

Offshore Hydromechanics

Module 1 : Hydrostatics Constant Flows Surface Waves

OE4620 Offshore Hydromechanics

Ir. W.E. de Vries

November 2007

Today

First hour:

- Schedule for remainder of hydromechanics module 1
- Assignment stability
- Basic flow properties
- Potential flow concepts

Second hour:

- Potential flow elements
- Superposition of flow elements
- Cylinder in uniform flow

Schedule OE4620 Module 1

- 13 November – Constant potential flow phenomena
- 20 November – Constant real flow phenomena 1
- 27 November – Constant real flow phenomena 2
- 4 December – Ocean surface waves 1 (!)
- 11 December – Ocean surface waves 2
- 18 December – Extra/Examples

Assignment: Stability

- Make the assignment for next lecture
- Next lecture the assignment will be worked out briefly
- Questions regarding the assignment or the subjects of module 1?

Contact:

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- Tel. 015 278 7568
- E-mail w.e.devries@tudelft.nl

CONSTANT POTENTIAL FLOW PHENOMENA

Flows in this chapter:

- Obey simplified laws of fluid mechanics
- Are subject to limitations
- Give qualitative impressions of flow phenomena

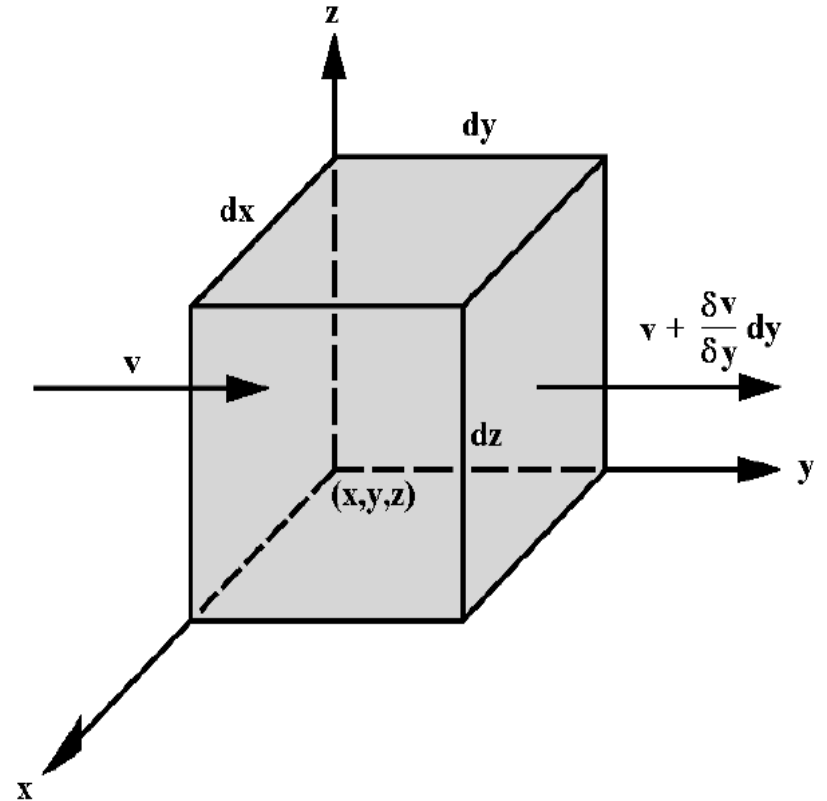
Basic Flow Properties

- Ideal fluid :
 - Non – viscous
 - Incompressible
 - Continuous
 - Homogeneous

Continuity Condition

- Increase of mass per unit time:

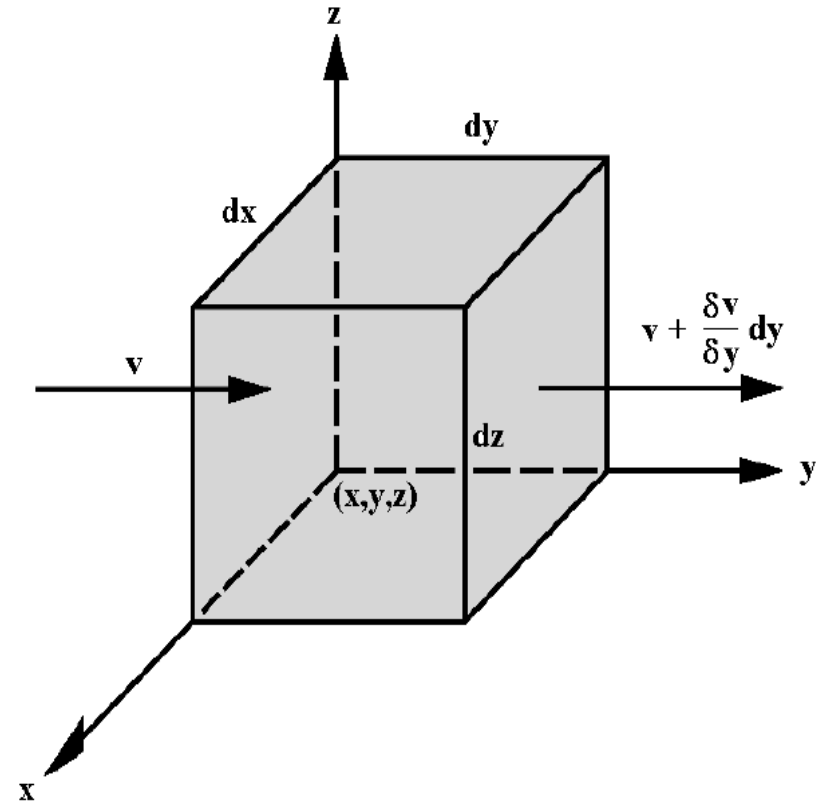
$$\frac{\partial m}{\partial t} = -\frac{\partial}{\partial t}(\rho \cdot dx dy dz)$$



Continuity Condition

- Mass through a plane $dx dz$ during a unit of time:

$$m_{in} = \rho \cdot v \cdot dx dz dt$$

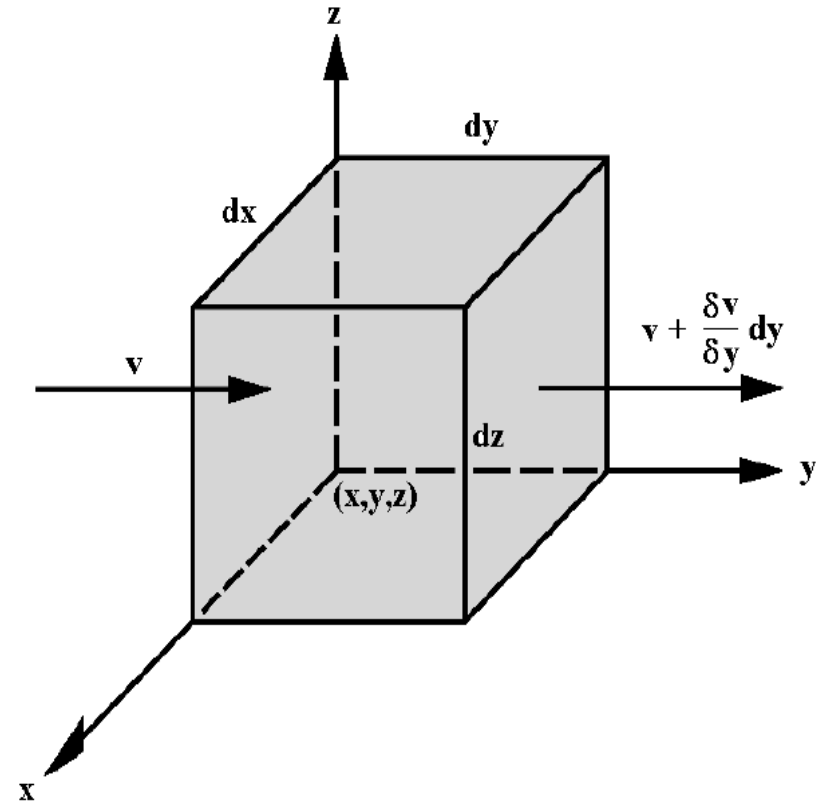


Continuity Condition

- Mass through a plane $dx dz$ during a unit of time:

$$m_{in} = \rho \cdot v \cdot dx dz dt$$

$$m_{out} = \left[\rho v + \frac{\partial(\rho v)}{\partial y} dy \right] \cdot dx dz dt$$



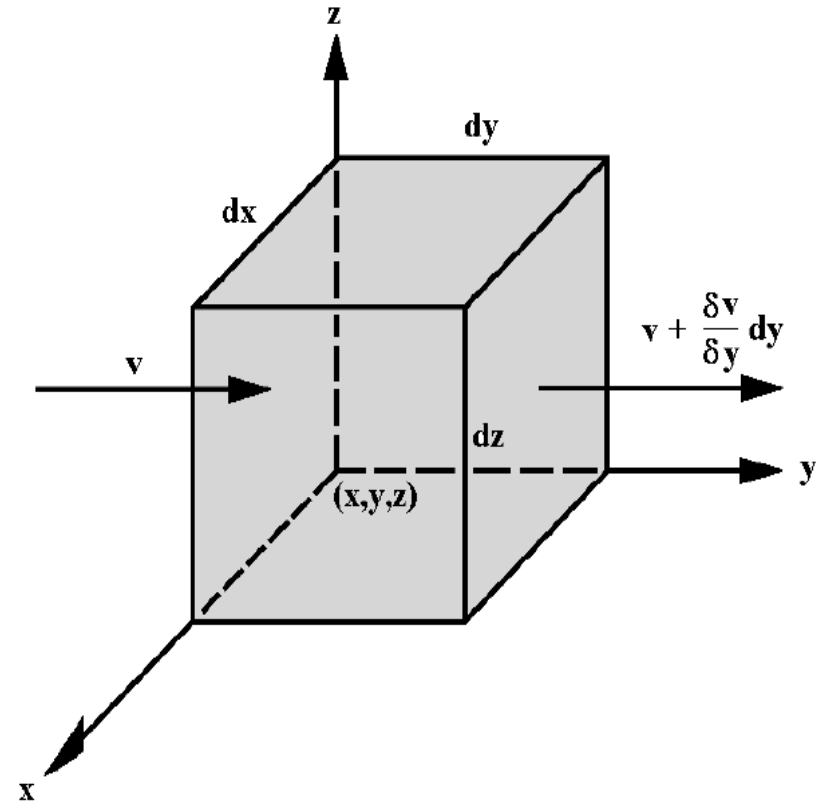
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$$m_{out} = \left[\rho v + \frac{\partial(\rho v)}{\partial y} dy \right] \cdot dx dz dt$$

$$\left(\frac{\partial m}{\partial t} \right) = \left[\rho v + \frac{\partial(\rho v)}{\partial y} dy \right] \cdot dx dz - \rho v dx dz$$



