

Iron removal at groundwater pumping station Harderbroek



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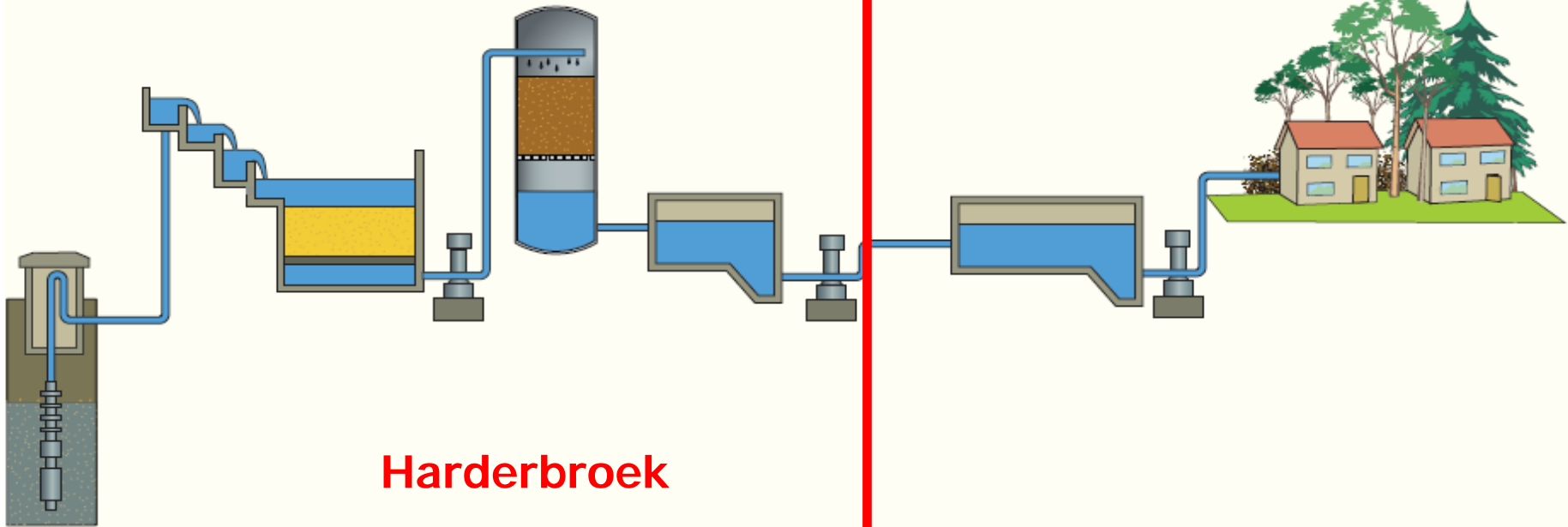
Conclusions and recommendations

