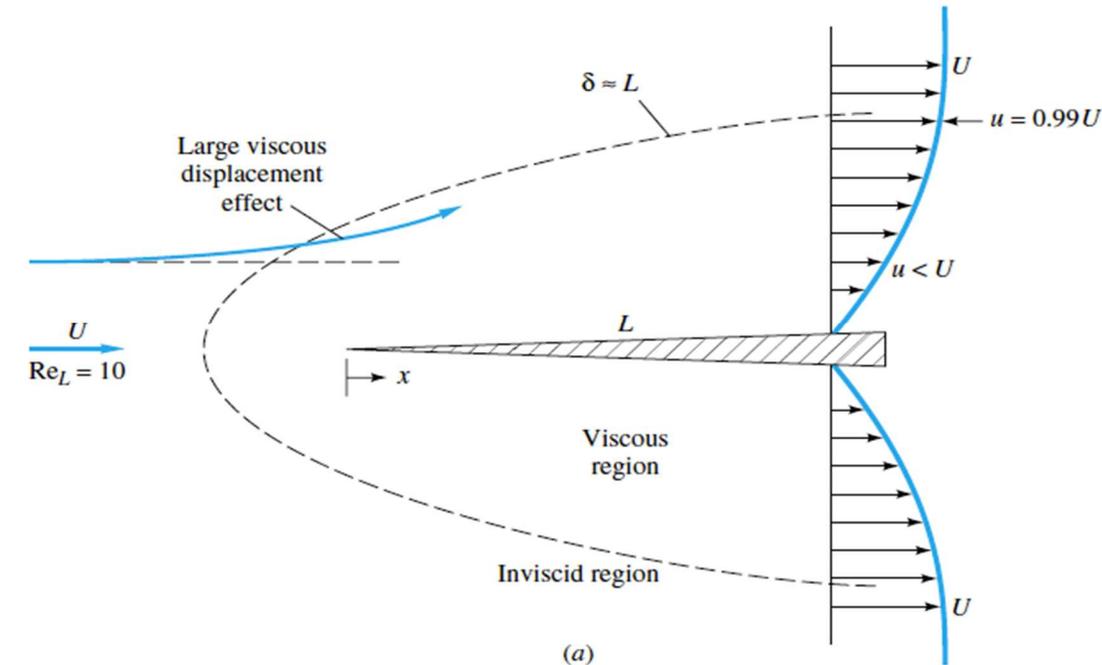


Fluid mechanics (wb1225)

Lecture 10: boundary layers

Flow past a thin plate

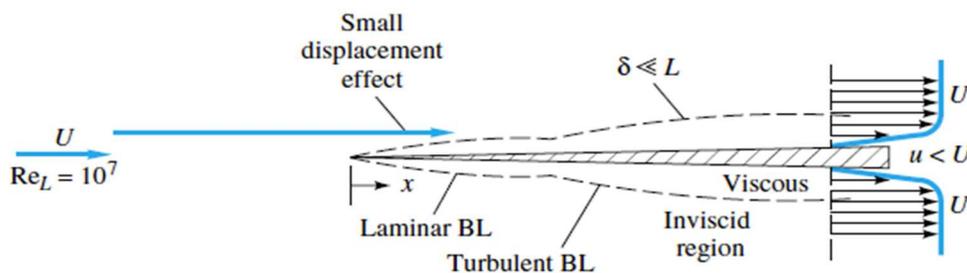


laminar flow:

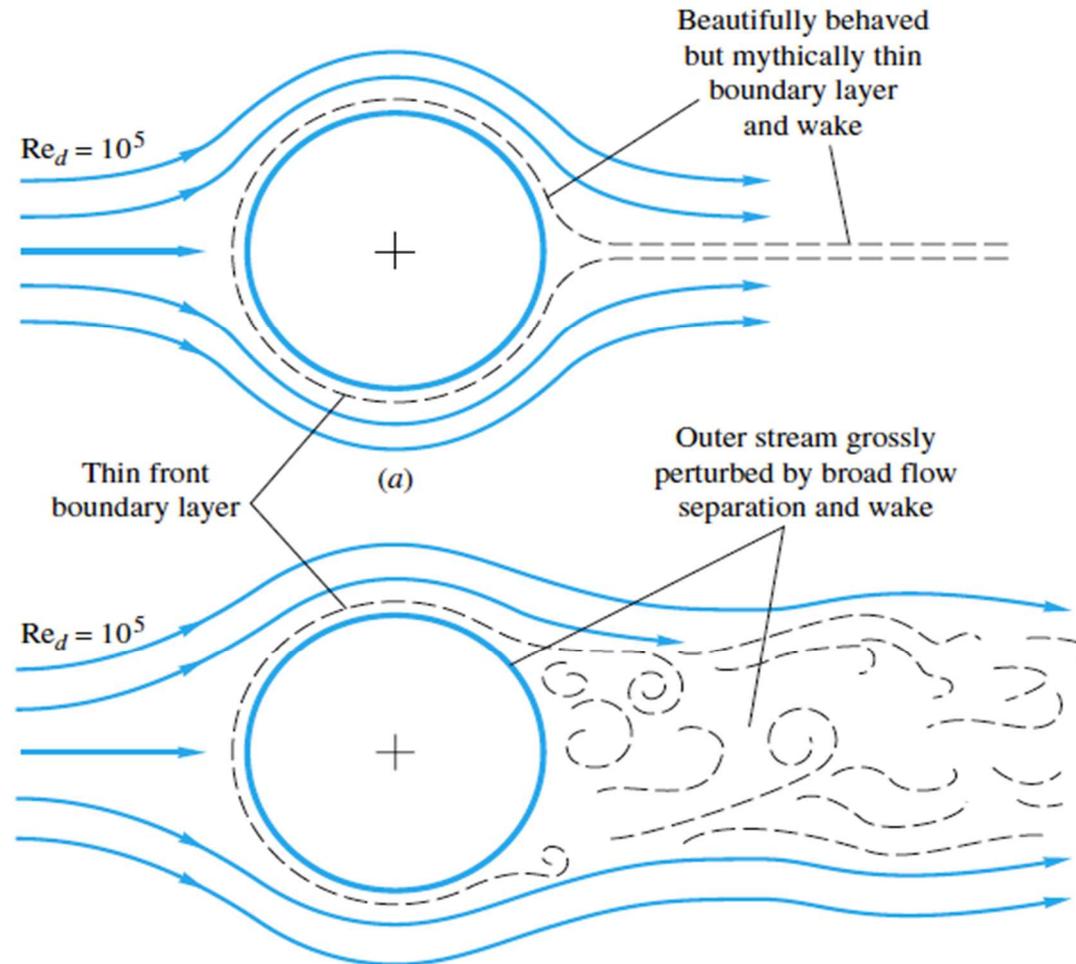
$$\frac{\delta}{x} \approx 5.0 Re_x^{-1/2}$$

turbulent flow:

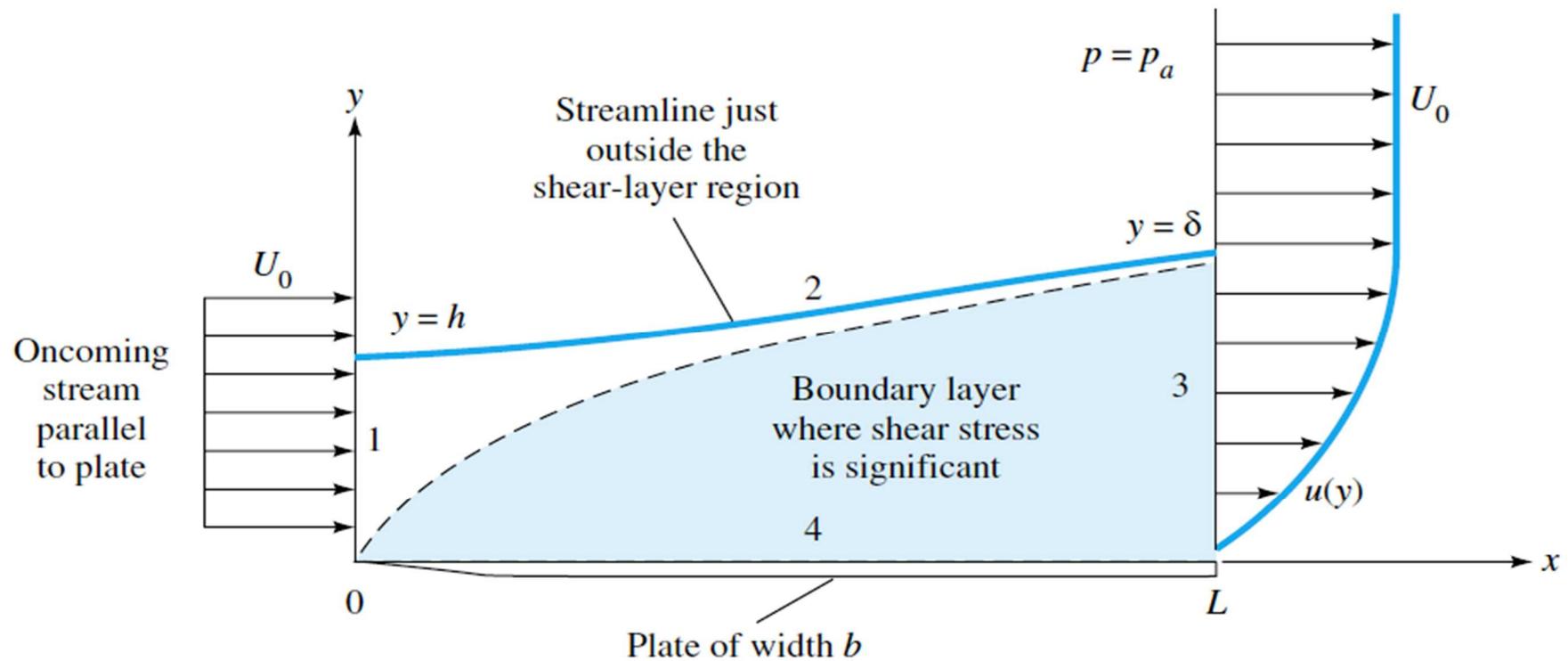
$$\frac{\delta}{x} \approx 0.16 Re_x^{-1/7}$$



Flow around an object



Boundary layer



Example 3.11

$$\begin{aligned}\sum F_x &= -D = \rho \int_1 u V_n dA + \rho \int_3 u V_n dA \\ &= \rho \int_0^h U_0 (-U_0) b dy + \rho \int_0^\delta u(y) (+u(y)) b dy\end{aligned}$$