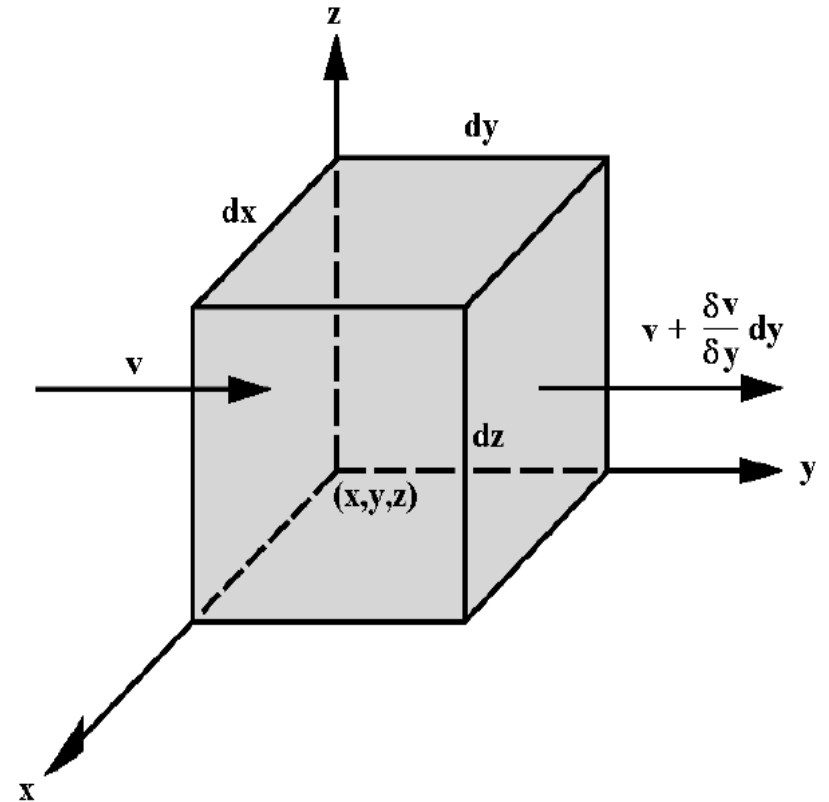
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$$\left(\frac{\partial m}{\partial t} \right) = \left[\rho v + \frac{\partial(\rho v)}{\partial y} dy \right] \cdot dx dz - \rho v dx dz = \frac{\partial(\rho v)}{\partial y} dx dy dz$$



Continuity Condition

Combining for x , y and z direction yields the **Continuity Equation**

$$\frac{\partial m}{\partial t}$$

Continuity Condition

Combining for x , y and z direction yields the **Continuity Equation**

$$\frac{\partial m}{\partial t} = -\frac{\partial \rho}{\partial t} dx dy dz$$

Continuity Condition

Combining for x , y and z direction yields the **Continuity Equation**

$$\frac{\partial m}{\partial t} = -\frac{\partial \rho}{\partial t} dx dy dz = \left\{ \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} \right\} dx dy dz$$

Continuity Condition

Combining for x , y and z direction yields the **Continuity Equation**

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

Continuity Condition

For an ideal, *incompressible* fluid:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

Continuity Condition

For an ideal, *incompressible* fluid:

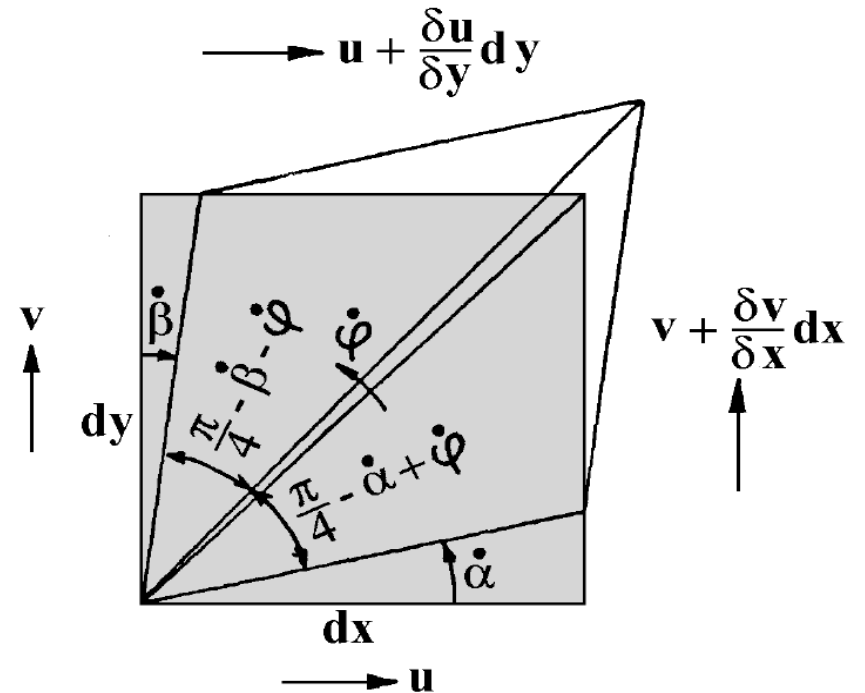
$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

Or, with $\nabla = \frac{\partial}{\partial x} + \frac{\partial}{\partial y} + \frac{\partial}{\partial z}$: $\nabla \bar{V} = 0$

Deformation of flow particles

Deformation

$$\frac{\partial v}{\partial x} = \tan \dot{\alpha} \approx \dot{\alpha} \quad \frac{\partial u}{\partial y} = \tan \dot{\beta} \approx \dot{\beta}$$



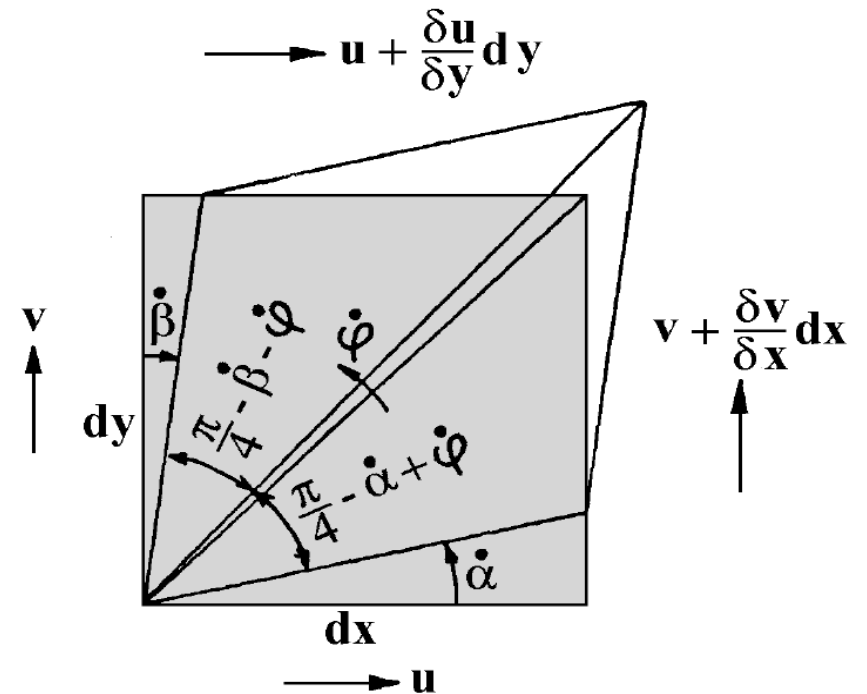
Deformation of flow particles

Deformation

$$\frac{\partial v}{\partial x} = \tan \dot{\alpha} \approx \dot{\alpha} \quad \frac{\partial u}{\partial y} = \tan \dot{\beta} \approx \dot{\beta}$$

Deformation velocity (dilatation):

$$\frac{\dot{\alpha} + \dot{\beta}}{2} = \frac{1}{2} \left(\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)$$



Deformation of flow particles

Deformation

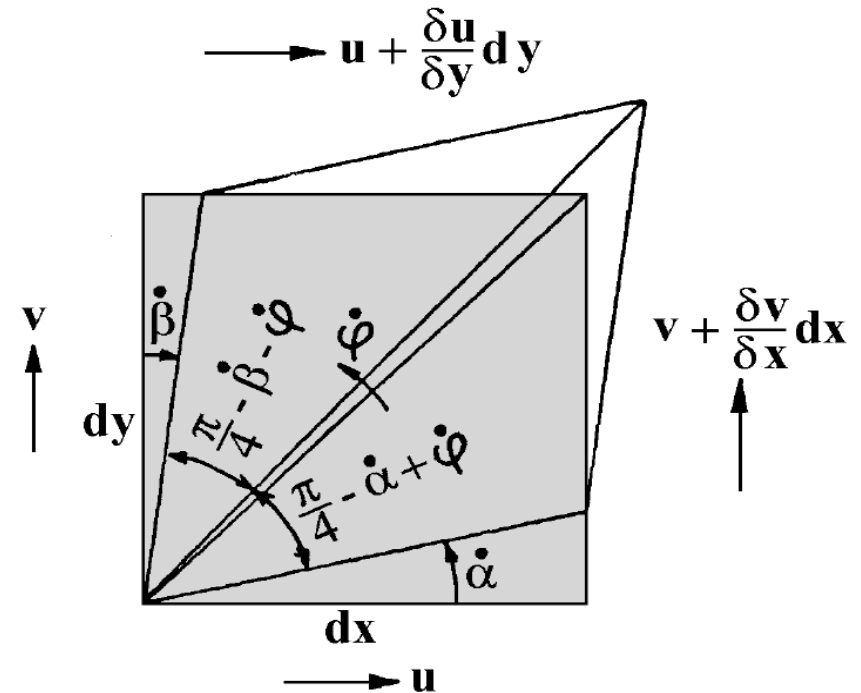
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Deformation velocity (dilatation):

$$\frac{\dot{\alpha} + \dot{\beta}}{2} = \frac{1}{2} \left(\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)$$

Rotation (in 2 D) :

$$\dot{\phi} = \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$



Velocity Potential

A scalar function, Φ

The velocity in any point of the fluid and in any direction is the derivative to that direction of the potential

$$u = \frac{\partial \Phi}{\partial x}$$

$$v = \frac{\partial \Phi}{\partial y}$$

$$w = \frac{\partial \Phi}{\partial z}$$

Properties of Velocity Potentials

- Combining the continuity condition with the velocity potentials results in the *Laplace* equation :

$$\frac{\partial^2 \Phi}{\partial x^2} + \frac{\partial^2 \Phi}{\partial y^2} + \frac{\partial^2 \Phi}{\partial z^2} = 0 \quad \text{or} \quad \nabla^2 \Phi = 0$$

- Potential flow is rotation-free by definition :

$$\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = 0 \quad \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} = 0 \quad \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x} = 0$$

Properties of Velocity Potentials

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Euler and Bernoulli

- Euler: Apply Newton's 2nd law to non viscous and incompressible fluid

$$dm \frac{Du}{Dt}$$

Euler and Bernoulli

- Euler: Apply Newton's 2nd law to non viscous and incompressible fluid

$$dm \frac{Du}{Dt} = \rho \cdot dx dy dz \cdot \frac{Du}{Dt} =$$

Euler and Bernoulli

- Euler: Apply Newton's 2nd law to non viscous and incompressible fluid

$$dm \frac{Du}{Dt} = \rho \cdot dx dy dz \cdot \frac{Du}{Dt} = -\frac{\partial p}{\partial x} dx \cdot dy dz$$