HARDERBROEK

Drinking water supply Flevoland



Treatment scheme Harderbroek



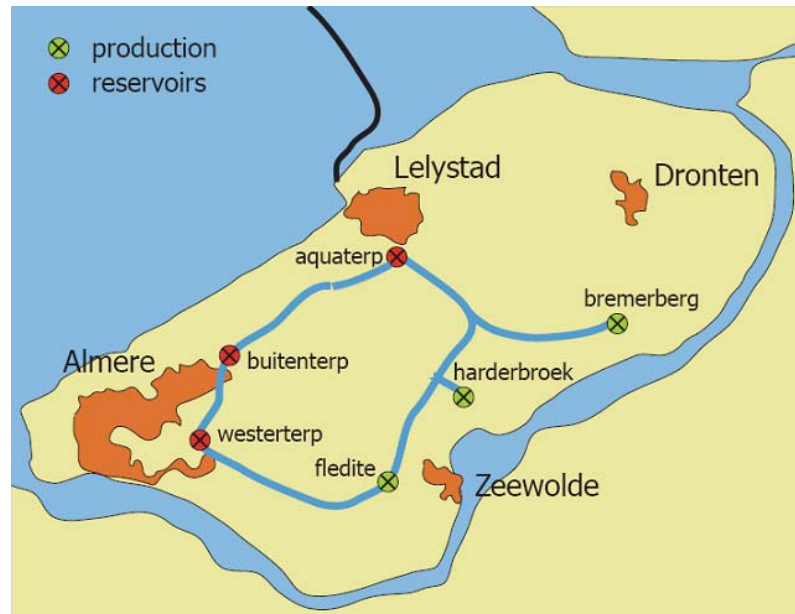
Harderbroek

IRON REMOVAL

Iron removal

Iron is removed to avoid iron deposits

- In distribution system
- In laundry
- In drinking water



Iron in groundwater

Fe^{2+}

- Present in anaerobic groundwater
- Dissolved in water



Fe^{3+}

- Forms iron flocks in water
- Gives brownish colour to the water



Iron Removal

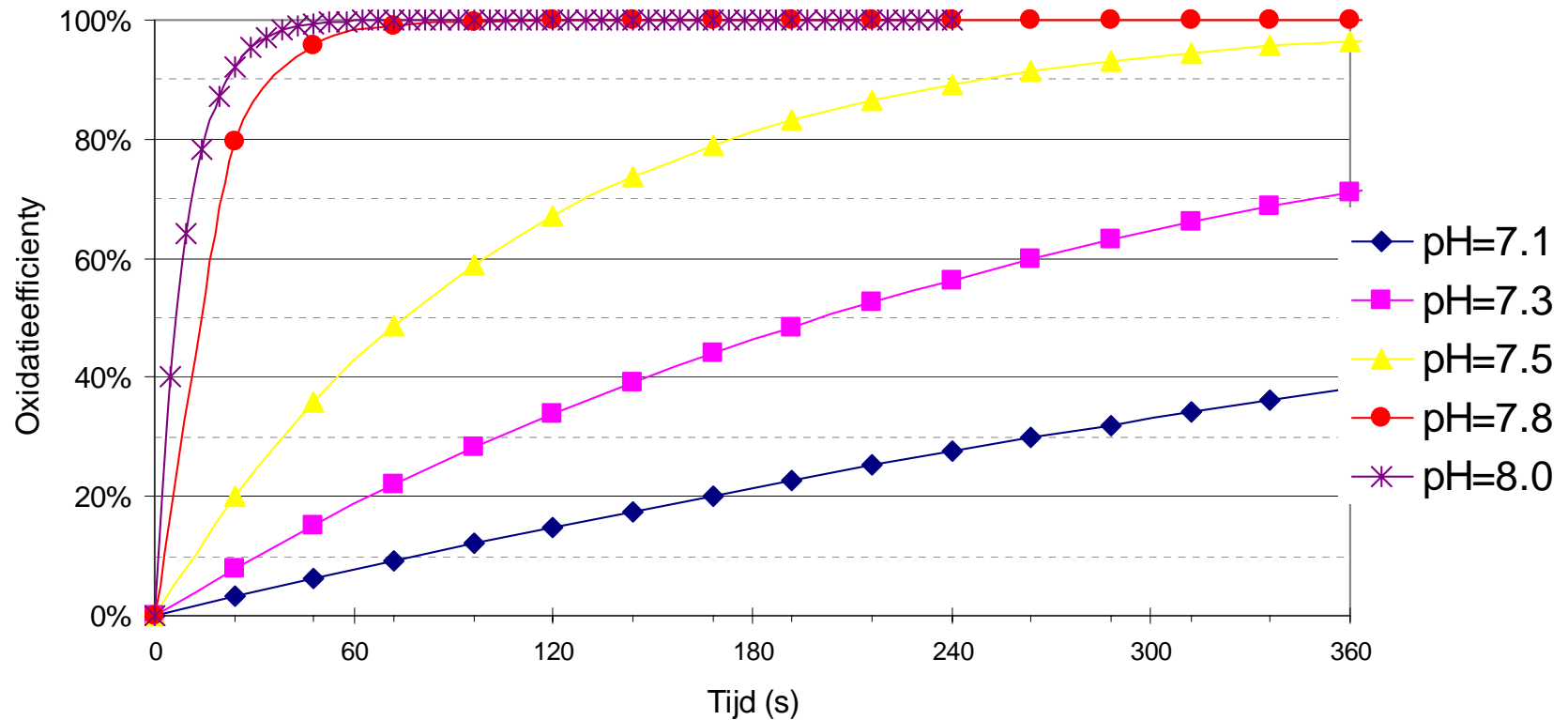


Iron oxidation:



+

oxygen

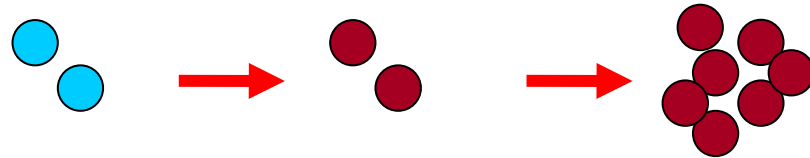


Iron removal

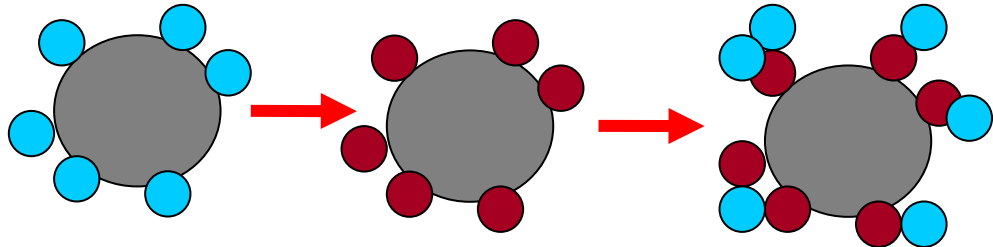
● Fe^{2+} ● Fe^{3+}

Iron removal mechanisms:

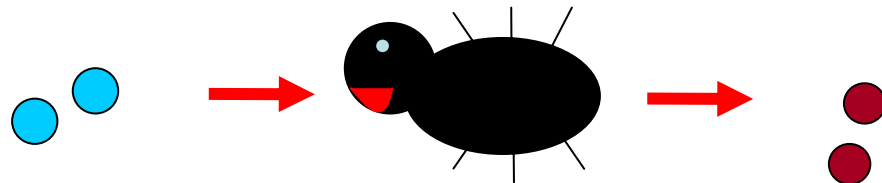
Flock filtration
iron removal



Adsorptive
iron removal



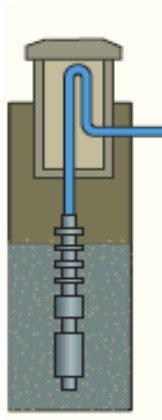
Biological
iron removal



Iron Removal



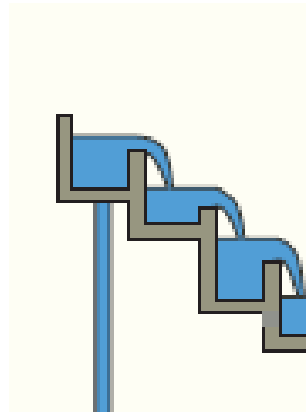
Fe^{2+}



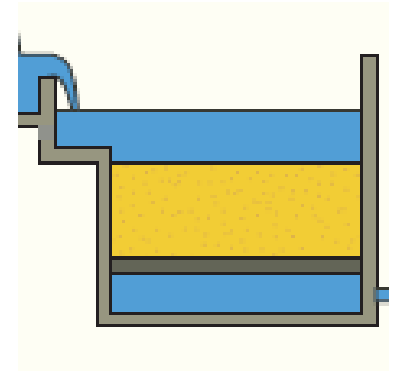
+



O_2



Fe^{3+}



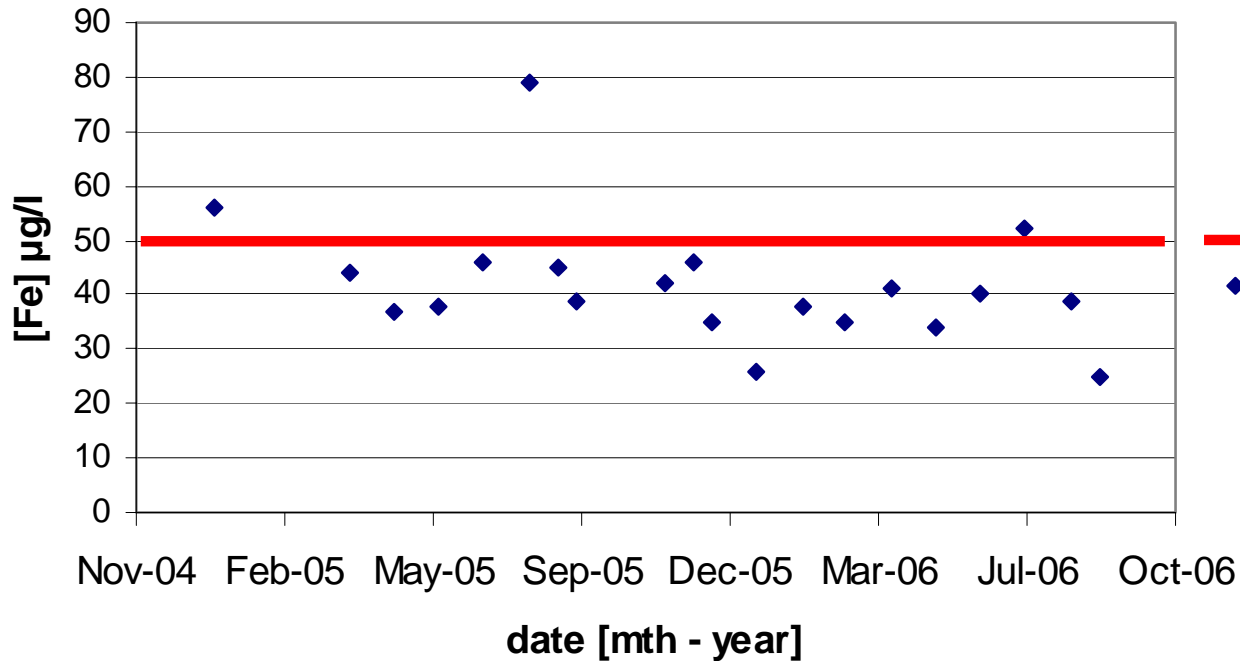
OBJECTIVE

Situation at Harderbroek

Expensive cleaning events



iron concentration in clear water



Vewin

— recommendation
◆ iron clear water



Harderbroek vs Fledite

Comparable water source

Same filters

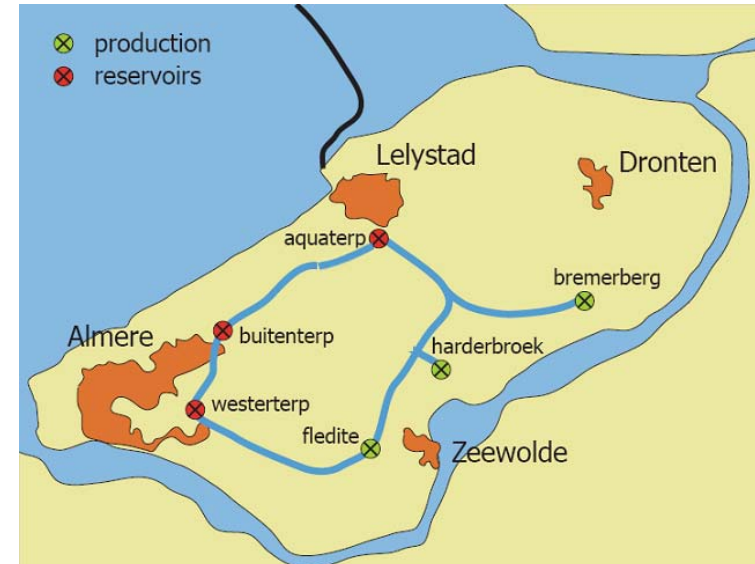
Different aeration

- Harderbroek cascade aeration
- Fledite spray aeration

Hypothesis (1)

Formed iron hydroxide flocks
breakdown in cascade or filter inlet
construction

Small flocks break through the filters



Methods

Particle fingerprint

- To identify the presence of particles through the treatment plant in relation to operational events

