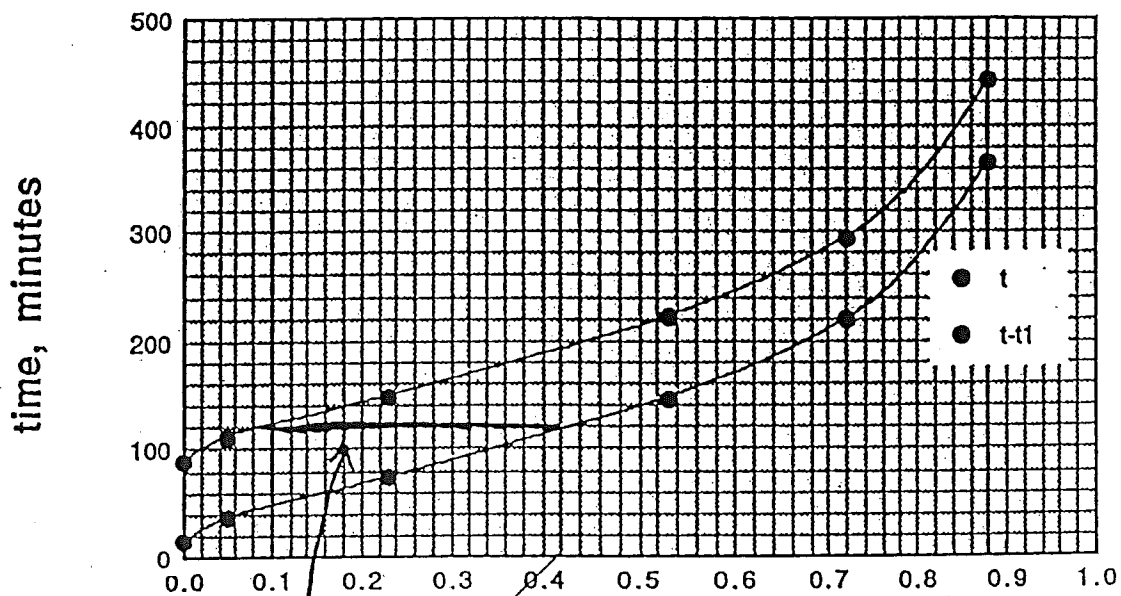
I would guess max  $T$  is between 30 and 35°C, occurring between about 100 and 130 min.

Another, possibly better way to plot the results is as follows. Plot  $\Theta_1(y, t)$  and  $\Theta_1(y, t-t_1)$  on the same axes.  $\Theta$  is the difference between the two plots

$4k/b^2$	$t$ (sec)	$t$ (min)	$\Theta_1(y=0, t)$
$\leq 0.04$	5875	$14\frac{1}{2}$	0
0.1	2190	$36\frac{1}{2}$	0.05
0.2	4380	73	0.23
0.4	8750	146	0.53
0.6	13,130	219	0.72
1.0	21,880	365	0.88

$\Theta_1(y=0, t-t_1)$  is simply the same curve displaced by 75 min.

### Problem 4 solution



dimensionless temperature ( $\Theta_1(y=0), t$ )  
 Max of  $\Theta_1(t) - \Theta_1(t-t_1) \approx 0.34$

Since the maximum of  $\Theta(y=0, t) \equiv \Theta_1(0, t) - \Theta_1(0, t-t_1)$   
 $\approx 0.34 = \frac{T-T_0}{T_1-T_0} = \frac{T-0}{100-0}$

the maximum  $T$  at the center is  $34^\circ\text{C}$ .