Mass* acceleration = pressure*area

Euler and Bernoulli

- Euler Equations:

$$\frac{\partial u}{\partial t} = u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial p}{\partial x}$$

With

$$u \frac{\partial u}{\partial x} = \frac{\partial \Phi}{\partial x} \cdot \frac{\partial^2 \Phi}{\partial x^2} = \frac{1}{2} \cdot \frac{\partial}{\partial x} \left(\frac{\partial \Phi}{\partial x} \right)^2$$

$$v \frac{\partial u}{\partial y} = \frac{\partial \Phi}{\partial y} \cdot \frac{\partial^2 \Phi}{\partial x \partial y} = \frac{1}{2} \cdot \frac{\partial}{\partial x} \left(\frac{\partial \Phi}{\partial y} \right)^2$$

$$w \frac{\partial u}{\partial z} = \frac{\partial \Phi}{\partial z} \cdot \frac{\partial^2 \Phi}{\partial x \partial z} = \frac{1}{2} \cdot \frac{\partial}{\partial x} \left(\frac{\partial \Phi}{\partial z} \right)^2$$

Euler and Bernoulli

- Differentiate w.r.t. x , y or z gives 0:

$$\frac{\partial}{\partial x} \left\{ \frac{\partial \Phi}{\partial t} + \frac{1}{2} \left[\left(\frac{\partial \Phi}{\partial x} \right)^2 + \left(\frac{\partial \Phi}{\partial y} \right)^2 + \left(\frac{\partial \Phi}{\partial z} \right)^2 \right] + \frac{p}{\rho} \right\} = 0 \quad (\text{similar for } y, z)$$

Euler and Bernoulli

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$$\frac{\partial}{\partial x} \left\{ \frac{\partial \Phi}{\partial t} + \frac{1}{2} \left[\left(\frac{\partial \Phi}{\partial x} \right)^2 + \left(\frac{\partial \Phi}{\partial y} \right)^2 + \left(\frac{\partial \Phi}{\partial z} \right)^2 \right] + \frac{p}{\rho} \right\} = 0 \quad (\text{similar for } y, z)$$

- This expression is a function of time only, providing the **Bernoulli Equation**:

$$\frac{\partial \Phi}{\partial t} + \frac{1}{2} V^2 + \frac{p}{\rho} + gz = C(t)$$

Euler and Bernoulli

- For a *stationary* flow along a streamline :

$$\frac{1}{2}V^2 + \frac{p}{\rho} + gz = C$$

- This can be written in two alternative ways :

$$\frac{V^2}{2g} + \frac{p}{\rho g} + z = C$$

$$\frac{1}{2}\rho V^2 + p + \rho gz = C$$

Stream Function Ψ

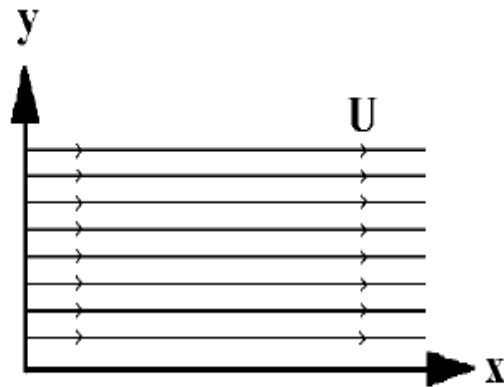
- $\Psi = \text{constant}$ along a streamline
- Definition : $u = \frac{\partial \Psi}{\partial y}$ and $v = -\frac{\partial \Psi}{\partial x}$
- Stream lines and equipotential lines are orthogonal
- No cross flow, impervious boundary of stream tube

Potential Flow Elements

- Uniform flow
- Source
- Sinks
- Circulation

Superposition is allowed

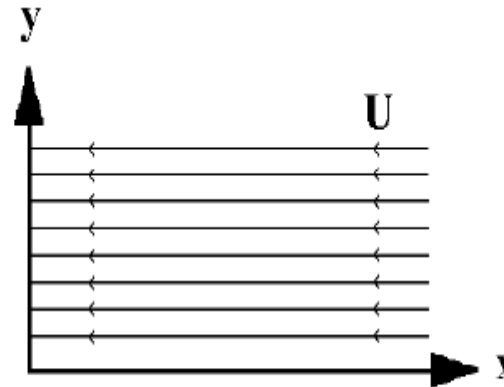
Uniform Flow



**a. Uniform Flow
(in positive x-direction)**

$$\Phi = +U \cdot x$$

$$\Psi = +U \cdot y$$

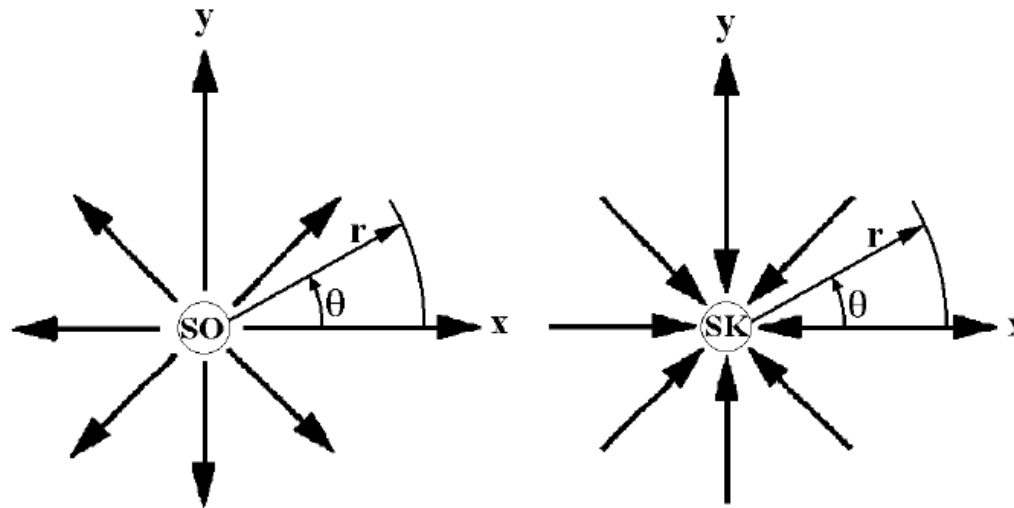


**b. Uniform Flow
(in negative x-direction)**

$$\Phi = -U \cdot x$$

$$\Psi = -U \cdot y$$

Source & Sink



c. Source

d. Sink

$$\Phi = -\frac{Q}{2\pi} \cdot \ln r$$

$$\Phi = +\frac{Q}{2\pi} \cdot \ln r$$

$$\Psi = +\frac{Q}{2\pi} \cdot \theta$$

$$\Psi = -\frac{Q}{2\pi} \cdot \theta$$

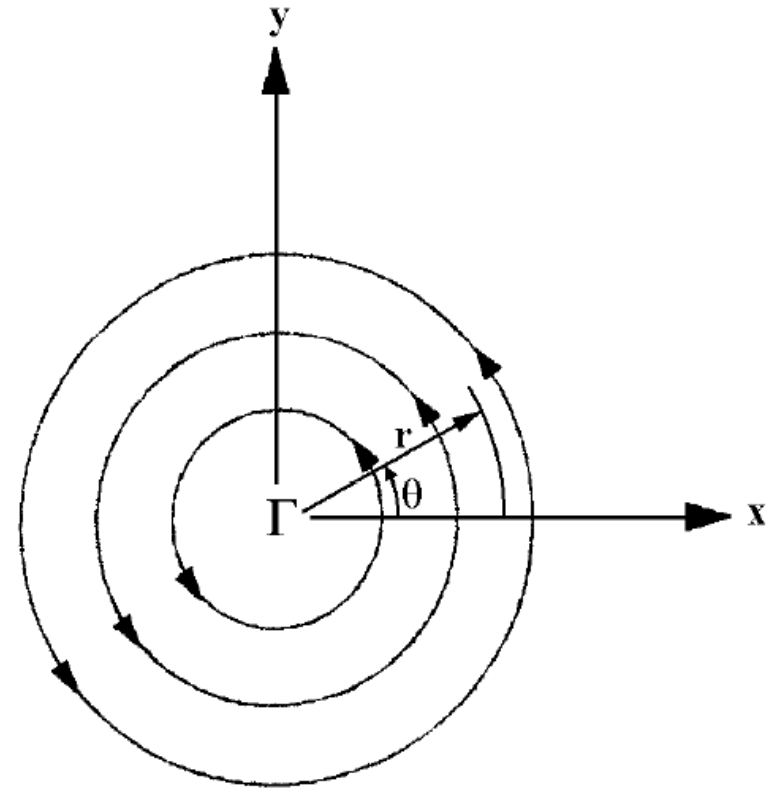
Circulation (Vortex)

- Counter clockwise flow:

$$\Phi = +\frac{\Gamma}{2\pi} \cdot \theta \quad \Psi = -\frac{\Gamma}{2\pi} \cdot \ln r$$

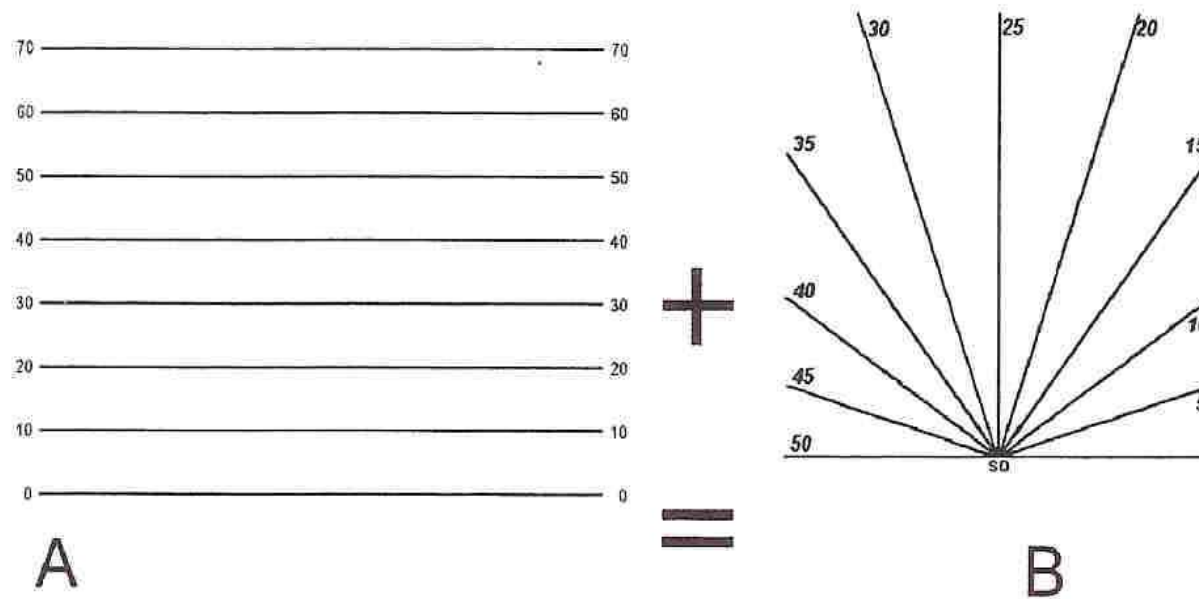
- Clockwise flow

$$\Phi = -\frac{\Gamma}{2\pi} \cdot \theta \quad \Psi = +\frac{\Gamma}{2\pi} \cdot \ln r$$