Column experiments

- To get information on oxidation and flock formation

Model

- Generate insight in processes in the filter
- Elaborate future scenarios

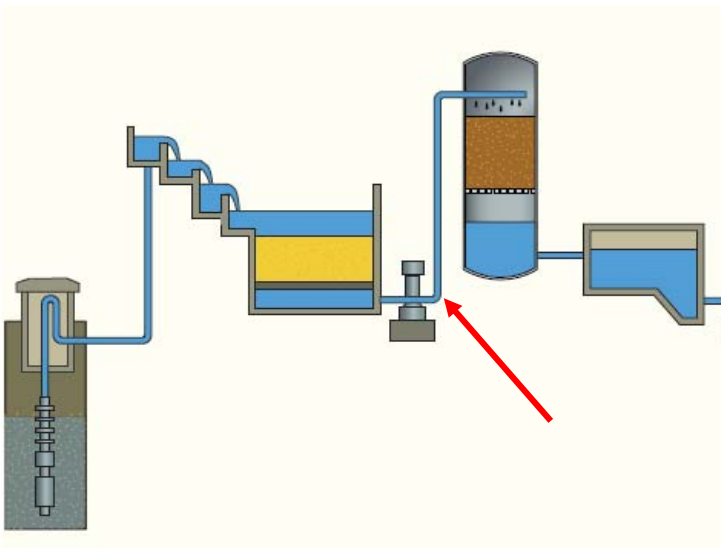
FINGERPRINT

Fingerprint

Particles identified with particle counters

Mainly focussed on filtration step

- After switching a filter
- After a backwash



Fingerprint results

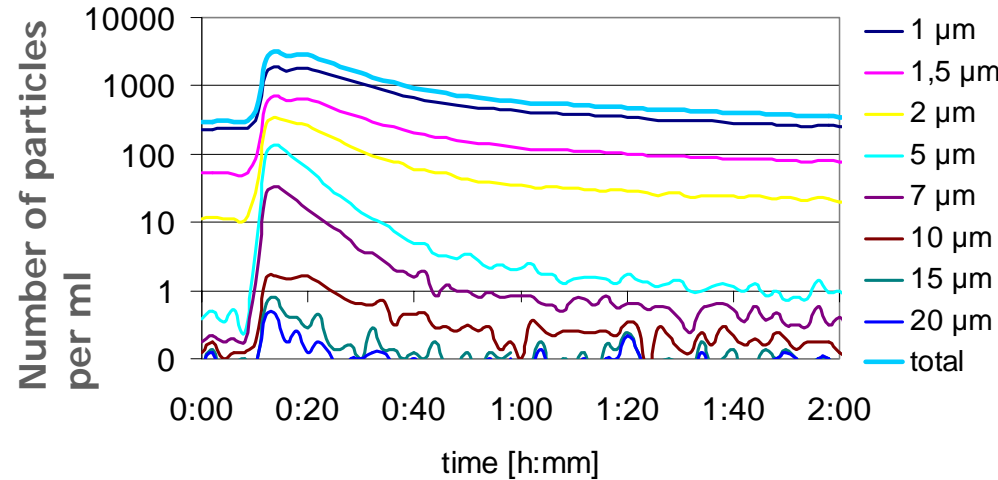
After filter switch

ppb

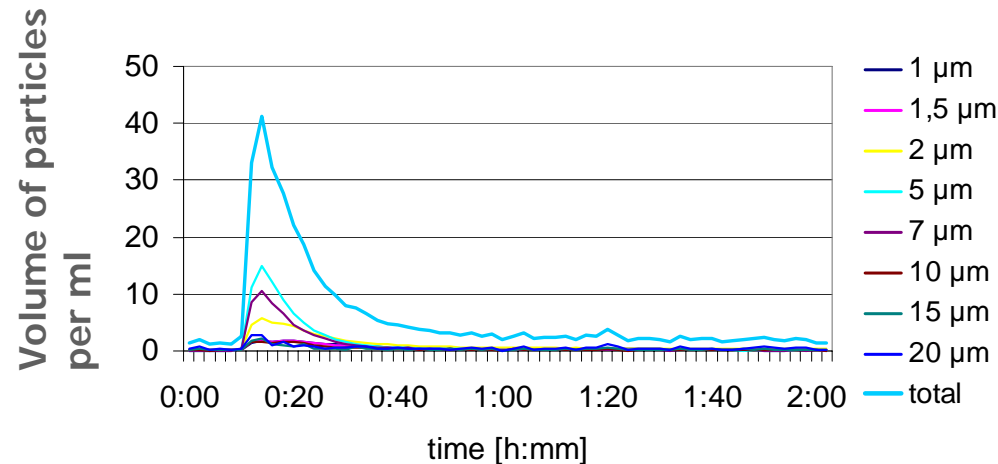
$$V = \frac{1}{6} \pi \sqrt{d_i \cdot d_j}^3 \cdot \text{number}$$