$$\Rightarrow D = \rho U_0^2 b h - \rho b \int_0^\delta u^2(y) dy$$

$h \rightarrow \delta ? \Rightarrow$ conservation of mass

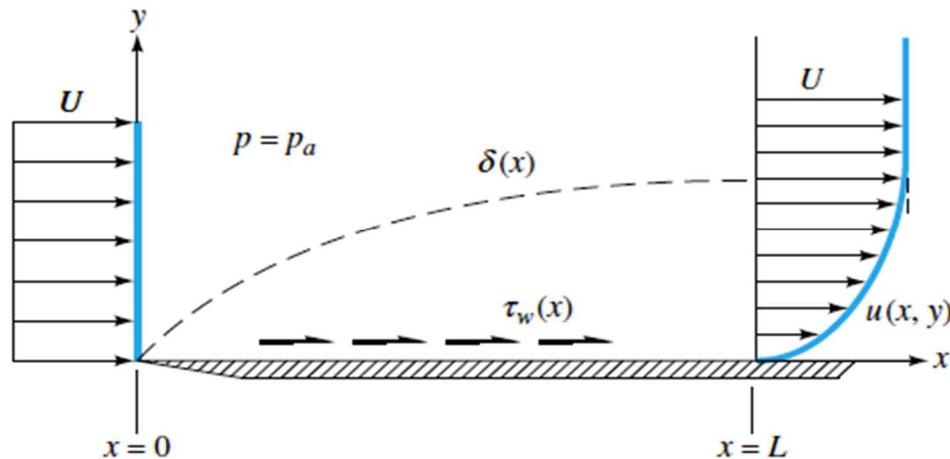
$$U_0 h = \int_0^\delta u(y) dy$$

$$D = \rho b \int_0^\delta u (U_0 - u) dy$$

momentum defect

Theodore von Kármán
(1921)

Growth of a boundary layer



momentum integral:

$$D(x) = \rho b \int_0^{\delta(x)} u(U - u) dy$$

$$D(x) = \rho b U^2 \theta, \quad \theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U} \right) dy$$

momentum thickness

drag equals integrated wall shear stress:

$$D(x) = b \int_0^x \tau_w(x) dx \quad \Rightarrow \quad \frac{dD}{dx} = b \tau_w$$

also:

$$\frac{dD}{dx} = \rho b U^2 \frac{d\theta}{dx}$$

momentum integral relation:

$$\tau_w = \rho U^2 \frac{d\theta}{dx}$$

assume: $u(x, y) \approx U \left(\frac{2y}{\delta(x)} - \frac{y^2}{\delta(x)^2} \right), \quad 0 \leq y \leq \delta(x) \Rightarrow \frac{\delta}{x} \approx 5.5 \left(\frac{\nu}{Ux} \right)^{1/2} = 5.5 \text{Re}_x^{-1/2}$

$$\tau_w = \rho U^2 \frac{d\theta}{dx} \quad \theta = \frac{2}{15} \delta \quad \tau_w = \mu \left. \frac{du}{dy} \right|_{y=0} = \frac{2\mu U}{\delta} \Rightarrow \frac{2\mu U}{\delta} = \frac{2}{15} \rho U^2 \frac{d\delta}{dx}$$