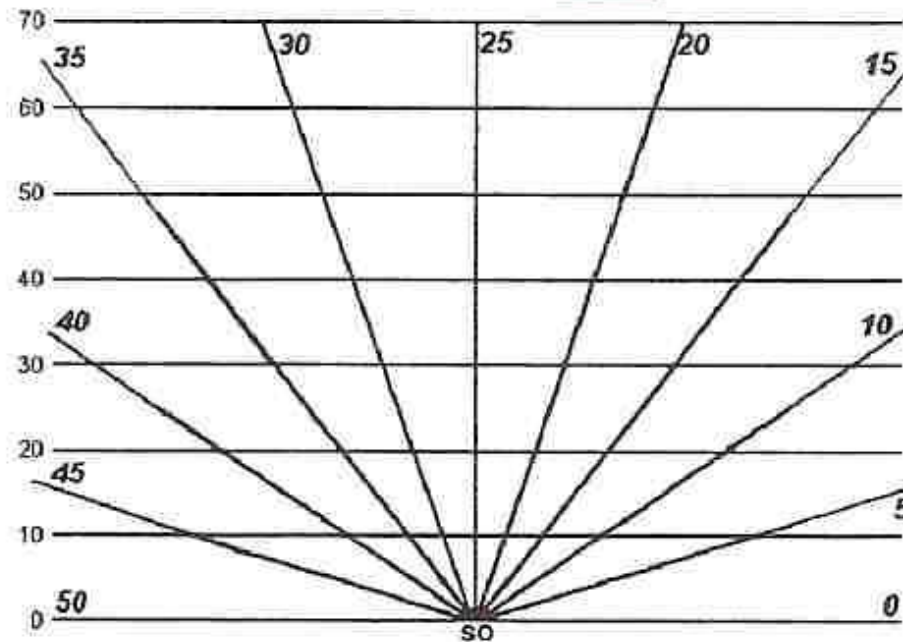


e. Circulation

Superposition - principle

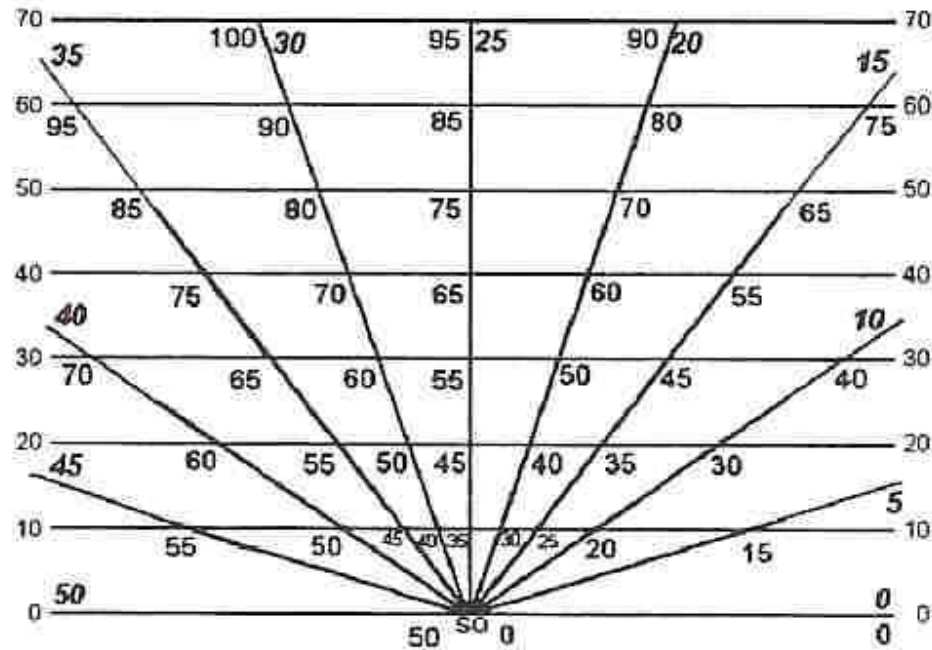


Superposition - principle



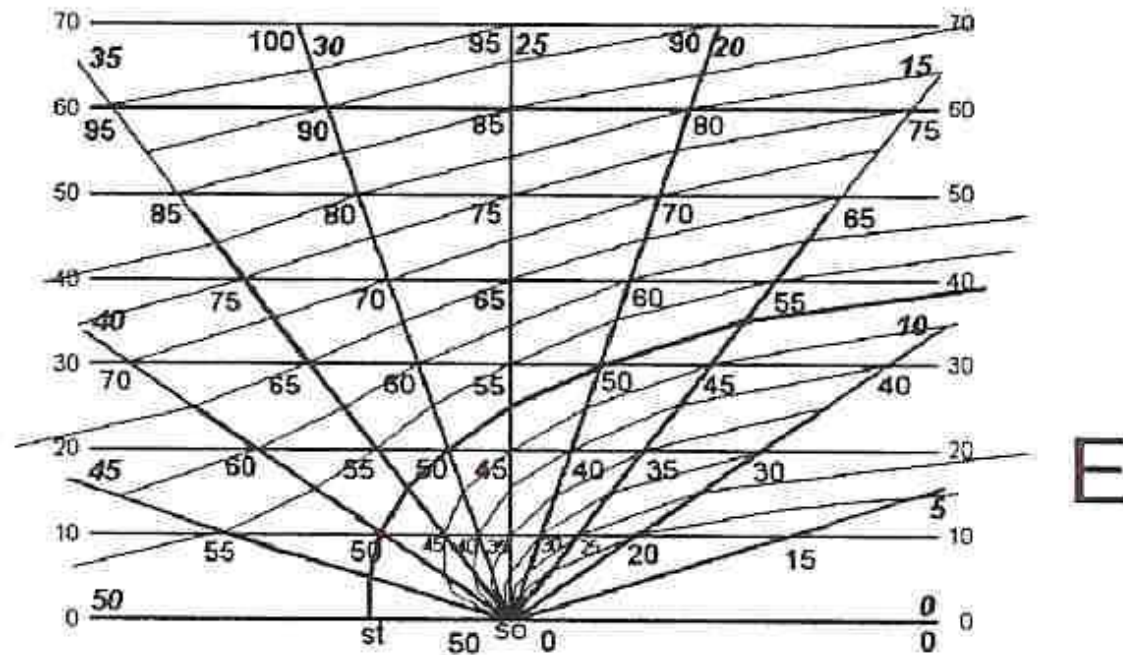
C

Superposition - principle



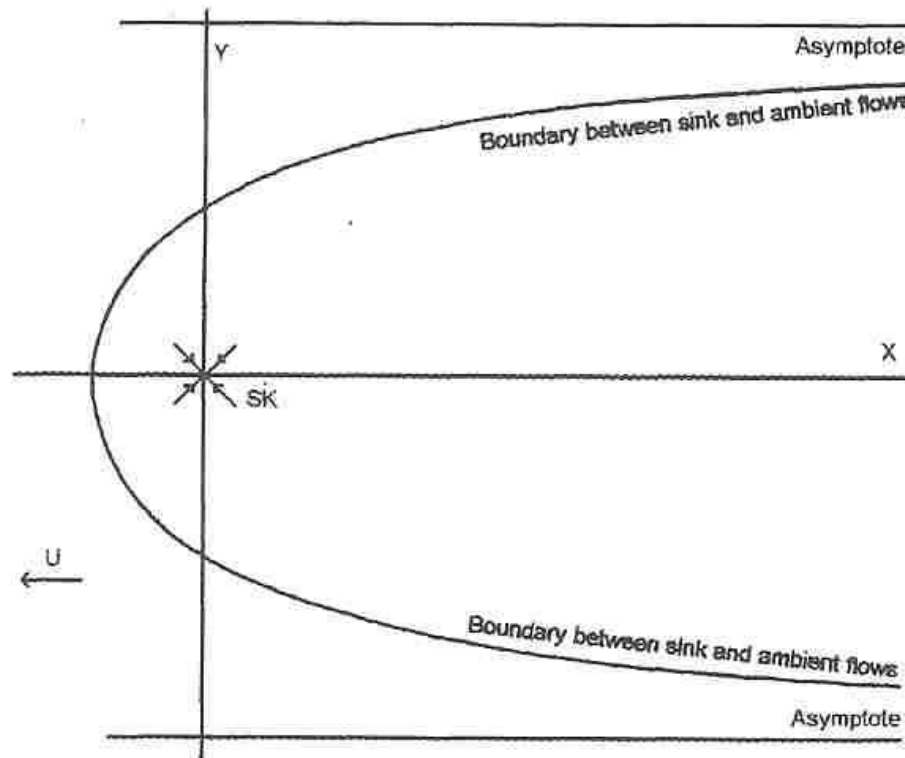
D

Superposition - principle



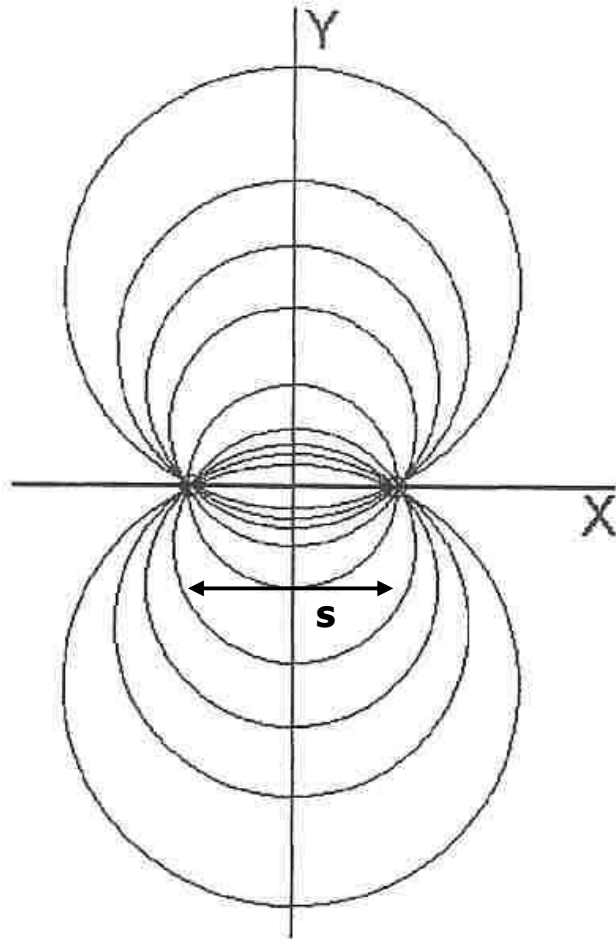
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Uniform flow + sink



$$\Psi = -\frac{Q}{2\pi} \cdot \arctan\left(\frac{y}{x}\right) - U_{\infty} \cdot y$$

