

# Pumping station of Harderbroek

## Improving iron removal

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## Previous presentation

- Analysis of the alternatives

  - » cascade – **limestone filtration** – tower aeration – rapid sand filtration

Same structure but changes in the use of the existing filters

## This presentation

- Calculations of the capacity of the treatment
- Hydraulic line

# Cascades

- 4 cascades each one with 6 steps
- Lower reservoir
- The water enters a division gutter that feeds only one filter
- Maximum flow through one cascade  $500 \text{ m}^3/\text{h}$
- Efficiency = 20%



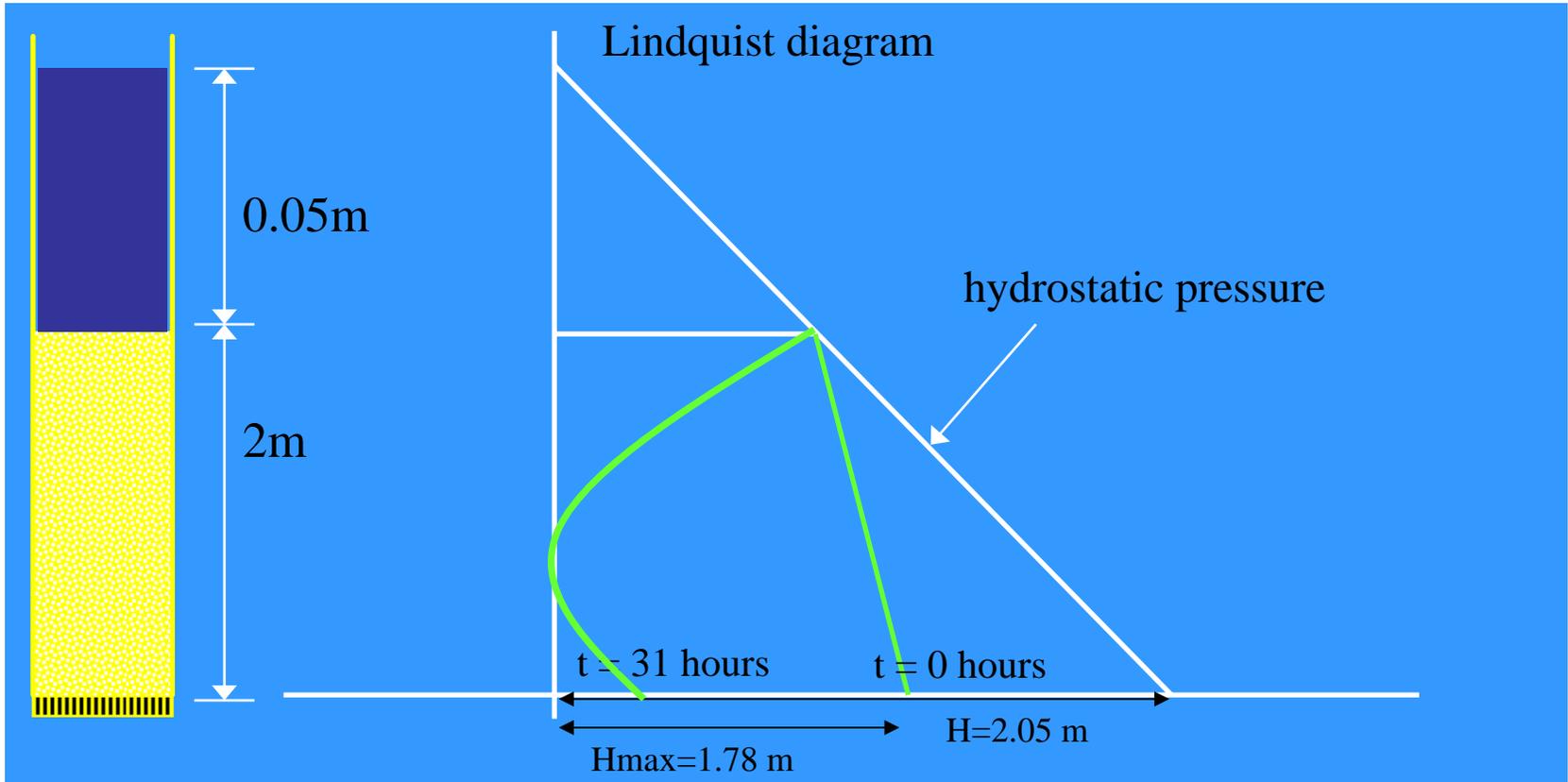
# Crushed limestone filtration

- 4 filters  $\longrightarrow$  2 lines
- Filter material  $\longrightarrow$  Jura Perle grains of limestone (1,1-1,8mm)
- Area = 24m<sup>2</sup>
- Max flux (Q) = 500m<sup>3</sup>/h
- Filtration rate (v) = Q/A = 20,8m/s
- Height of the bed (L) = 2m
- Height of the supernatant = 0,05m