Turbulent boundary layer

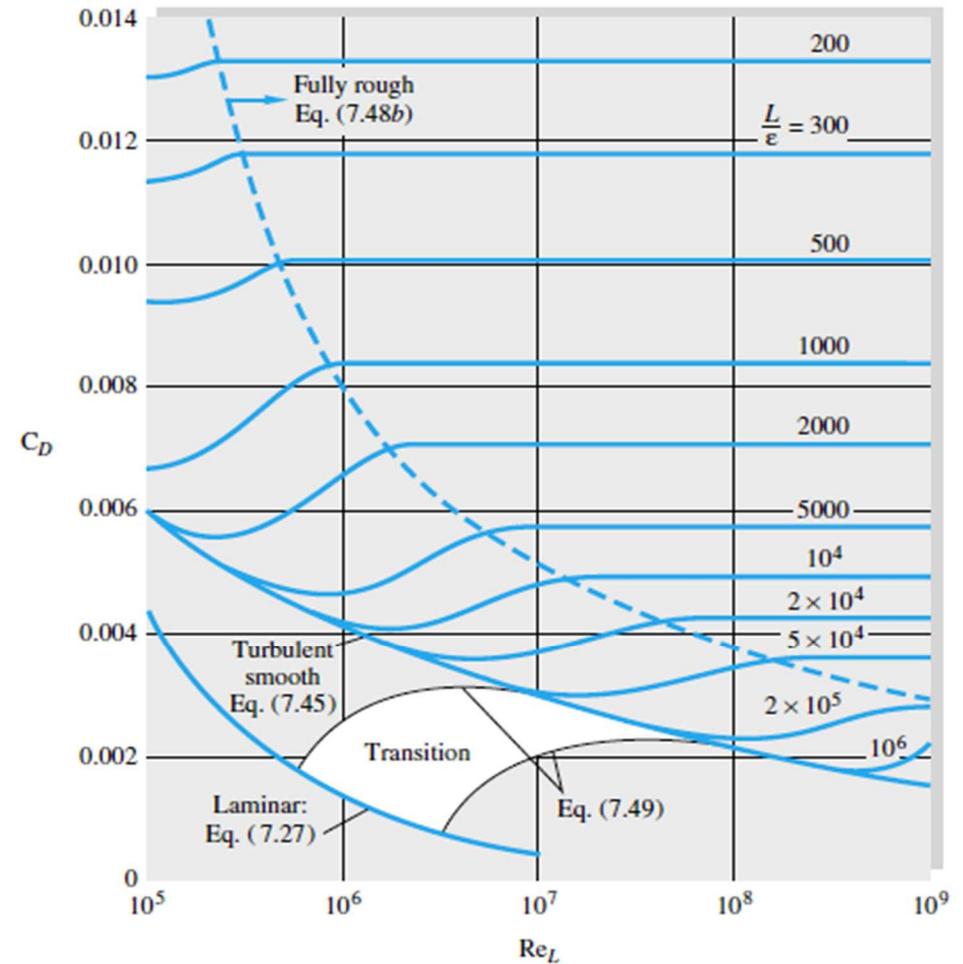
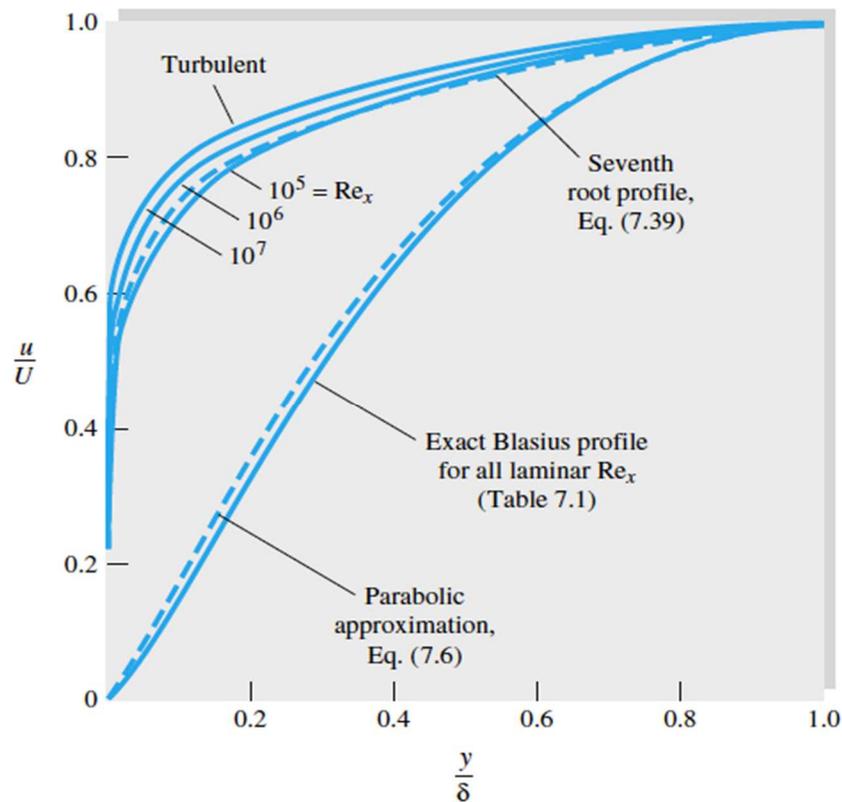
$$\tau_w = \rho U^2 \frac{d\theta}{dx} \quad \frac{u}{U} = \left(\frac{y}{\delta}\right)^{1/7} \quad \theta = \frac{7}{72} \delta$$

$$\text{empirical: } \tau_w \cong 0.01 \rho U^2 \left(\frac{\mu}{\rho U \delta}\right)^{1/6}$$