1 part per billion =
1 volume of particles in
1,000,000,000 volumes of water

Number of particles in filter effluent



Volume of particles in filter effluent

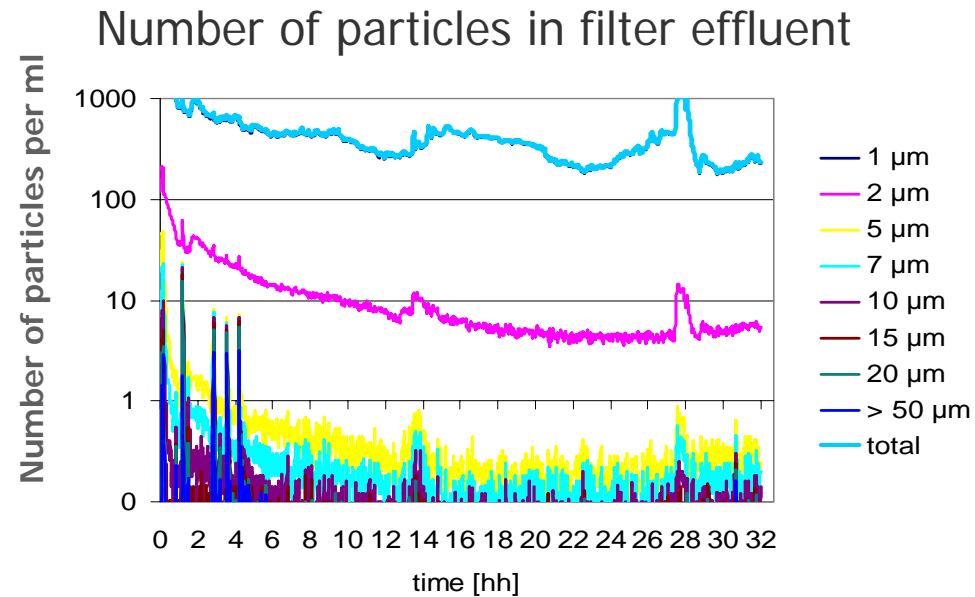


Fingerprint results

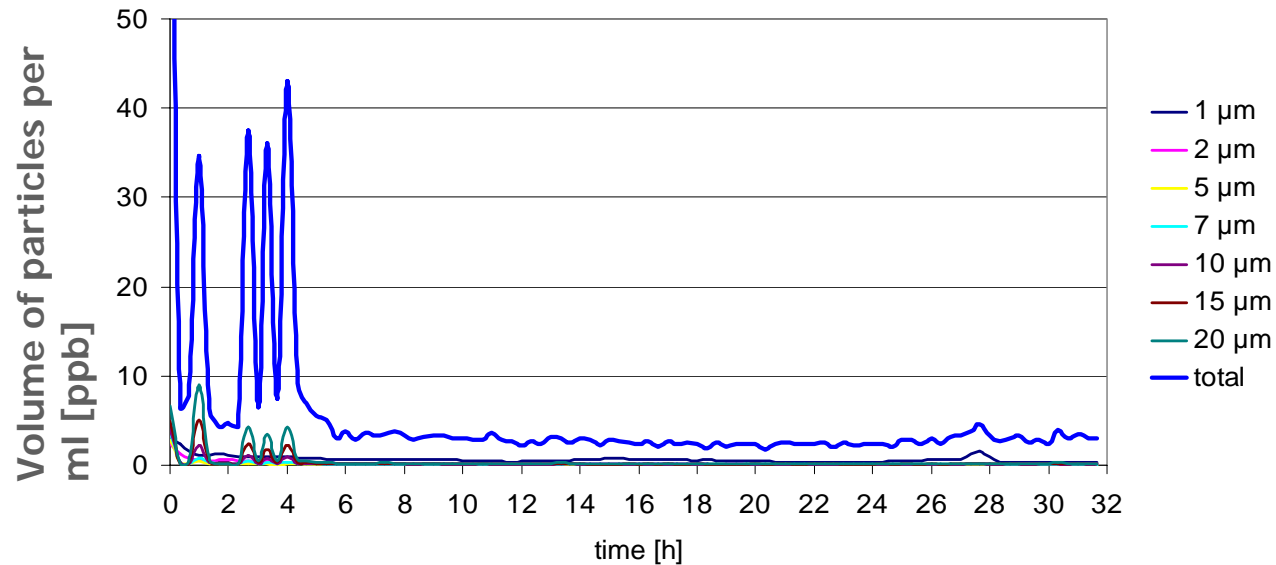
After backwash

Volume concentration increased for 4 hours

→ recirculation



Volume of particles in filter effluent



Fingerprint

Volume load by events compared to stable operation

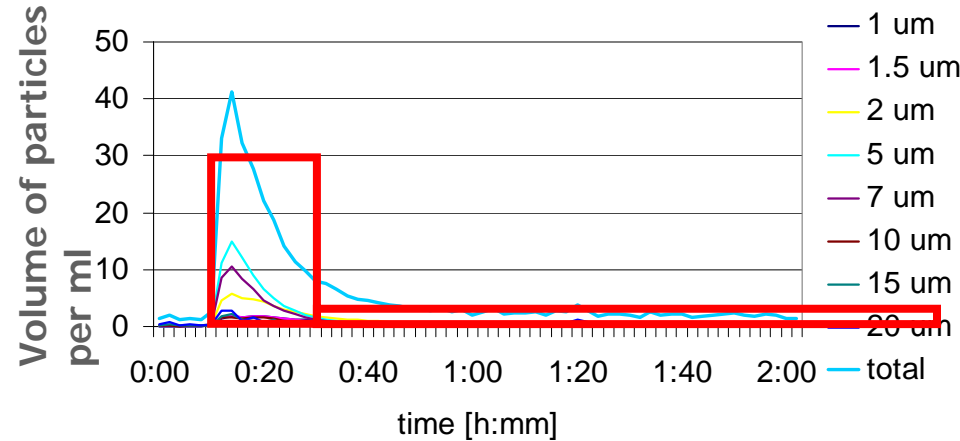
Switch filter

In 2 % of the time
15 % of the load

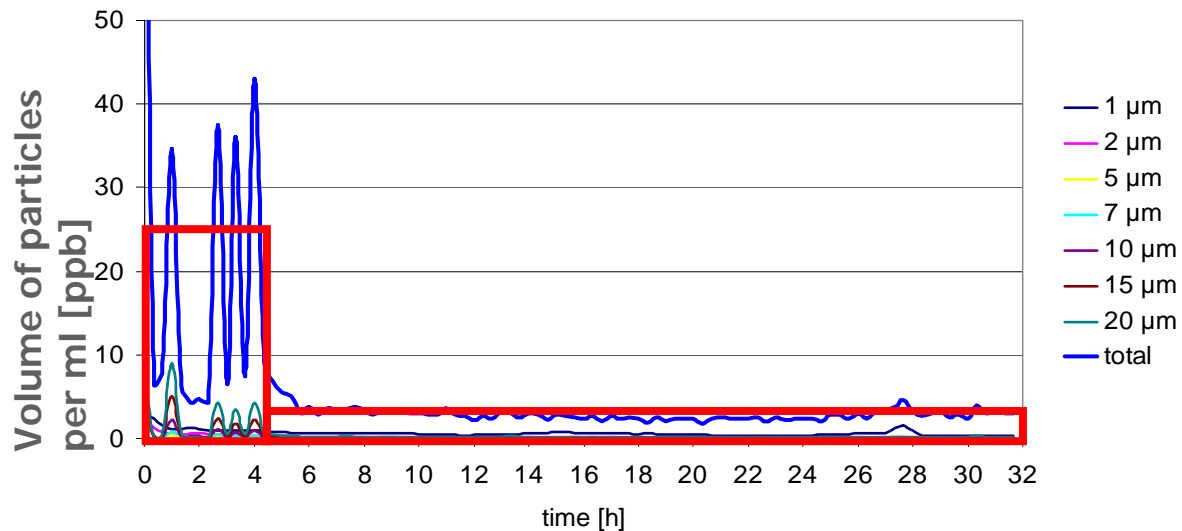
Backwash filter

In 13% of the filter run
time 45 % of the volume
load

Volume of particles in filter effluent



Volume of particles in filter effluent



Fingerprint

Aim

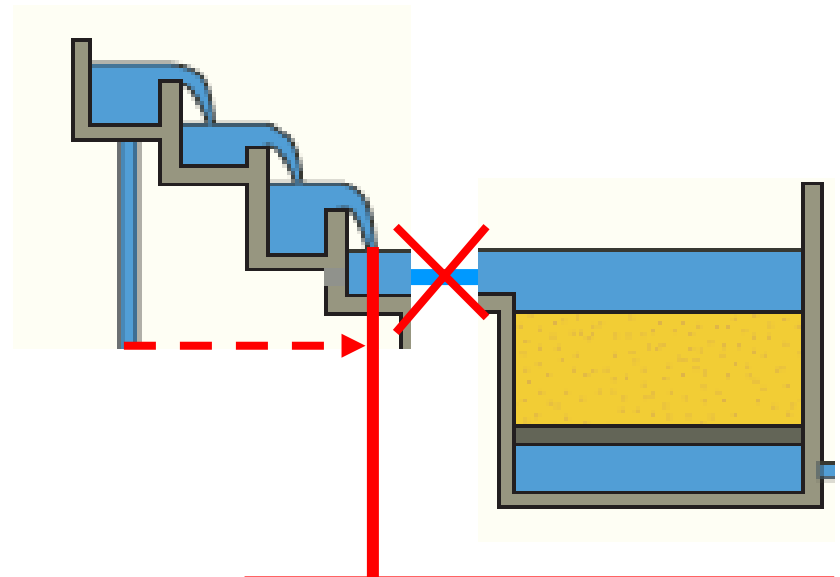
Average 1 ppb

Reduce peaks

Pumping station	Average ppb clear water	Cleaning frequency
Harderbroek	5	1 in 3 years
Franeker	15	1 in 1 year
Franeker + UF	1	1 in 10 - 12 years (expected)