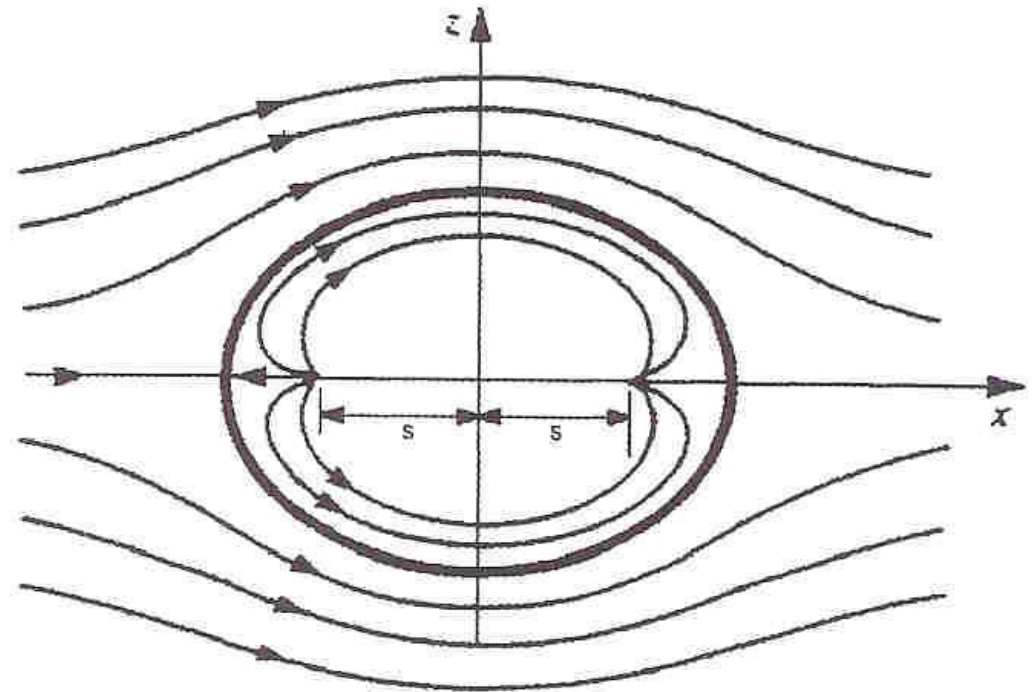
Separated Source + sink



$$\Psi = \frac{Q}{2\pi} \cdot \arctan\left(\frac{2ys}{x^2 + y^2 + s^2}\right)$$

Uniform flow + source + sink

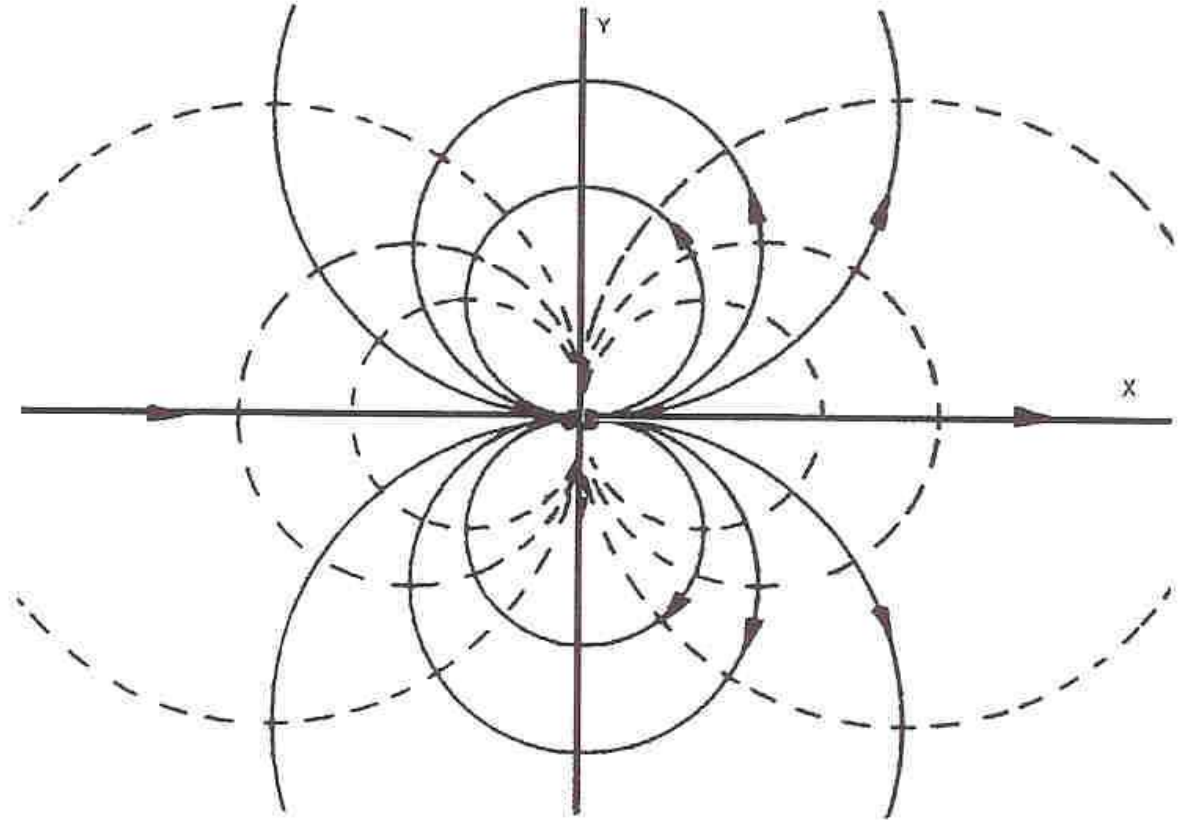
- No flow through boundary
(= streamline)
- Rankine ship forms



$$\Psi = \frac{Q}{2\pi} \cdot \arctan\left(\frac{2ys}{x^2 + y^2 - s^2}\right) + U_\infty \cdot y$$

Doublet or Dipole

- A source and sink pair placed very close together
- ($s \rightarrow 0$)

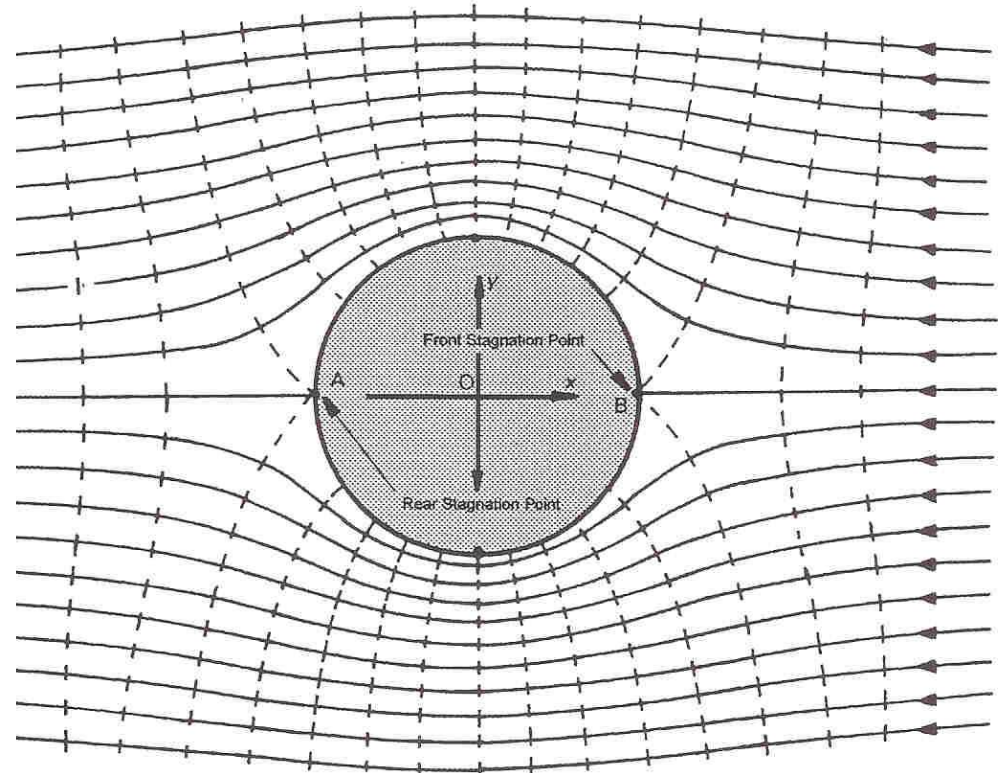


$$\Psi = \mu \cdot \frac{y}{x^2 + y^2}$$

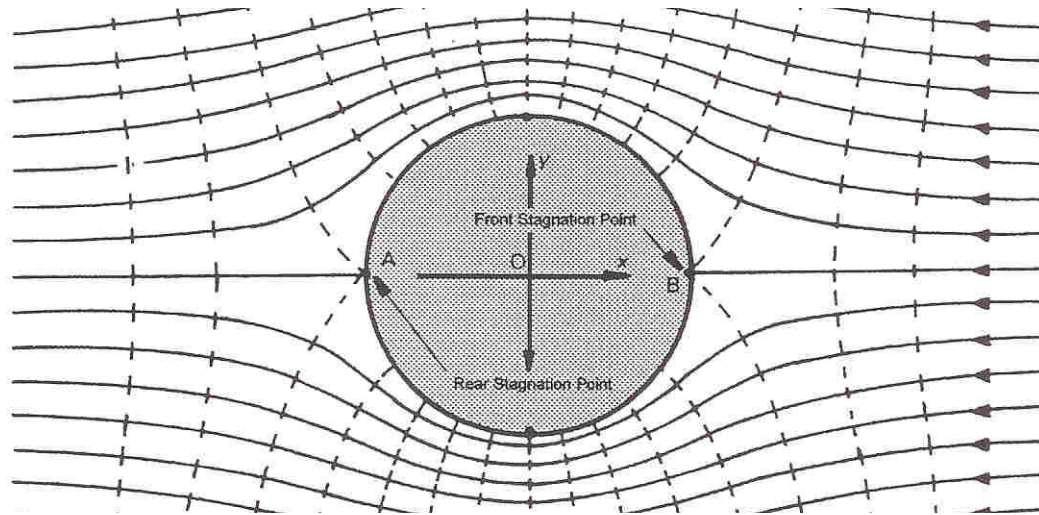
$$\Phi = \mu \cdot \frac{x}{x^2 + y^2}$$

Dipole + uniform flow

- Model for cylinder
- X-axis is a streamline
- Boundary at $R = \sqrt{\frac{\mu}{U_\infty}}$
is also a streamline