# BACKWASH 1

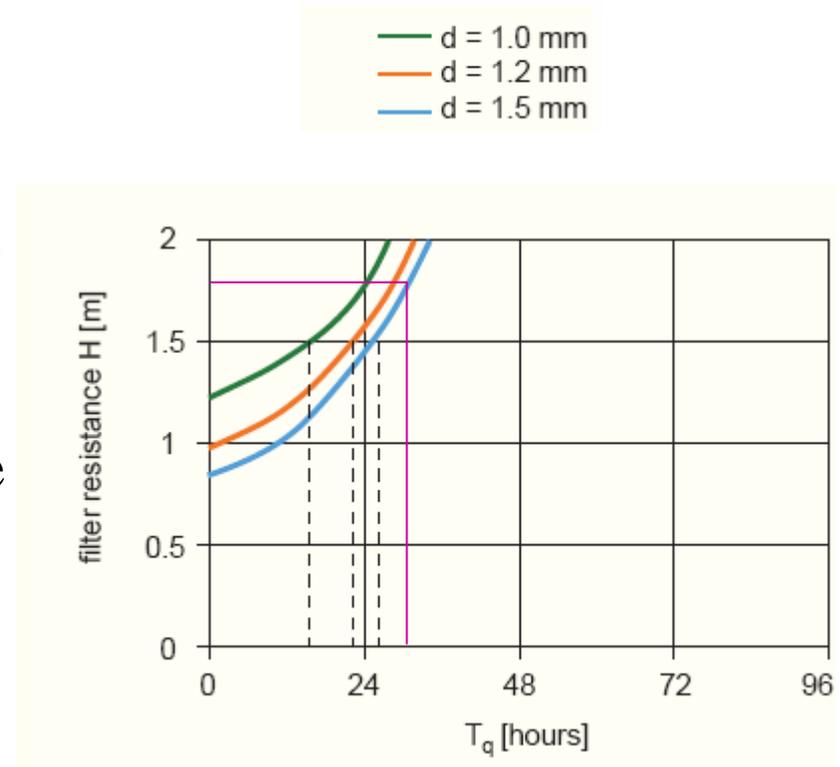
- 8000m<sup>3</sup> at least 32 hours

- Clean bed resistance = 
$$H_o = I_o \cdot L = 180 \cdot \frac{v}{g} \cdot \frac{(1-p_o)^2}{p_o^3} \cdot \frac{v}{d_o^2} \cdot L = 0.27$$



# BACKWASH 2

- $H_{\max} = 1.78 \longrightarrow 28$  hours
- $8000\text{m}^3 \longrightarrow 14000\text{m}^3$
- Backwash based on measure of pressure



# Tower aeration



- Aim: decrease CO<sub>2</sub> and increase of O<sub>2</sub>
- Three towers
- Surface of 6.06 m<sup>2</sup>
- Bed load = 50 m<sup>3</sup>/m<sup>2</sup>\*h
- Bed height = 2m

# Rapid sand filtration

- 4 filters  $\longrightarrow$  2 lines
- Filter material  $\longrightarrow$  **sand (0.6-1mm)**
- Area =  $24\text{m}^2$
- Max flux (Q) =  $500\text{m}^3/\text{h}$
- Filtration rate (v) =  $Q/A = 20,8\text{m}/\text{s}$
- Height of the bed (L) =  $2\text{m}$
- Height of the supernatant =  $0,05\text{m}$
- **Higher efficiency but more tests are necessary to calculate the improvement in the suspended solids removal**

# pH calculation

## CASCADES:

- The pH is raised because of the CO<sub>2</sub> removal
- The pH is lowered because of the flocks formation
- The value remains of 7.46

## CRUSHED LIMESTONE FILTRATION:

- pH = 8  $\longrightarrow$  1:50 = CO<sub>2</sub>:HCO<sub>3</sub><sup>-</sup>
- Removal of all the CO<sub>2</sub> (5,5mg/l)  
CO<sub>2</sub> = 0.125 mmol/l      HCO<sub>3</sub><sup>-</sup> = 1.34 mmol/l  
CaCO<sub>3</sub> + CO<sub>2</sub> + H<sub>2</sub>O  $\longrightarrow$  Ca + 2HCO<sub>3</sub><sup>-</sup>

Q(m<sup>3</sup>/h)  $\longrightarrow$  mg CO<sub>2</sub>/h  $\longrightarrow$  mg CaCO<sub>3</sub>/h

# Fe concentration

- The pH is high so the oxydation of Fe(II) is faster
- The flocks are removed through the filtrations
- **GOAL concentration of 0.02 mg/l 90% time**



**Thanks for your attention**

**Questions???**