COLUMN EXPERIMENTS

Column experiments



Part 1

- mixing intensity
- residence time
- and aeration

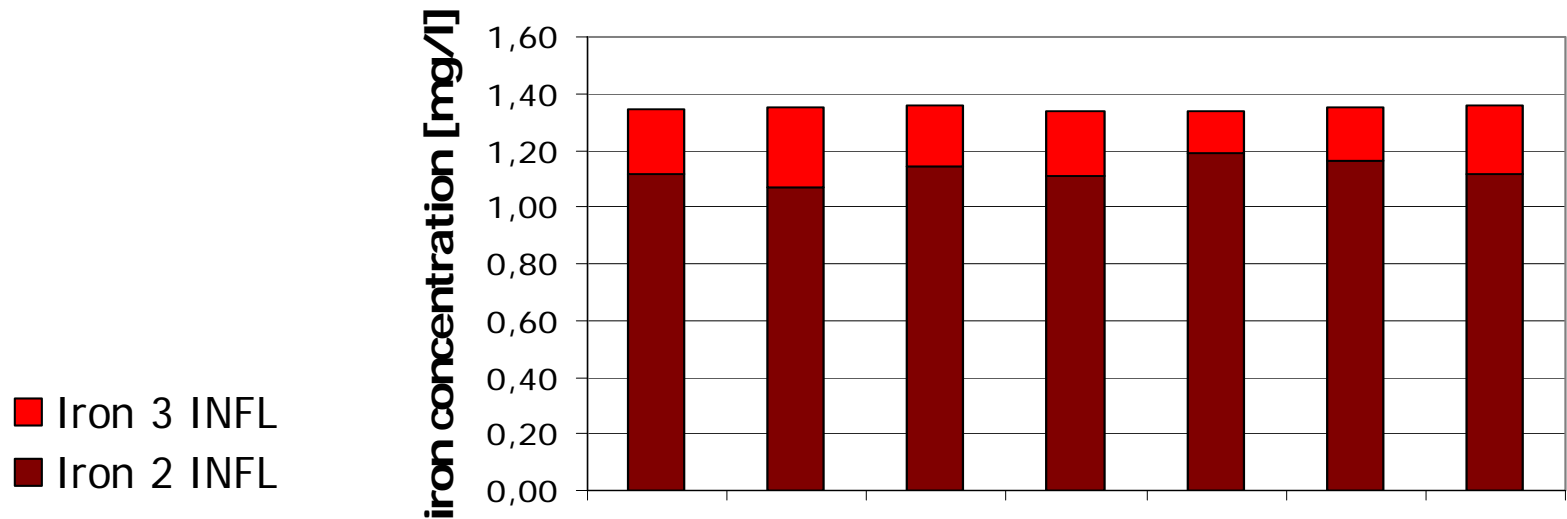
Part 2

- pH



Column results

Iron in cascade effluent



Hypothesis (2)