Uniform flow around a cylinder

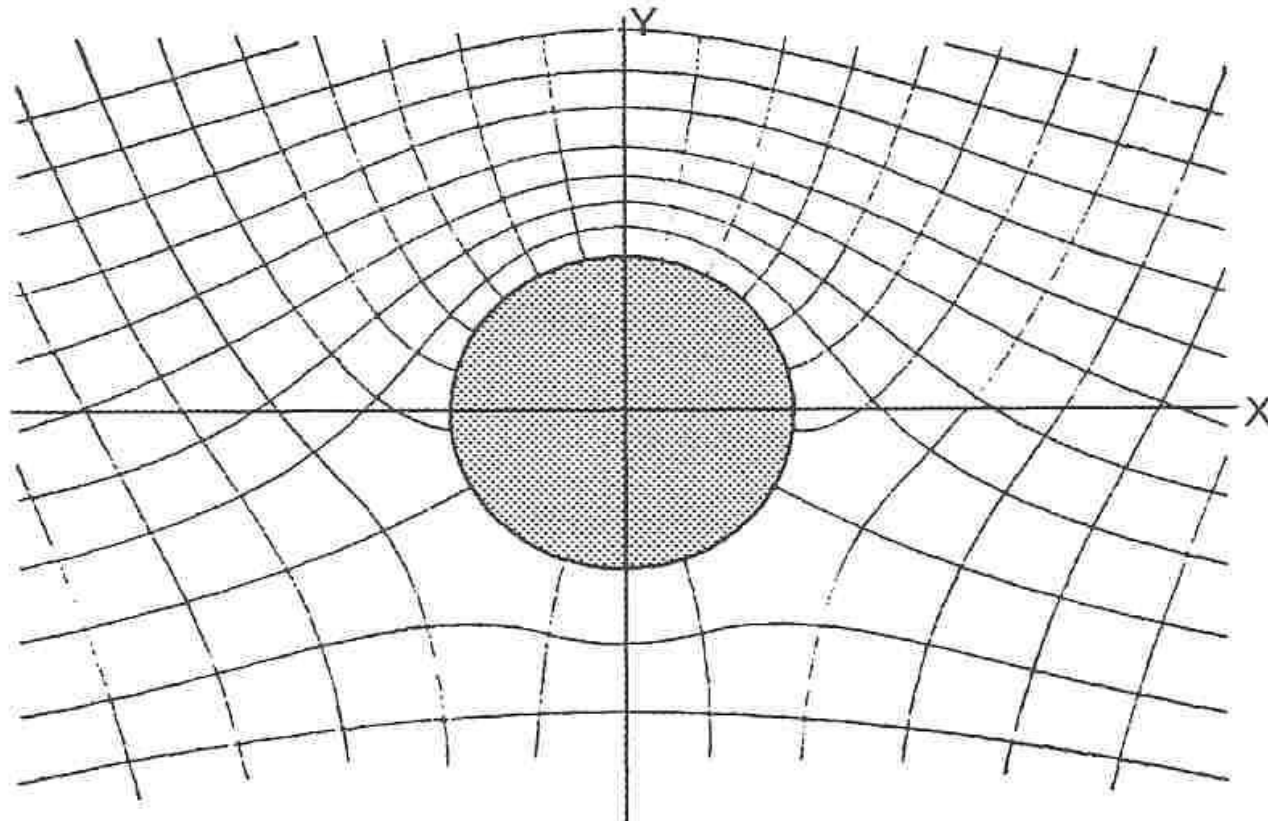


$$v_{\theta} = -\left[\frac{\partial\Psi}{\partial r}\right]_{r=R} = -\frac{\partial}{\partial r}\left\{\frac{\mu\sin\theta}{r} - U_{\infty}r\sin\theta\right\}_{r=R} \quad v_{\theta} = -2U_{\infty}\sin\theta$$

- $V_{\theta} = 0$ at stagnation points
- $V_{\theta} = 2*U_{\infty}$ at sides of cylinder

Uniform flow + circulation

Pressure asymmetry creates a lift force



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Continuity Condition

Continuity Equation, general case

$$\frac{\partial \rho}{\partial t} + \frac{\partial(\rho u)}{\partial x} + \frac{\partial(\rho v)}{\partial y} + \frac{\partial(\rho w)}{\partial z} = 0$$

Ideal fluid, incompressible

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

Deformation of flow particles

Deformation velocity or dilatation:

$$\frac{\dot{\alpha} + \dot{\beta}}{2} = \frac{1}{2} \left(\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right)$$

Rotation (in 2 D) :

$$\dot{\phi} = \frac{1}{2} \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$$

Velocity Potential

A scalar function, Φ

The velocity in any point of the fluid and in any direction is the derivative to that direction of the potential

$$u = \partial\Phi/\partial x \text{ etc}$$

Properties of Velocity Potentials

- The continuity condition results in the *Laplace* equation :

$$\left| \frac{\partial^2 \Phi}{\partial x^2} + \frac{\partial^2 \Phi}{\partial y^2} + \frac{\partial^2 \Phi}{\partial z^2} = 0 \right| \quad \text{or:} \quad \left| \nabla^2 \Phi = 0 \right|$$

- Potential flow is rotation-free by definition :

$$\left| \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = 0 \right|$$

Euler and Bernoulli

Force = mass * acceleration : Euler
non viscous and incompressible fluid

$$\left[\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \cdot \frac{\partial p}{\partial x} \right]$$

Energy conservation along a flowline : Bernoulli
non viscous and incompressible fluid

$$\frac{\partial}{\partial x} \left\{ \frac{\partial \Phi}{\partial t} + \frac{1}{2} \left[\left(\frac{\partial \Phi}{\partial x} \right)^2 + \left(\frac{\partial \Phi}{\partial y} \right)^2 + \left(\frac{\partial \Phi}{\partial z} \right)^2 \right] + \frac{p}{\rho} \right\} = 0 \quad \left[\frac{\partial \Phi}{\partial t} + \frac{1}{2} V^2 + \frac{p}{\rho} + gz = C(t) \right]$$

stationary flow :

$$\left[\frac{1}{2} \rho V^2 + p + \rho gz = \text{Constant} \right]$$

Stream Function Ψ

- Companion of the Velocity Potential

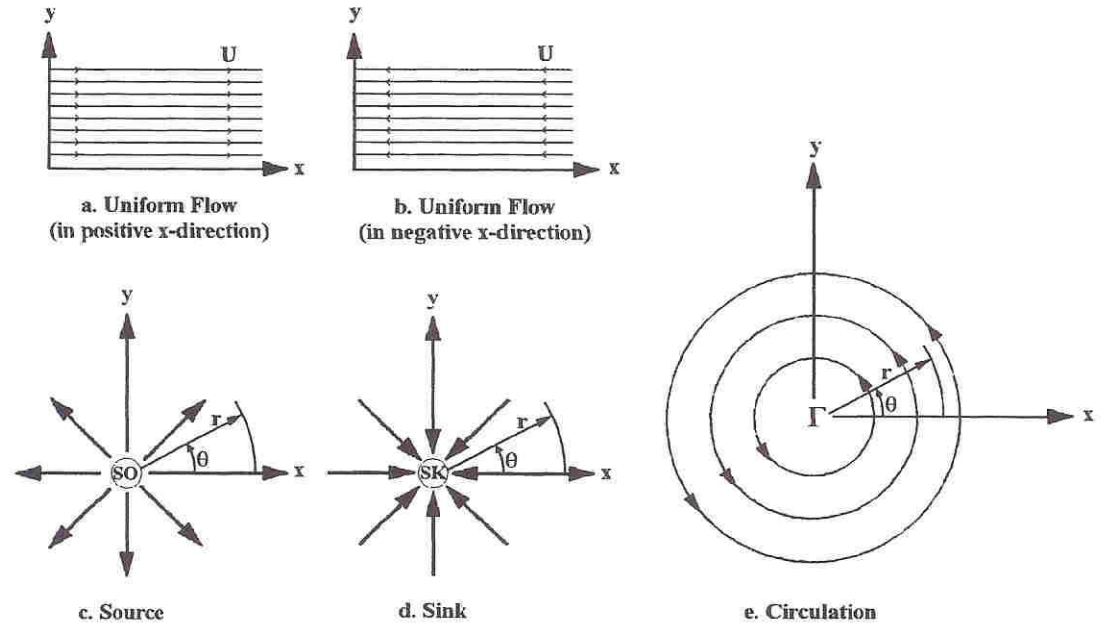
- Definition :
$$\boxed{u = \frac{\partial \Psi}{\partial y}} \quad \text{(a)} \quad \text{and} \quad \boxed{v = -\frac{\partial \Psi}{\partial x}} \quad \text{(b)}$$

- Stream lines and equipotential lines are orthogonal
- No cross flow, impervious boundary of stream tube

Potential Flow Elements

- Uniform flow
- Sources and sinks
- Circulating flows

Superposition is allowed



Polar Coordinate Description

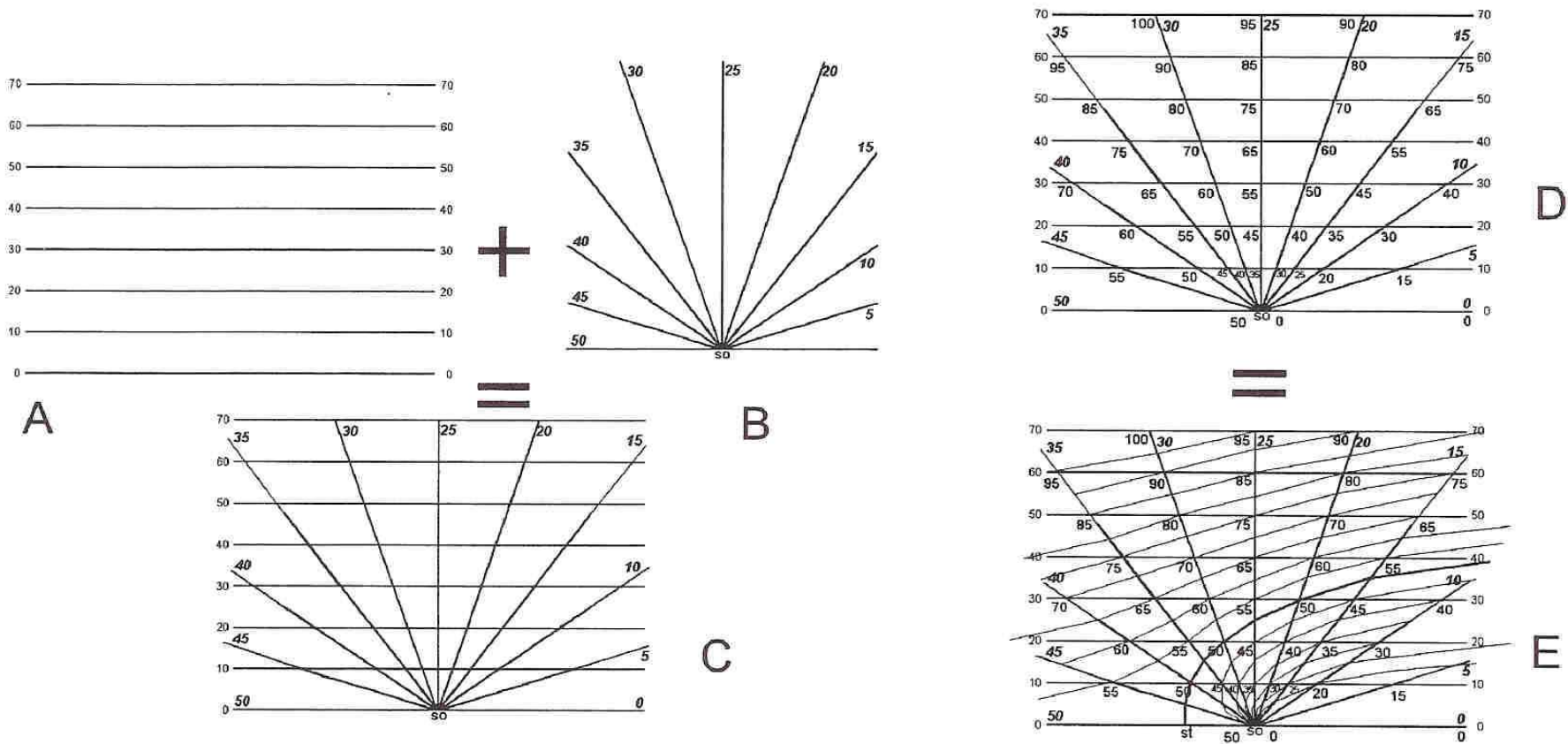
Basic definitions : $\boxed{v_r = +\frac{\partial\Phi}{\partial r} = \frac{1}{r} \cdot \frac{\partial\Psi}{\partial\theta}}$ (a) and $\boxed{v_\theta = \frac{1}{r} \cdot \frac{\partial\Phi}{\partial\theta} = -\frac{\partial\Psi}{\partial r}}$ (b)