$$\Rightarrow \frac{\delta}{x} \cong \frac{0.16}{\text{Re}_x^{1/7}}$$

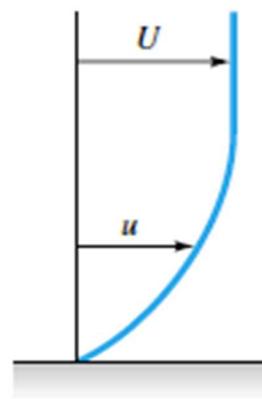
Flat-plate boundary layer

$$C_D = \frac{D(L)}{\frac{1}{2} \rho U^2 b L}$$

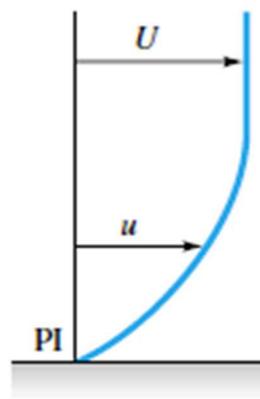


Effect of pressure gradient

$$\left. \frac{\partial \tau}{\partial y} \right|_{\text{wall}} = \mu \left. \frac{\partial^2 u}{\partial y^2} \right|_{\text{wall}} = \frac{dp}{dx} = -\rho U \frac{dU}{dx}$$



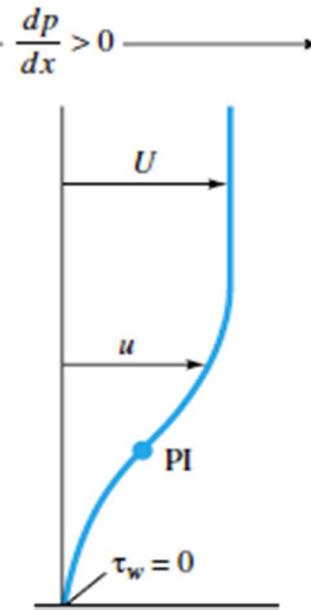
(a) Favorable gradient:
 $\frac{dU}{dx} > 0$
 $\frac{dp}{dx} < 0$
 No separation, PI inside wall



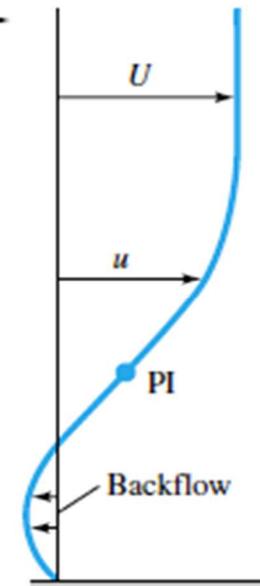
(b) Zero gradient:
 $\frac{dU}{dx} = 0$
 $\frac{dp}{dx} = 0$
 No separation, PI at wall



(c) Weak adverse gradient:
 $\frac{dU}{dx} < 0$
 $\frac{dp}{dx} > 0$
 No separation, PI in the flow