pH in cascade effluent water too low for efficient oxidation

Column experiments

Experiments with pH increase

NaOH dosage

pH from 7.5 to 8.0

Crushed limestone filtration

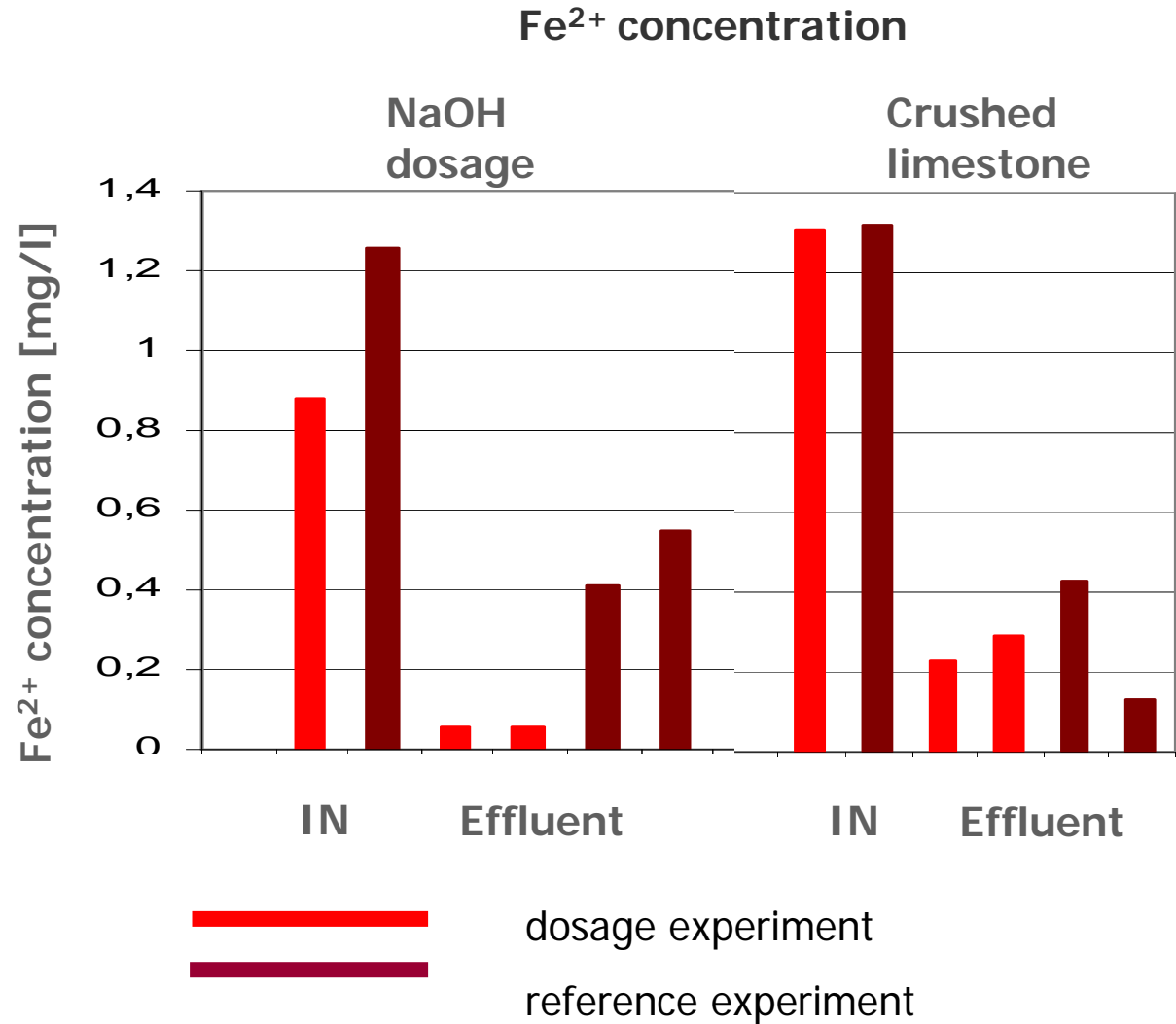
pH from 7.5 to 7.7



Column results

Results

decrease Fe^{2+}
concentration



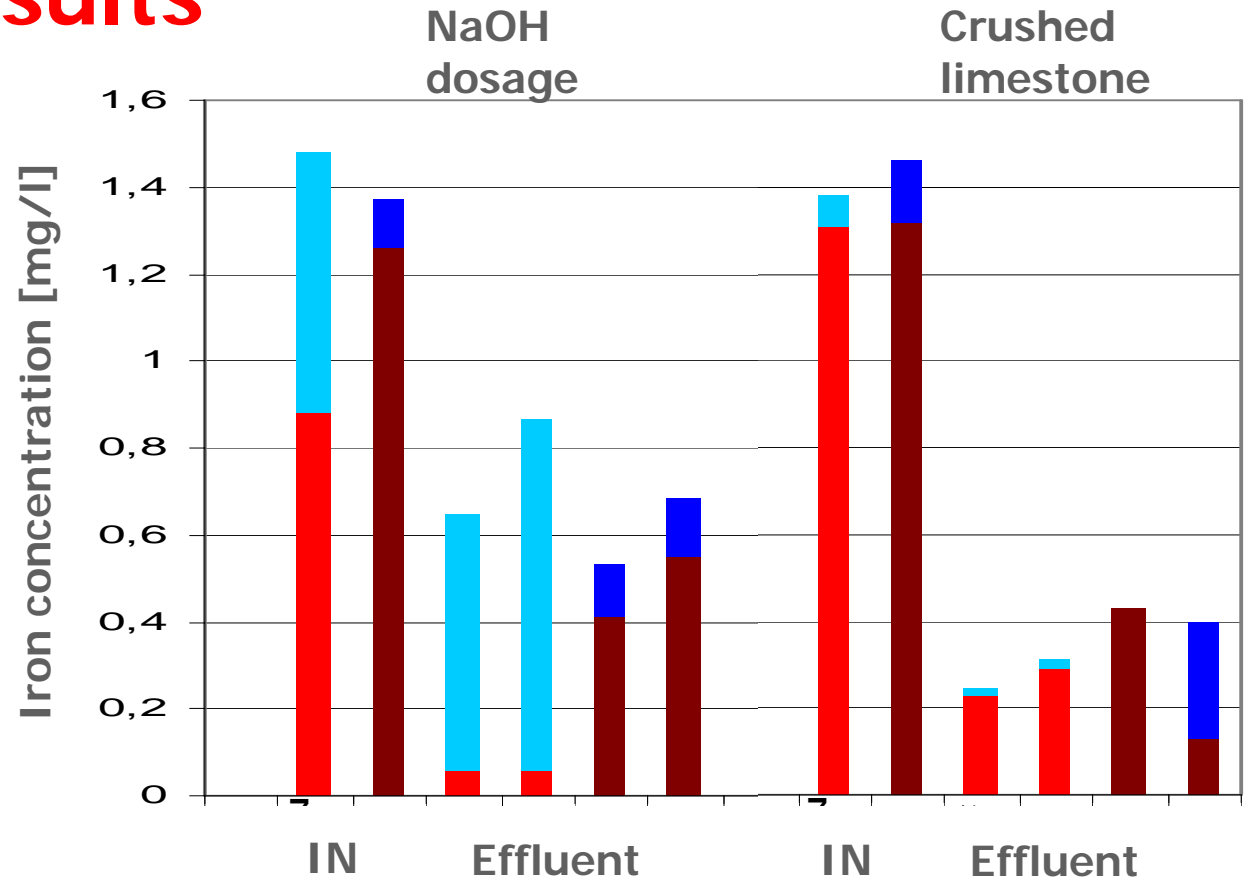
Column results

Results

Decrease Fe²⁺ concentration

Increase Fe³⁺ concentration

Total iron removal comparable



Fe²⁺ dosage experiment

Fe²⁺ reference experiment



Fe³⁺ dosage experiment

Fe³⁺ reference experiment

MODEL

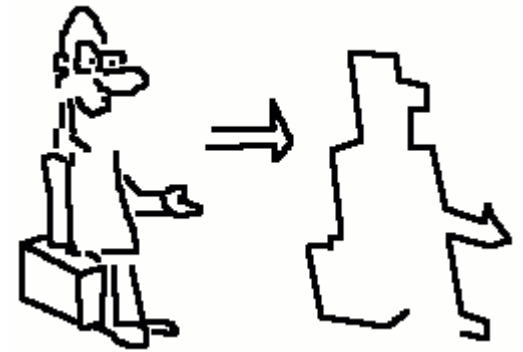
Model

Modelling

Reflection of reality

Simplification of reality

Easy and fast method to vary parameters



Model

Iron removal model is created in Stimela

First reservoir represents water phase before filter

Flock formation

No flock removal

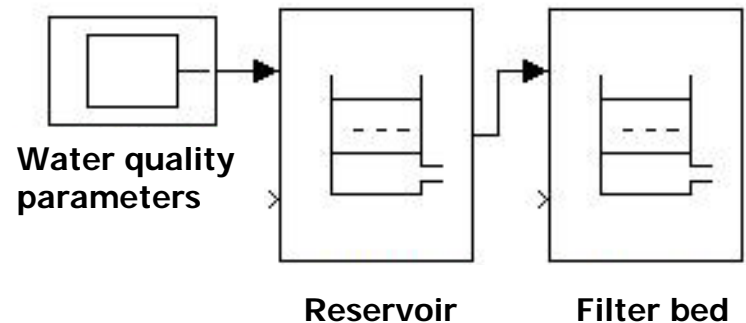
No adsorption

Filter represents filter bed

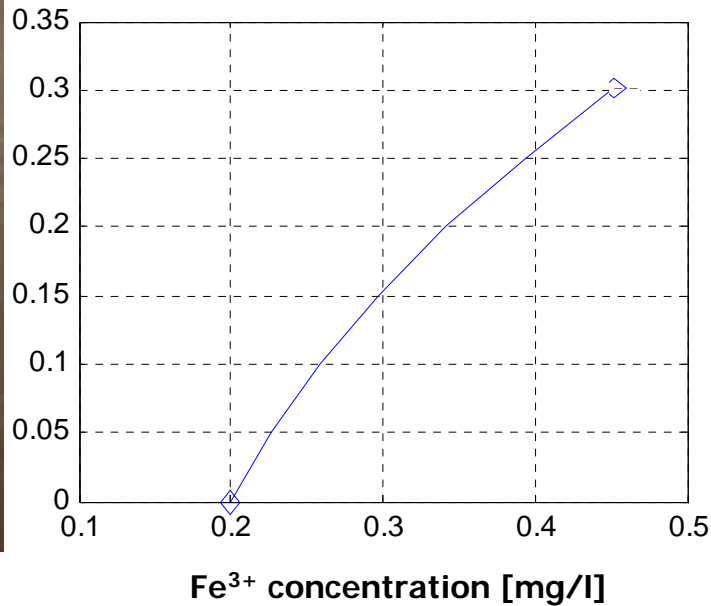
Flock formation

Flock removal

Adsorptive iron removal



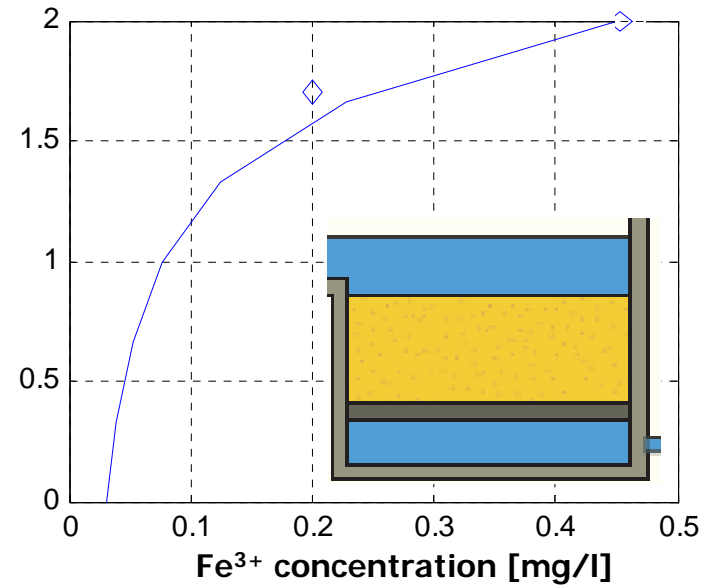
Model results



Column height 30 cm

Fe^{3+} influent concentration 0.45 mg/l

Fe^{3+} effluent concentration 0.20 mg/l



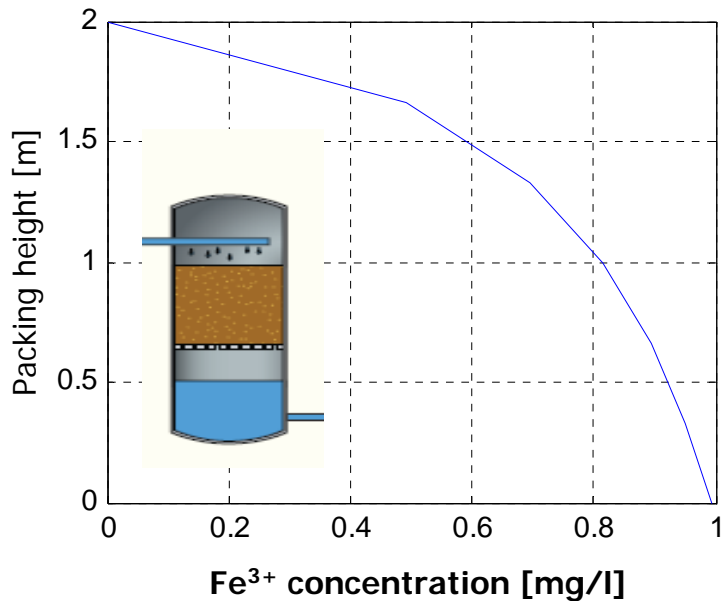