Source : $\boxed{\Phi = +\frac{Q}{2\pi} \cdot \ln r}$ (a) and $\boxed{\Psi = +\frac{Q}{2\pi} \cdot \theta}$ (b)
(Sink = - source)

Vortex : $\boxed{\Phi = +\frac{\Gamma}{2\pi} \cdot \theta}$ (a) and $\boxed{\Psi = -\frac{\Gamma}{2\pi} \cdot \ln r}$ (b)

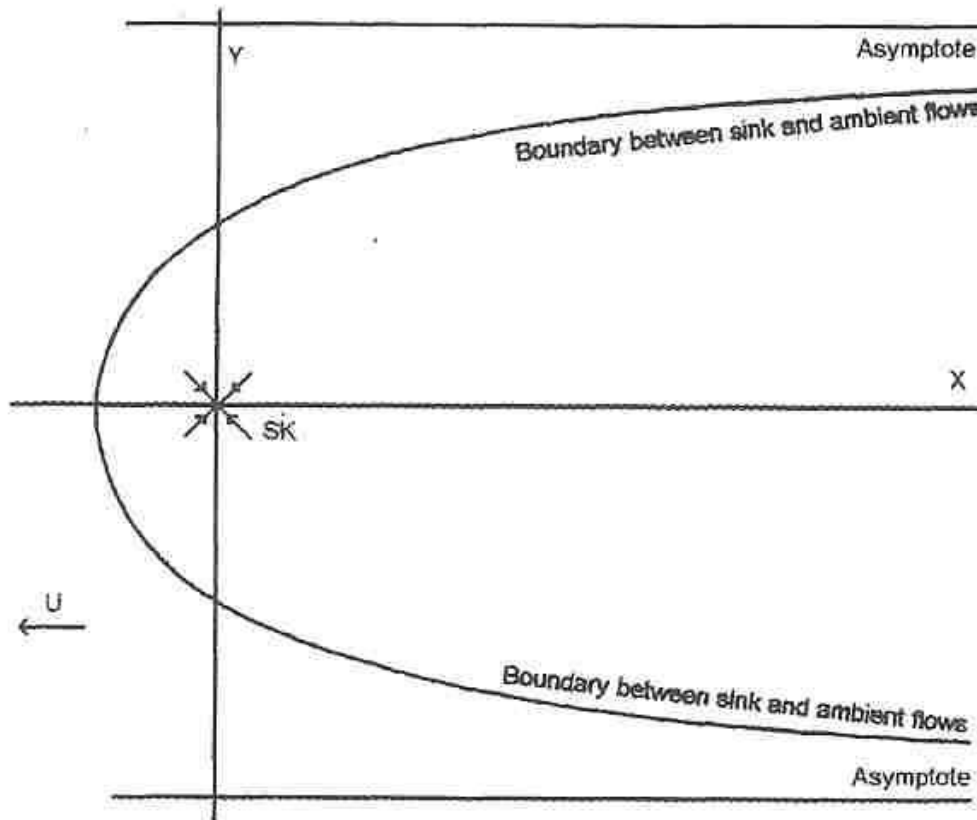
$$\Gamma = \oint v_\theta \cdot ds = 2\pi r \cdot v_\theta = \text{constant}$$

Superposition - principle



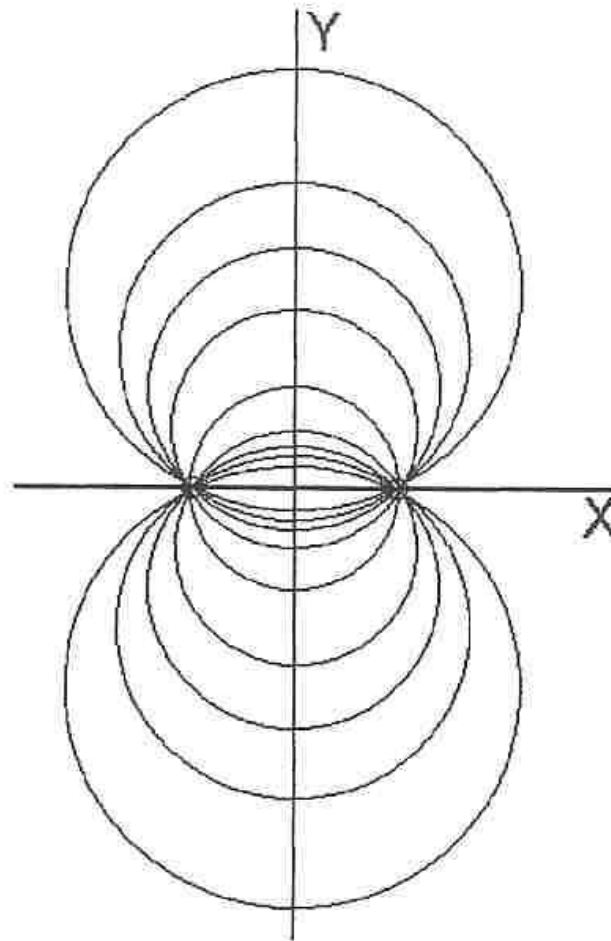
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Uniform flow + sink



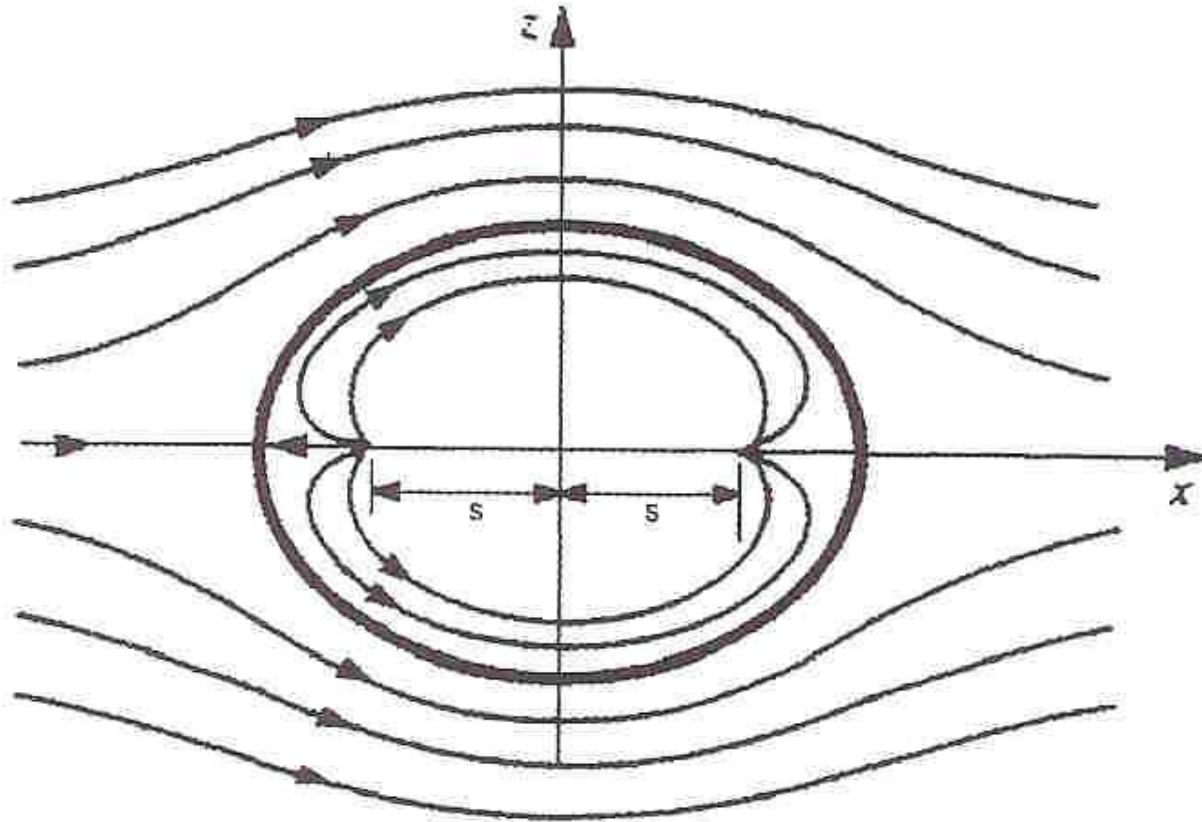
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Source + sink



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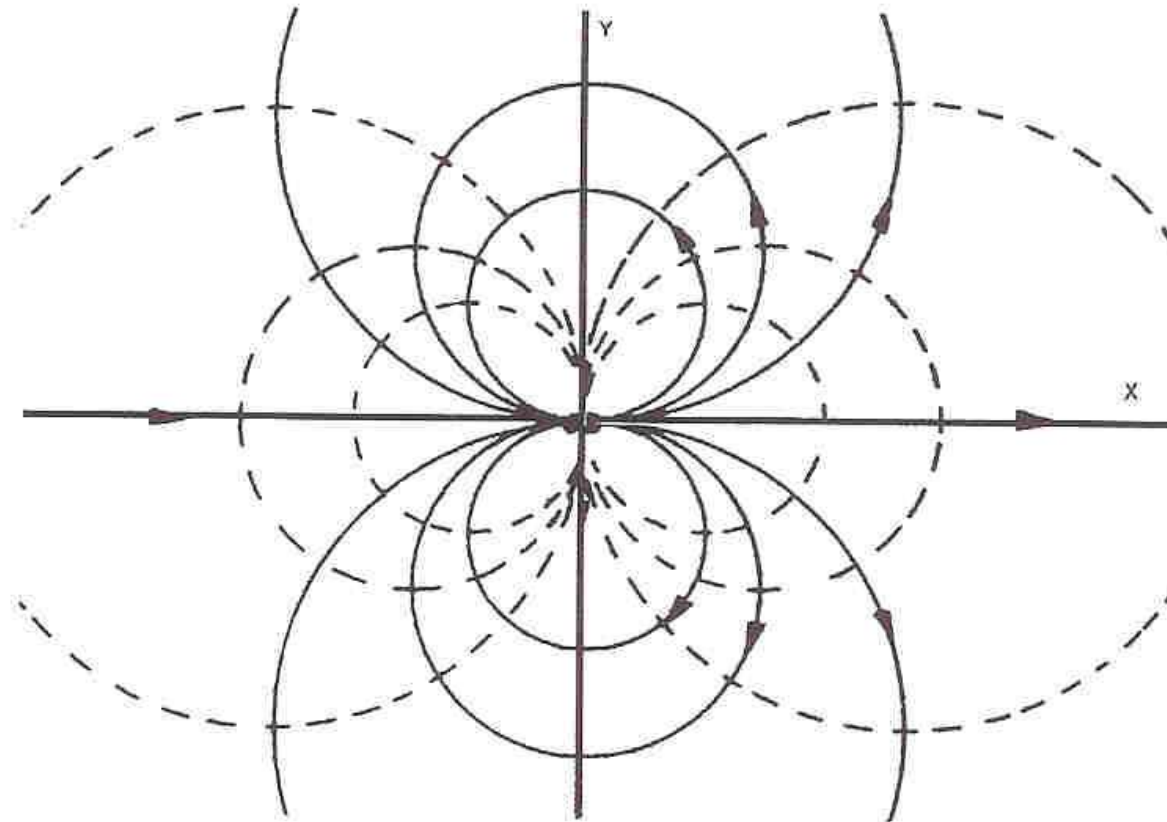
Uniform flow + source + sink