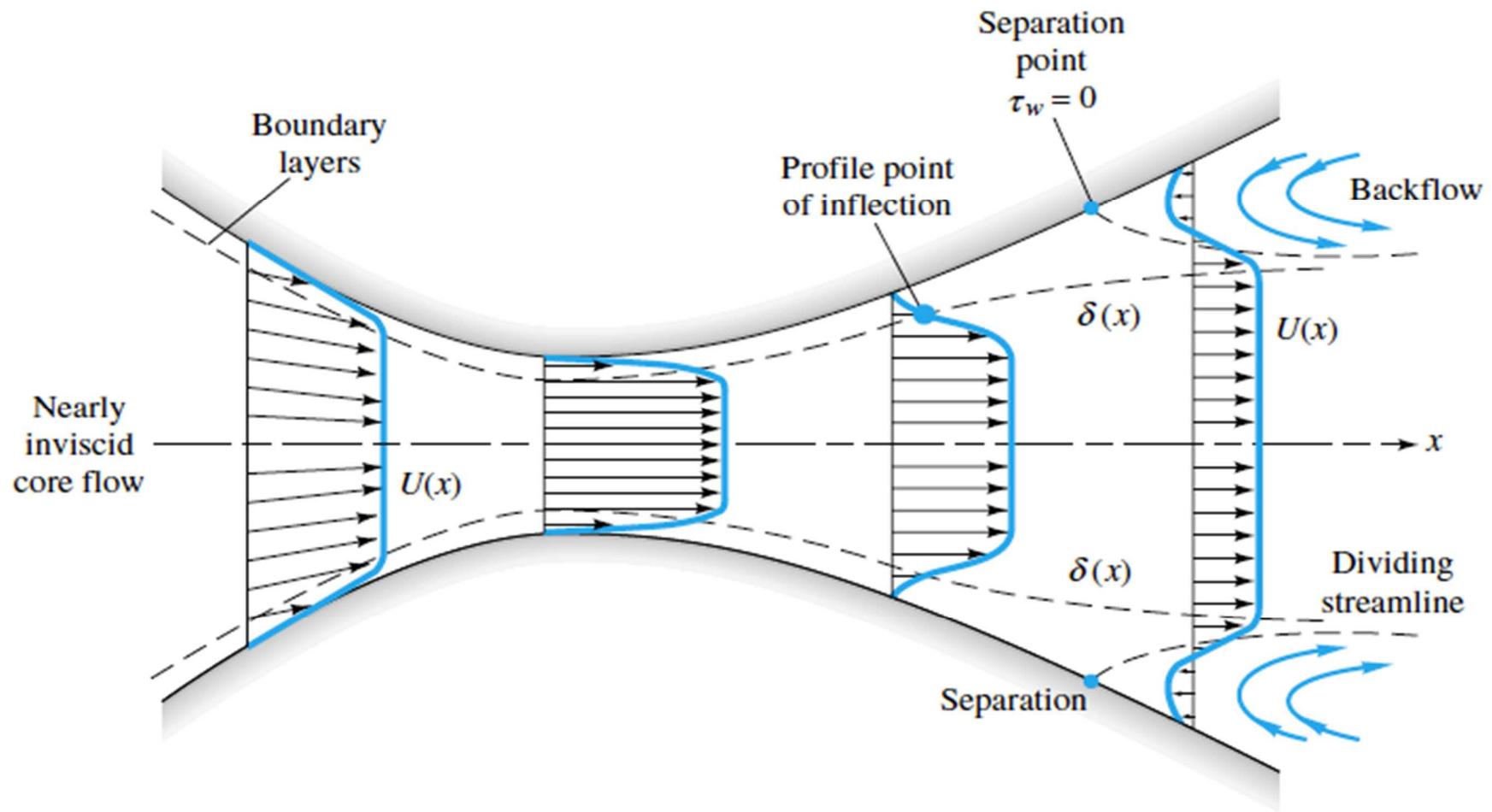
(d) Critical adverse gradient:
 Zero slope at the wall:
Separation



(e) Excessive adverse gradient:
 Backflow at the wall:
 Separated flow region

$$\leftarrow \frac{dp}{dx} > 0 \rightarrow$$

Nozzle-diffuser



Boundary layer integral theorem

$$\frac{\tau_w}{\rho U^2} = \frac{1}{2} c_f = \frac{d\theta}{dx} + (2 + H) \frac{\theta}{U} \frac{dU}{dx}$$

shape factor:

$$H = \frac{\delta^*}{\theta}$$

$$H = \begin{cases} 3.5 & \text{laminar flow} \\ 2.4 & \text{turbulent flow} \end{cases}$$

momentum thickness:

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$$

displacement thickness:

$$\delta^* = \int_0^{\delta} \left(1 - \frac{u}{U}\right) dy$$

NB: $\delta = \delta_{0.99}$

Summary

- Chapter 7:
- Examples:
- Problems:

Source

All images are from the book of Frank M. White, *Fluid Mechanics*, McGraw-Hill Series in Mechanical Engineering.