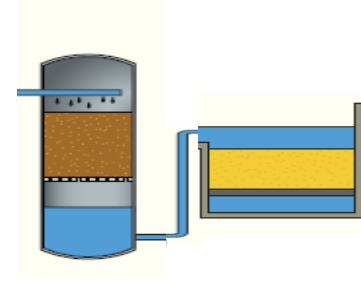
Filter bed height 2 m

Fe^{3+} effluent concentration

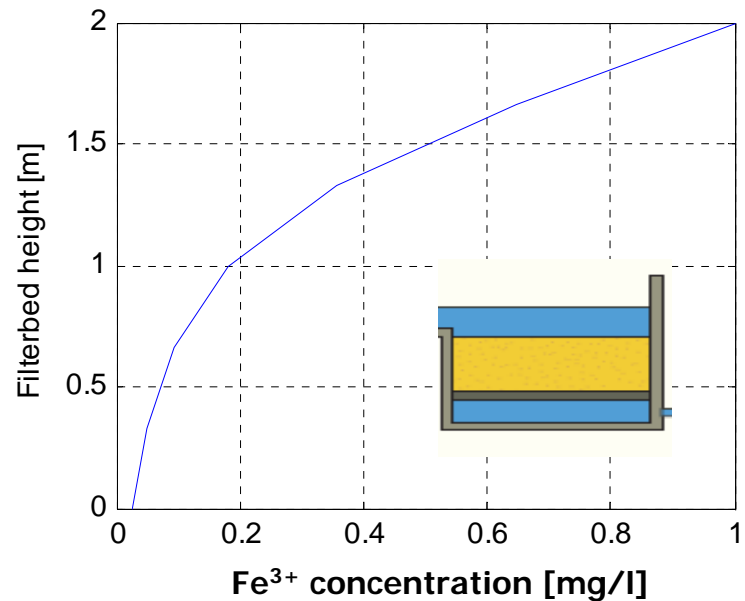
0.033 mg/l

Model results

Tower aeration before filtration:



Fe³⁺ effluent concentration
1 mg/l



Fe³⁺ effluent concentration
0.029 mg/l

CONCLUSIONS & RECOMMENDATIONS

Conclusion

Model

- First set-up made for iron removal model
- Quick insight in alternatives

Column experiments

- After cascade aeration the majority of iron is dissolved Fe^{2+}
- At Harderbroek oxidation is limited by the pH

Conclusion

Fingerprint

- Operational events have a significant contribution to volume load
- Relation between ppb's and cleaning frequency

Recommendations

- Apply a smooth treatment operation
- Recirculation of first filtrate after a backwash event
- Guideline 1 ppb?

Alternatives Harderbroek

Replace tower aeration directly after raw water

- More intensive aeration will increase the pH
- No addition of chemicals to the water

Caustic soda dosage

- Easy to implement
- Relatively sensitive to control

Crushed limestone filtration

- Automatic equilibrium, no need for control
- More investment costs, 2 filtration steps

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