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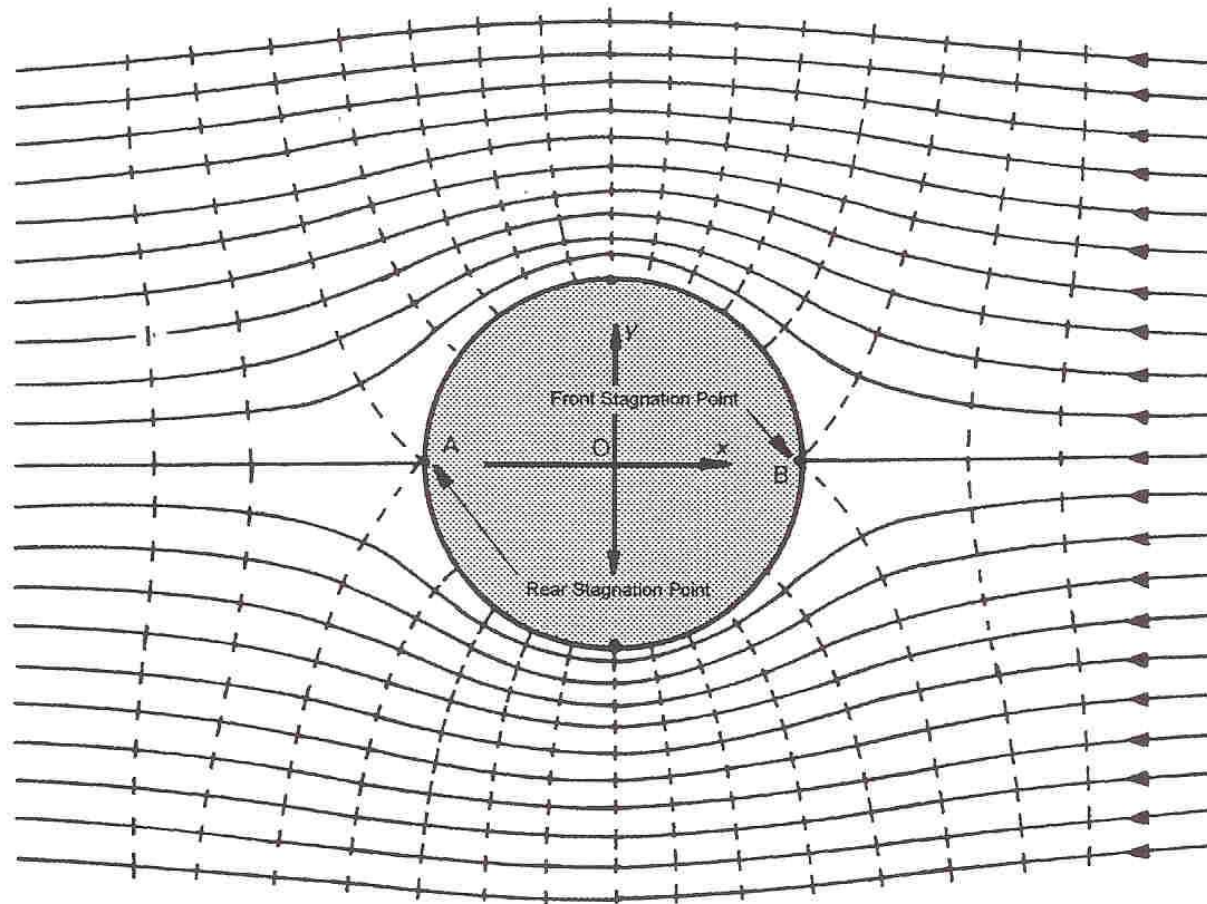
Dipole

Strength $\mu = Qs/\pi$



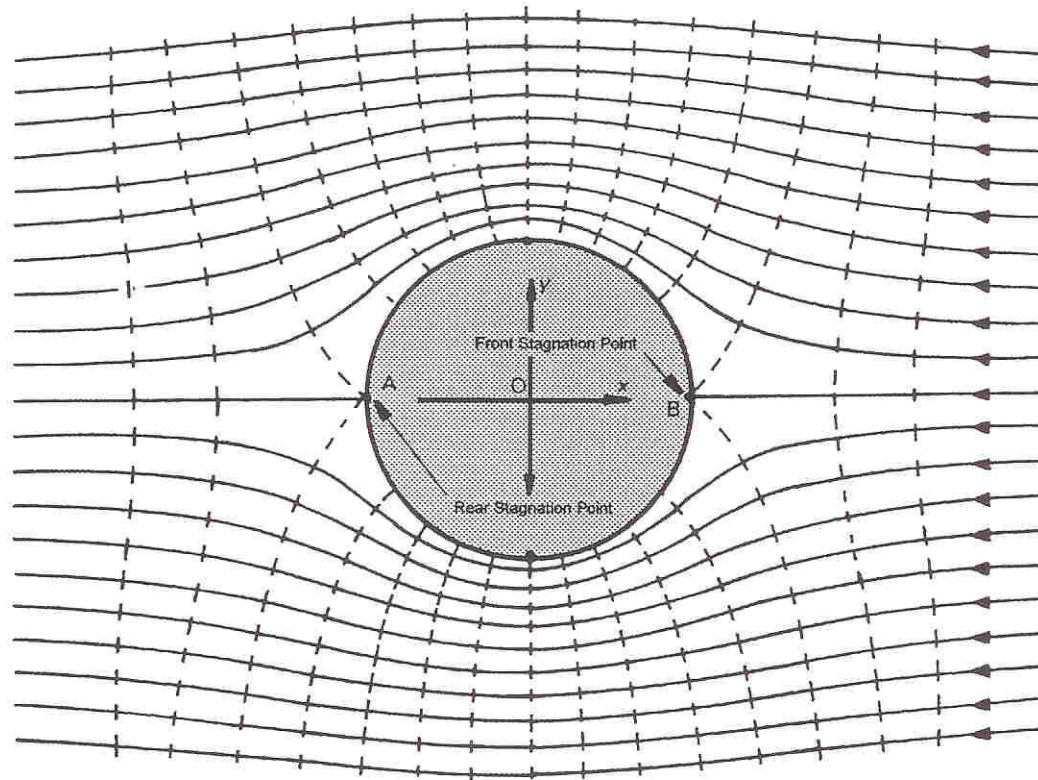
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Dipole + uniform flow



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Uniform flow around a cylinder



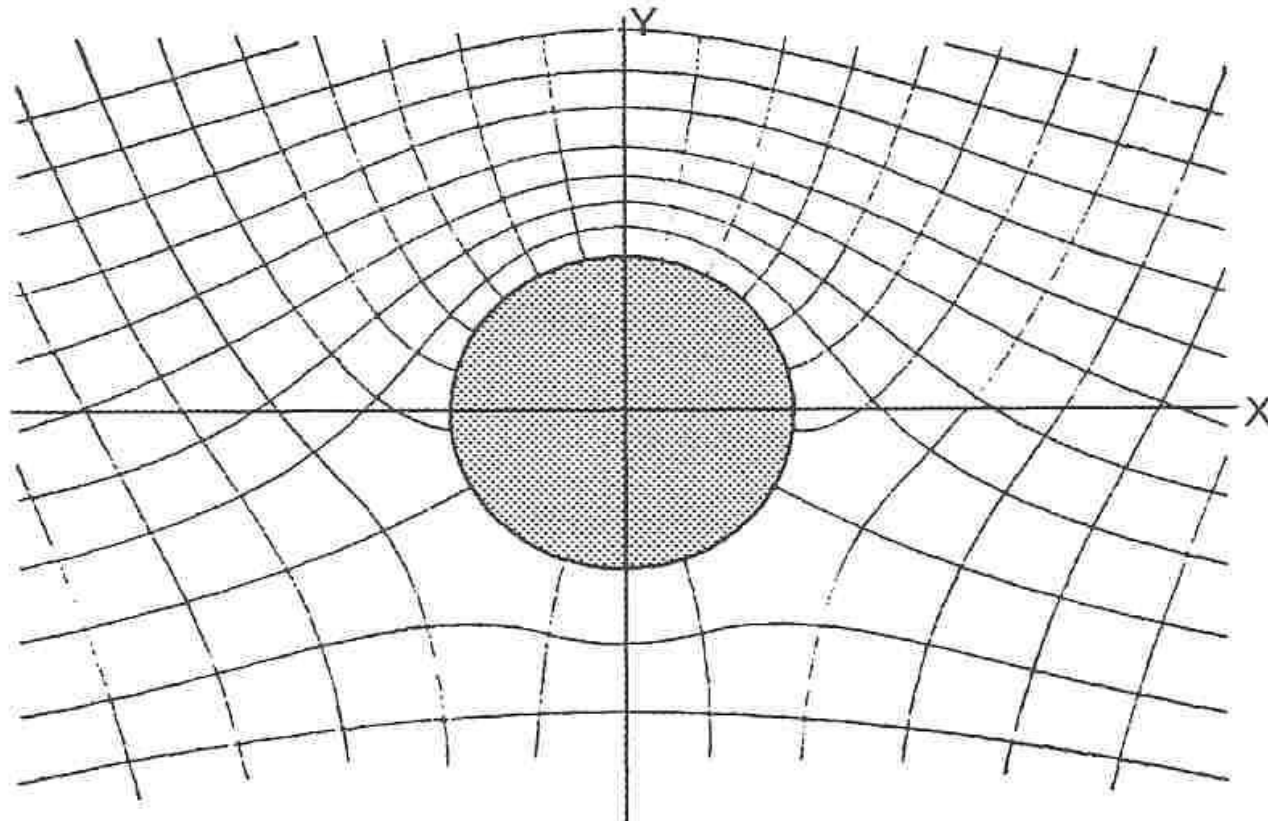
Stagnation points on the X axis

$$V_{\max} = 2 U \text{ at Y axis}$$

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Uniform flow + circulation

Pressure asymmetry creates a lift force



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